



# Development of autonomous platforms for kinetic model identification

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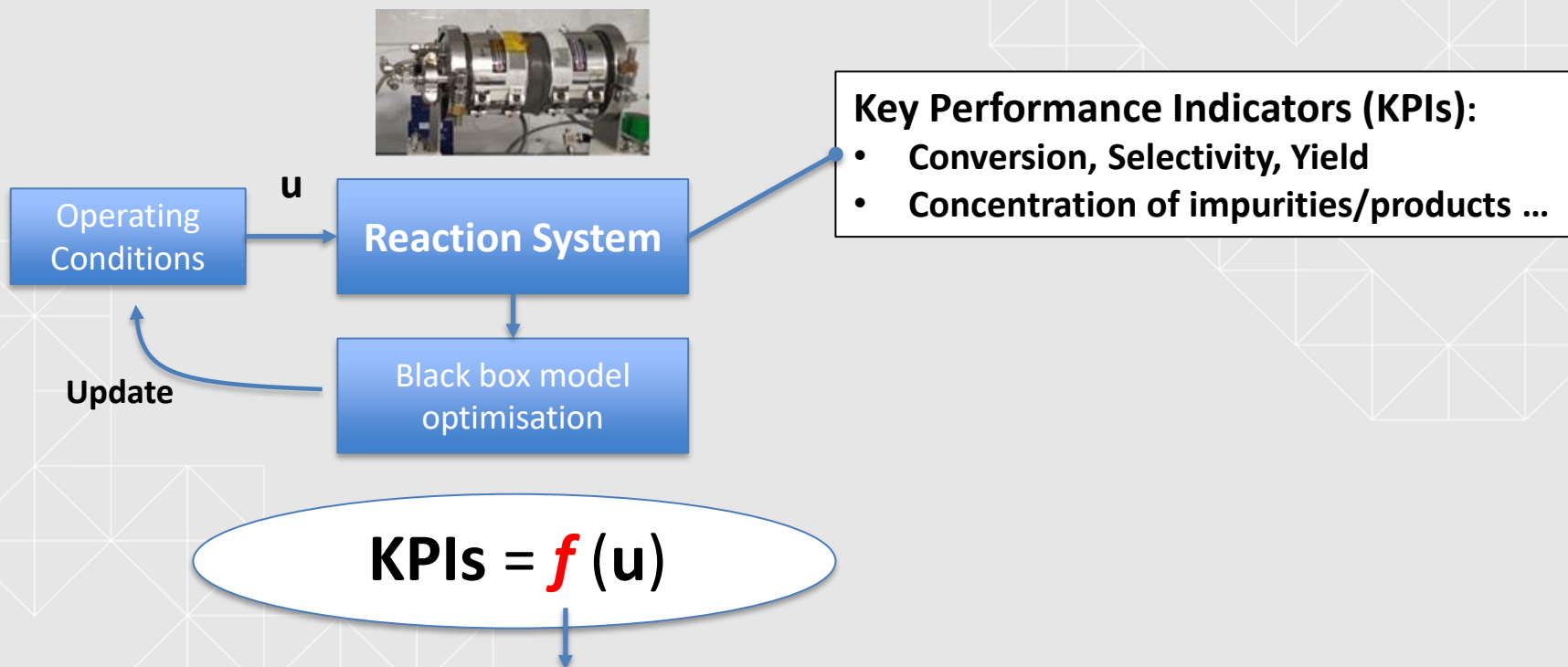


# Outline

- **Introduction**
  - Problem definition
  - Automated Vs Autonomous reaction systems
  - Model identification procedures: key steps and bottlenecks
  - Autonomous reaction systems: synergies and collaborations
- **Autonomous Platforms for Kinetic Model Identification**
  - Key elements and features
  - Integration of standard and advanced Model-based Design of Experiments (MBDoE) techniques
  - Case Study 1: Benzoic Acid Esterification in a Capillary Microreactor System
  - Case Study 2: Catalytic Methane Oxidation in a Microreactor Platform
  - The problem of practical distinguishability under uncertainty
- **ML-Assisted Model Identification**
  - Kinetic Model Structure Identification using ANNs-based Optimal Experimental Design
  - ML-Assisted Reliability Mapping
- **Final remarks**

# Introduction

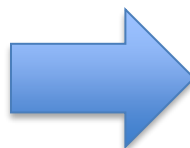
*Problem definition: optimisation of flow reaction systems<sup>1,2</sup>*



**Challenge:** identifying a reliable functional form  $f$  (model) relating operating conditions ( $u$ ) to KPIs

$f$  can be represented by

1. a **data-driven** or **surrogate model** (ML)
2. a **physics-based, mechanistic model**
3. a **hybrid model**, combining 1) and 2)



Interested in solving the **inverse problem**

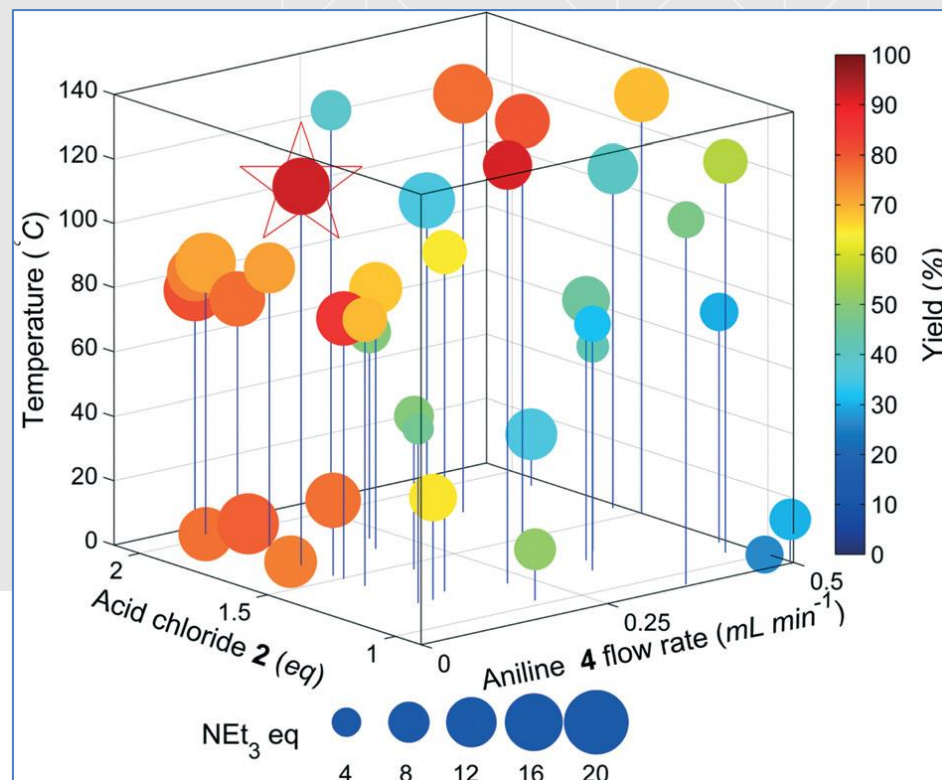
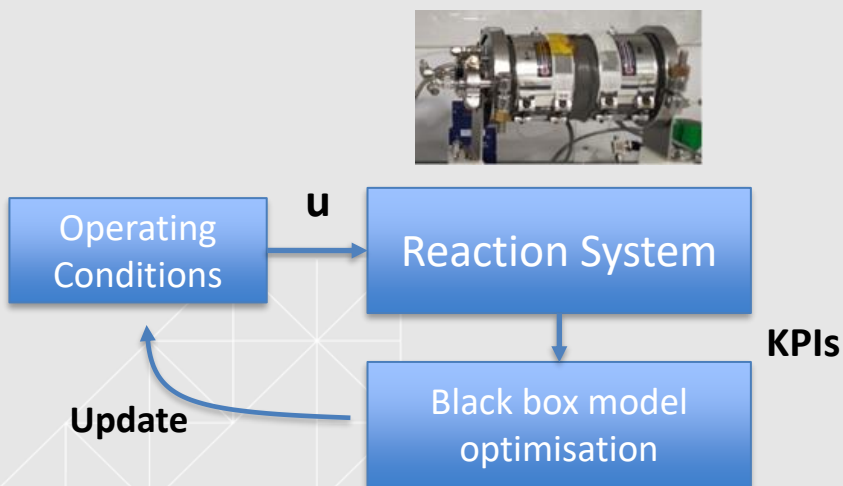
$$u = f^{-1}(\text{KPIs})$$

<sup>1</sup>Reizman, B. J., Jensen, K. F. (2012). An Automated Continuous-Flow Platform for the Estimation of Multistep Reaction Kinetics. *Org. Process Res. Dev.* 2012, 16, 11, 1770.

<sup>2</sup>Bourne, R. A. et al. (2016). Self-optimisation of the final stage in the synthesis of EGFR kinase inhibitor AZD9291 using an automated flow reactor. *React. Chem. Eng.*, 1, 366.

# Introduction

*Problem definition: data-driven optimisation in automated flow reaction systems<sup>1,2</sup>*



## PROS

- Agile exploration of reaction conditions
- Fast evaluation/optimisation of KPIs

## CONS

- Knowledge on reaction kinetics not guaranteed
- **Extrapolation to unexplored regions particularly challenging (critical for scale-up!)**
- May require many runs before reaching a convergence
- Extremely **sensitive to data quality**

<sup>1</sup>Reizman, B. J., Jensen, K. F. (2012). An Automated Continuous-Flow Platform for the Estimation of Multistep Reaction Kinetics. *Org. Process Res. Dev.* 2012, 16, 11, 1770.

<sup>2</sup>Bourne, R. A. et al. (2016). Self-optimisation of the final stage in the synthesis of EGFR kinase inhibitor AZD9291 using an automated flow reactor. *React. Chem. Eng.*, 1, 366.

# Introduction

*Reaction platforms: where are we heading to?*

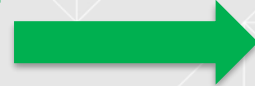


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## Reaction platforms<sup>1</sup> can be:

- **Automated:** systems allowing enhanced control and data acquisition, agile execution of scheduled **open-loop** experiments, requiring minimum user intervention
- **Autonomous:** automated reaction system enabling **closed-loop** operation, self-optimisation and experimental design with no user intervention during operation. High-level decisions still required (*Example: choice of design criteria/KPIs targets, stopping rules, etc.*)
- **Intelligent:** autonomous reaction system capable of **adapting through learning**, even in presence of disturbances from the environment. All decisions (including high-level ones) are directly taken by the platform (no inputs from the user are required)

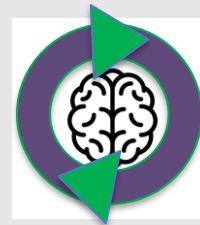
Past



Present



Future



<sup>1</sup>Barz, T., Kager, J., Herwig, C., Neubauer, P., Bournazou, M. N. C., Galvanin, F. (2022). Characterization of reactions and growth in automated continuous flow and bioreactor platforms—From linear DoE to model-based approaches, *Simulation and Optimization in Process Engineering*, 273-319.



# Introduction

## Autonomous Reaction Systems – Team Synergies (1)



### Federico Galvanin

- Computational Algorithms for Model Identification
- Optimal Experimental Design
- Autonomous Reaction Systems
- Machine Learning Applications to Systems Modelling

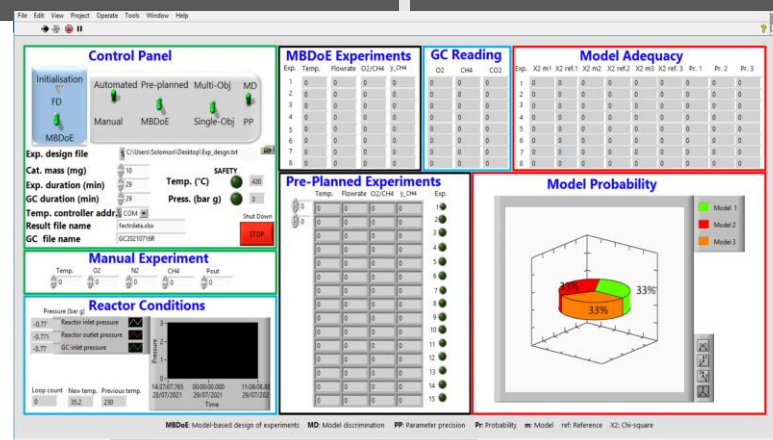
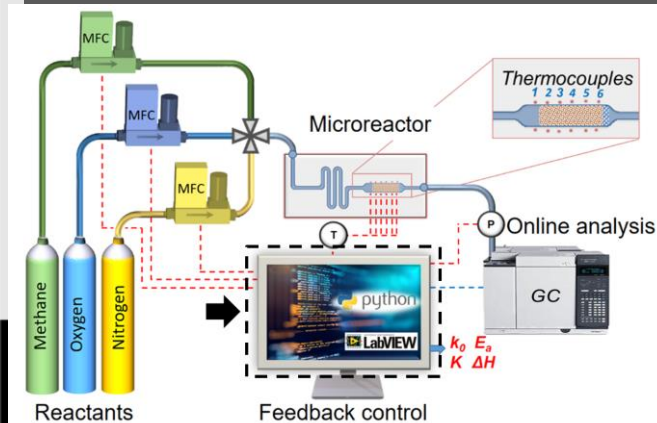
[www.homepages.ucl.ac.uk/~ucecfea/](http://www.homepages.ucl.ac.uk/~ucecfea/)



### Asterios Gavriilidis

- Reaction Engineering
- Flow chemistry
- Design of automated reactor platforms
- Integration with online analysis tools

[www.ucl.ac.uk/chemical-engineering/research/gavriilidis-lab](http://www.ucl.ac.uk/chemical-engineering/research/gavriilidis-lab)



## Development of autonomous platforms for kinetic model identification

# Introduction

## Cloud-based Experimental Design and Analysis Service (EDAS)



AstraZeneca

Lab-scale flow reactor

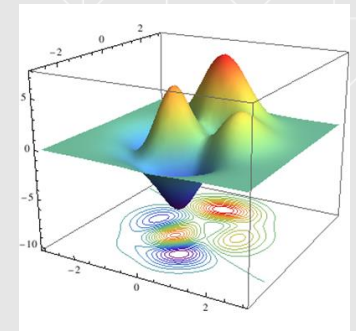
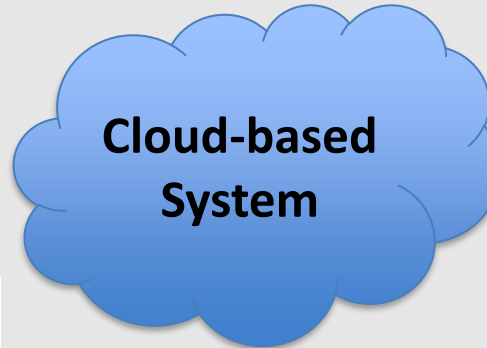
- Isothermal flow
- Plug flow
- Fast heating-cooling

EPSRC

Engineering and Physical Sciences Research Council

EP/R032807/1, Cognitive Chemical Manufacturing

Target: Pharma Applications



### Research Fellows



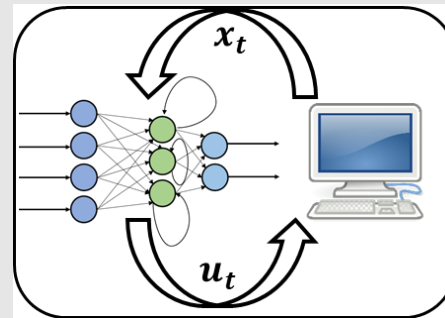
Emmanuel Agunloye



Panagiotis Petsagkourakis

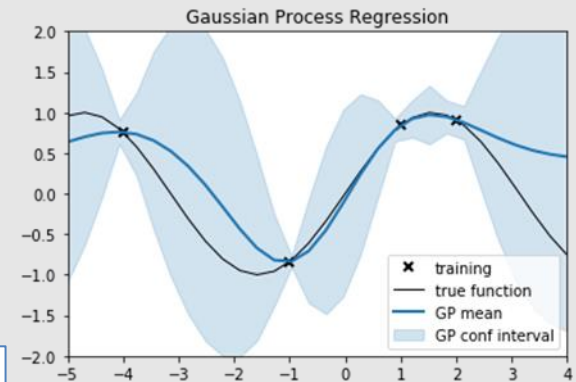


Richard Bourne (PI)



### Identification of kinetic models

- Mechanistic modelling
- Hybrid modelling<sup>1</sup>

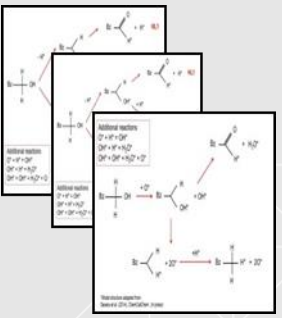


<sup>1</sup>Petsagkourakis, P., Galvanin, F. (2021). Safe model-based design of experiments using Gaussian processes, *Computers and Chemical Engineering*, 107339.

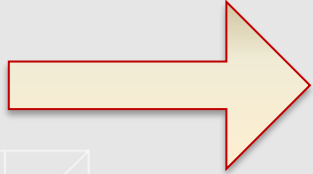
# Introduction

Modelling complex reaction systems: problem definition

**Chemistry-  
Surface Science**



Potential kinetic mechanisms



**Formulation of alternative kinetic models**

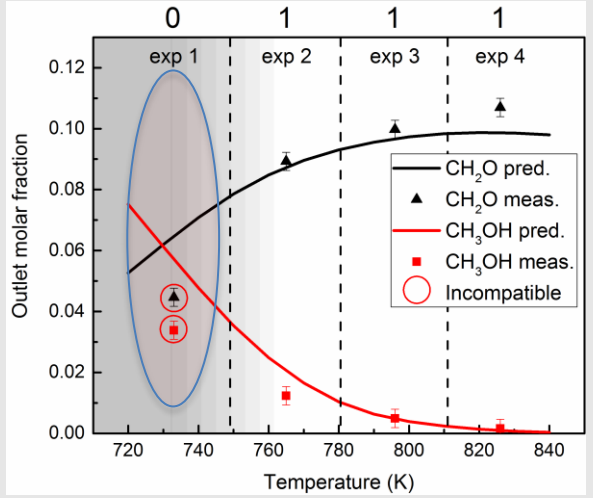
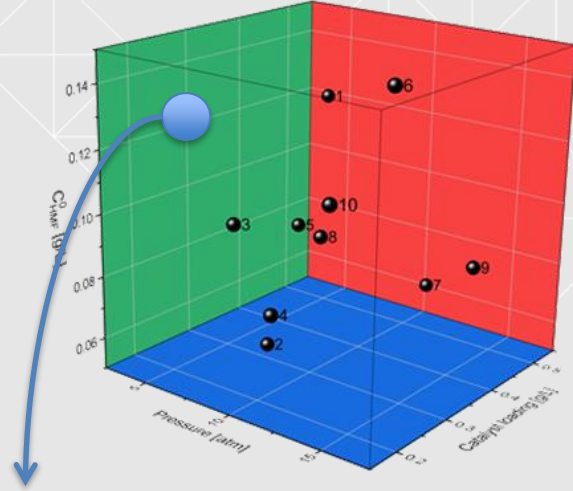
Kinetic model identification

**Reactor Model**

**Reliable phenomenological process model**

## Model requirements

- Adequate to represent the physical system
- Minimum variance of prediction(s) in the range of expected utilisation
- Robustness in unexplored regions of the design space



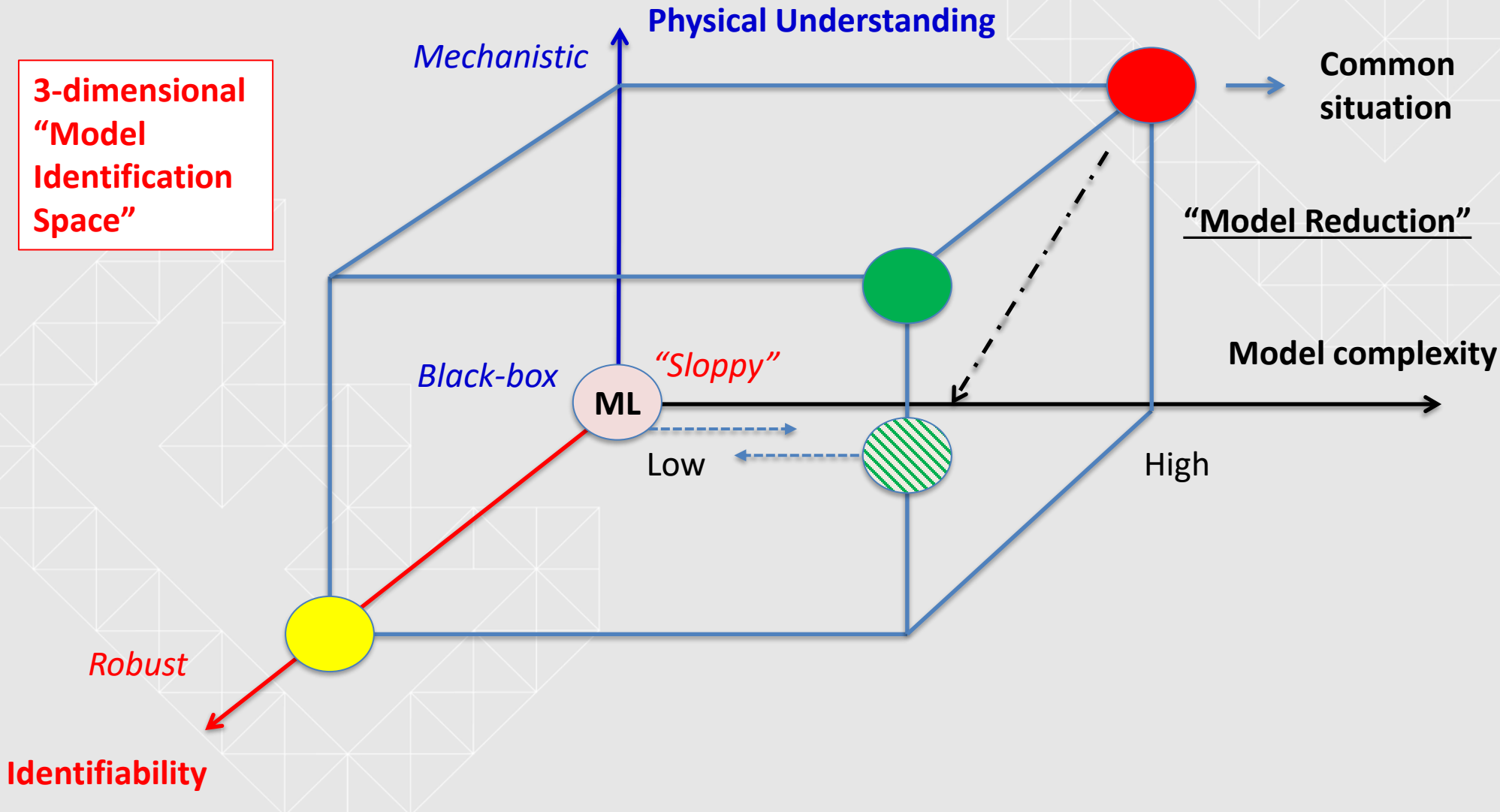


# Modelling complex reaction systems

The three dimensions of model identification

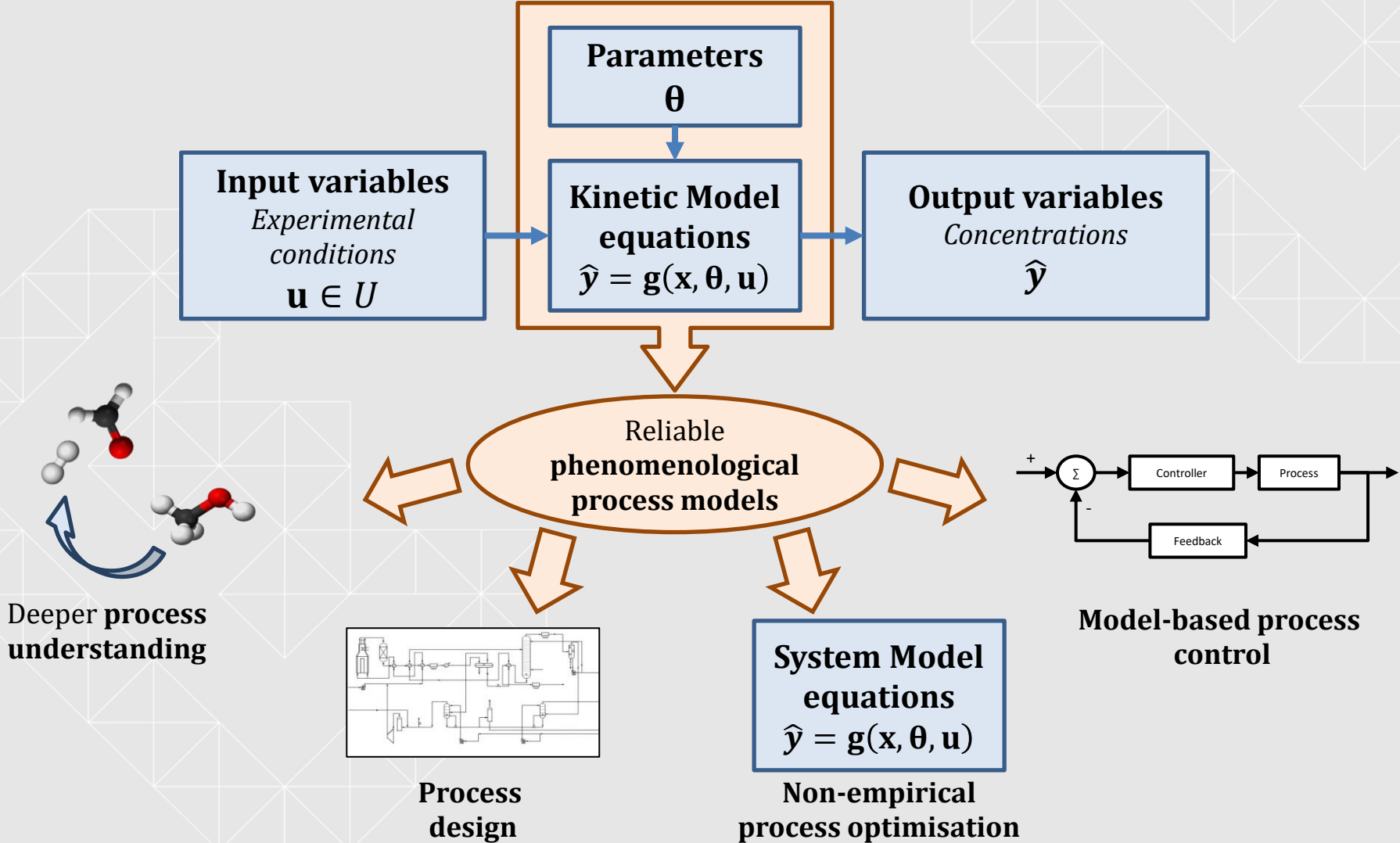


3-dimensional  
"Model  
Identification  
Space"



# Introduction

The mathematical problem: identification of parametric models

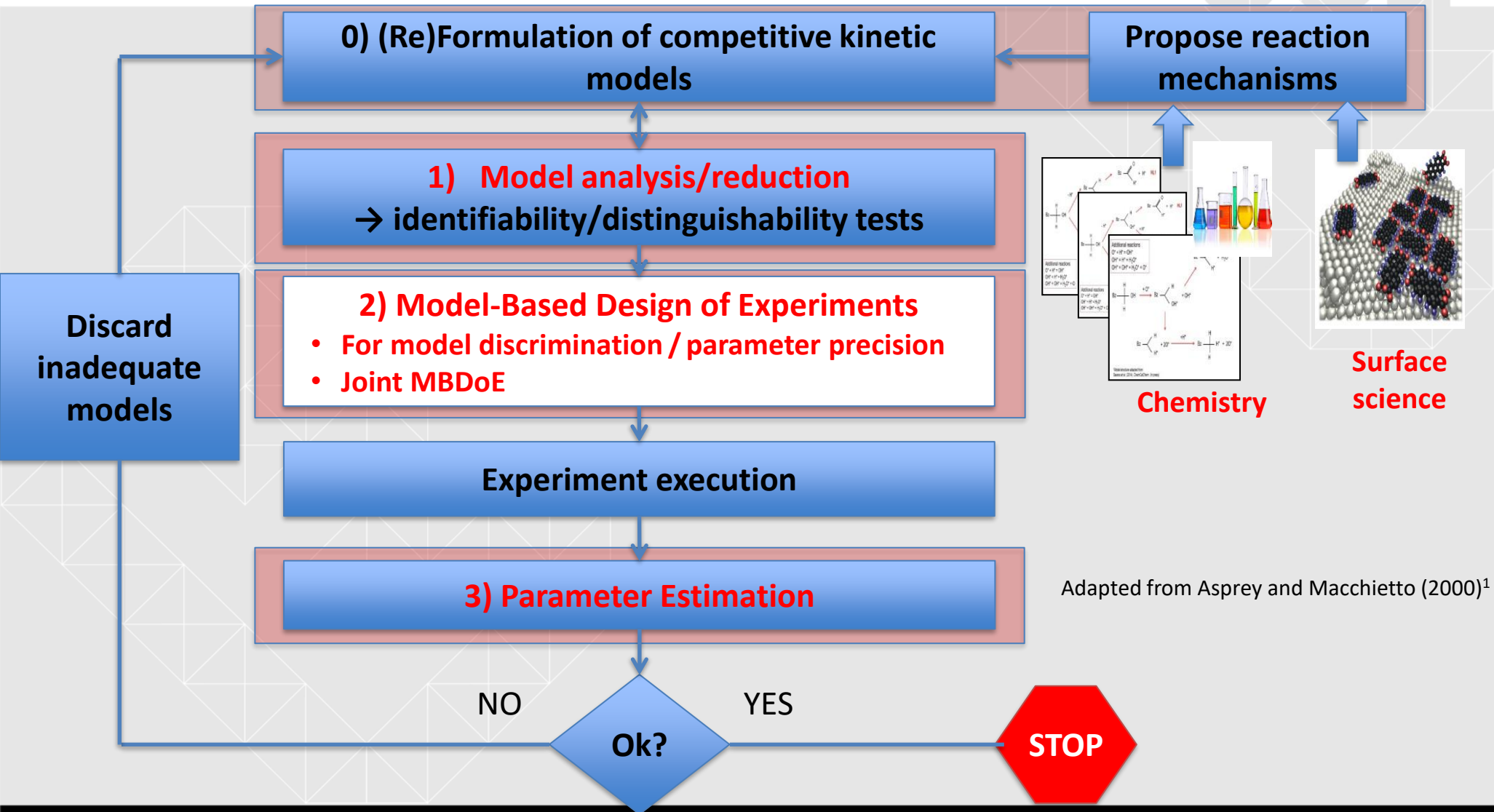


# Introduction

*Kinetic model identification procedures: key steps and bottlenecks*



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<sup>1</sup> Asprey, S. P., Macchietto, S. (2000), Statistical tools for optimal dynamic model building, Computers & Chemical Engineering, 24, 1261.

# Autonomous platforms for kinetic model identification

## Key elements of Autonomous Reaction Platforms

### • Model identification software

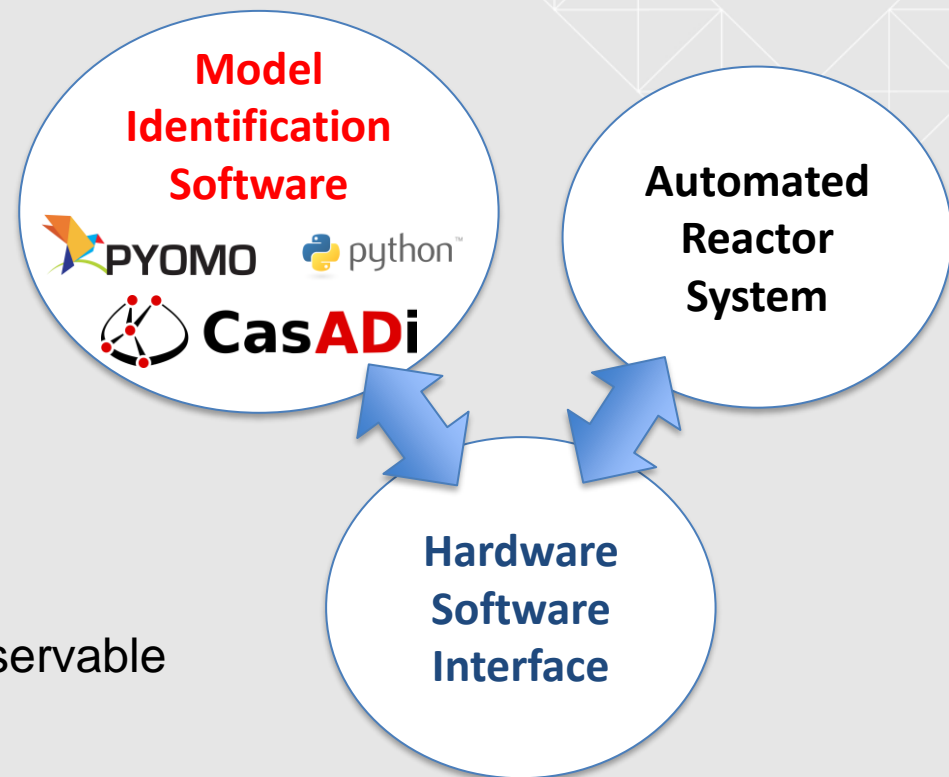
- DoE/Factorial design/User defined experiments -> Screening module
- Model-based design of experiments for model discrimination (MBDoe-MD)<sup>1</sup>
- Model-based design of experiments for parameter precision (MBDoe-PE)<sup>2</sup>
- Joint design (j-MBDoe)<sup>3</sup>
- Online model reparametrisation<sup>4</sup>
- Robust parameter estimation

### • Hardware/Software interface

- Establishing communication protocols
- Python-LabView-Devices integration

### • Automated reactor system

- Reactor design
- Safe/reliable operation
- Experiments must be reproducible and observable
- Measurement/control system



<sup>1</sup>Waldron, C; et al. (2019), React. Chem. Eng., 4, 1623.

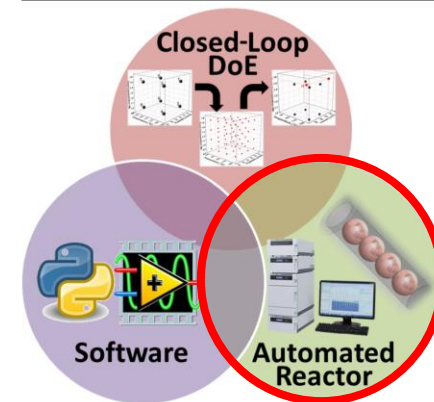
<sup>2</sup>Waldron, C et al. (2019). Ind. Eng. Chem Res. , 58 (49) 22165.

<sup>3</sup>Galvanin, F. et al. (2016), Computers & Chemical Engineering , 61, 5791.

<sup>4</sup>Quaglio, M et al. (2019) ,Computers & Chemical Engineering , 124, 270.

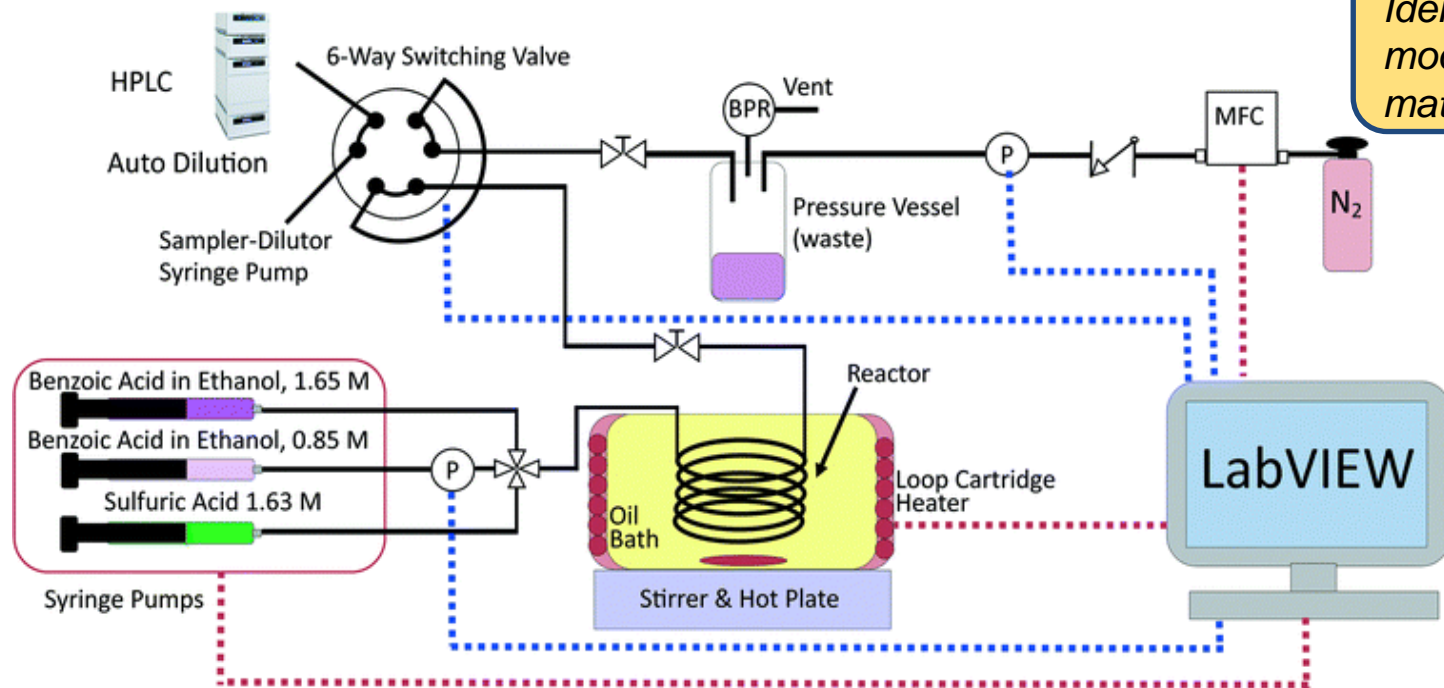
# Autonomous platforms for kinetic model identification

Framework example<sup>1,2</sup>



Automated reactor → **Autonomous (self-optimising) reactor**

**Goal**  
Identification of reliable kinetic models with minimum time, materials and effort



**Model Identification Algorithms**



<sup>1</sup>Waldron C., Pankajakshan A., Quaglio M., Cao E., Galvanin F., Gavriilidis A. (2019), *An autonomous microreactor platform for the rapid identification of kinetic models*, Reaction Chemistry & Engineering, 4, 1623-1636.

<sup>2</sup>Quaglio M., Waldron C., Pankajakshan A., Cao E., Gavriilidis A., Fraga E. S., Galvanin F. (2019), *An online reparametrisation approach for robust parameter estimation in automated model identification platforms*, Computers & Chemical Engineering, 124, 270-284.

# Standard MBDoe techniques

MBDoE-MD: Optimal Design for Model Discrimination



## Example of MBDoe-MD criterion<sup>1</sup>

maximize  $T_{ij}(\boldsymbol{\varphi})$  → “Discriminating power”

$$= \left[ \hat{\mathbf{y}}(\boldsymbol{\varphi}, \hat{\boldsymbol{\theta}}_i) - \hat{\mathbf{y}}(\boldsymbol{\varphi}, \hat{\boldsymbol{\theta}}_j) \right]^T \mathbf{V}_{ij}^{-1}(\boldsymbol{\varphi}) \left[ \hat{\mathbf{y}}(\boldsymbol{\varphi}, \hat{\boldsymbol{\theta}}_i) - \hat{\mathbf{y}}(\boldsymbol{\varphi}, \hat{\boldsymbol{\theta}}_j) \right]$$

Operating conditions optimised online to maximise the divergence between model predictions

**Different criteria for model discrimination** are integrated in the software

### Design vector

$$\boldsymbol{\varphi} = [\mathbf{y}_0, \mathbf{u}, \mathbf{t}^{sp}, \mathbf{z}^{sp}, \tau]^T$$

- $\mathbf{y}_0$  set of initial conditions on the measured variables ( $C_i$ )
- $\mathbf{u}$  set of manipulated inputs ( $T, P, F$ )
- $\mathbf{t}^{sp}$  set of time instants at which the measured variables are sampled
- $\mathbf{z}^{sp}$  set of time instants at which the measured variables are sampled
- $\tau$  the experiment duration (possibly)

<sup>1</sup>Buzzi-Ferraris G, Forzatti P. (1983), A new sequential experimental design procedure for discriminating among rival models. Chemical Engineering Science, 1, 38, 225.

# Standard MBDoe techniques

MBDoE-PE: Optimal Design for Improving Parameter Precision



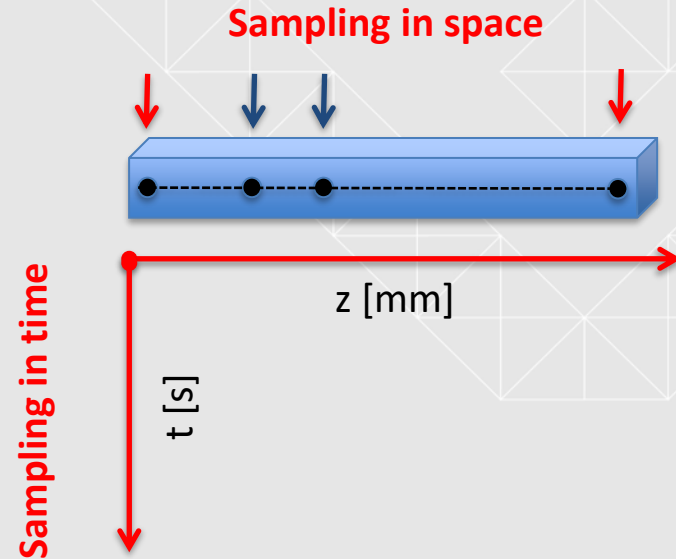
## MBDoE formulation for flow reactor systems

### Fisher information matrix (FIM)

$$\mathbf{H}_\theta(\boldsymbol{\theta}, \boldsymbol{\varphi}) = \mathbf{H}_\theta^0 + \sum_{k=1}^{n_{sp}} \sum_{i=1}^{N_y} \sum_{j=1}^{N_y} s_{ij} \begin{bmatrix} \frac{\partial \hat{y}_i(z_k, t_k)}{\partial \theta_l} & \frac{\partial \hat{y}_j(z_k, t_k)}{\partial \theta_m} \end{bmatrix}_{l,m=1 \dots N_\theta}$$

INFO from spatial domain

INFO from time domain



### Optimal design for improving parameter estimation

$$\boldsymbol{\varphi}^{PE} = \arg \min_{\boldsymbol{\varphi} \in D} \{ \psi[\mathbf{V}_\theta(\boldsymbol{\theta}, \boldsymbol{\varphi})] \} = \arg \min_{\boldsymbol{\varphi} \in D} \{ \psi[\mathbf{H}_\theta^{-1}(\boldsymbol{\theta}, \boldsymbol{\varphi})] \}$$

MBDoE-PE criterion (A, D, E, ...)

### Design vector

$$\boldsymbol{\varphi} = [\mathbf{y}_0, \mathbf{u}, \mathbf{t}^{sp}, \mathbf{z}^{sp}, \tau]^T$$

- $\mathbf{y}_0$  set of initial conditions on the measured variables ( $C_i$ )
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- $\tau$  the experiment duration (possibly)

# Advanced MBDoe techniques

## Joint Model-based Design of Experiments (j-MBDoe)<sup>1</sup>

### Multi-objective MBDoe formulation (MBDoe-MD/MBDoe-PE)

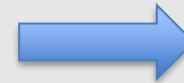
- Optimal design for discriminating between  $N_M$  competing kinetic models<sup>2</sup>
- Optimal design for improving the estimation of kinetic parameters<sup>3</sup>

j-MBDoe

$$\boldsymbol{\varphi}^{\text{MD}} = \arg \max_{\boldsymbol{\varphi} \in D} \{\Psi^{\text{MD}}\} = \arg \max_{\boldsymbol{\varphi} \in D} \left\{ \sum_{M,N=1}^{N_M} P_M P_N \left[ \sum_{i=1}^{N_y} \frac{(\hat{y}_{M,i} - \hat{y}_{N,i})^2}{\sigma_{y,i}^2} \right]_{M,N} \right\}$$

$$\Psi^{\text{PE}} = \sum_{j=1}^{N_M} \|\mathbf{H}_j\| / N_M \leq \varepsilon$$

st  $\varepsilon^{\text{MIN}} \leq \varepsilon \leq \varepsilon^{\text{MAX}}$  "ε-constraint method"



Design of experimental conditions providing the **greatest difference between model predictions**



... ensuring at the same time the best possible **reduction of parametric uncertainty**

**MBDoe for model discrimination**

**MBDoe for improving parameter estimation**

$P_i$  = probability of the  $i$ -th model to be the "true" model  
 $\hat{y}_{ji}$  =  $i$ -th predicted response of the  $j$ -th model

<sup>1</sup>Galvanin, F. et al. (2016), Comp. Chem. Eng, 61, 5791-5806

<sup>2</sup>Schwaab, M. et al. (2006), Chem. Eng. Sci., 61, 5791-5806

<sup>3</sup>Reizman, B. J., Jensen, K. F. (2012), Org. Process Des. Dev., 16, 1770-1782



# Advanced MBDoe techniques

## Explorative MBDoe based on G-optimality maps<sup>1</sup>

### Challenges:

- MBDoe algorithms tend to be “**greedy**”  
→ only highly informative regions of the design space are mapped in the online optimization
- Can we formulate an optimal experimental design problem allowing **agile experimental design space exploration?**



Francesca Cenci



Pierantonio Facco



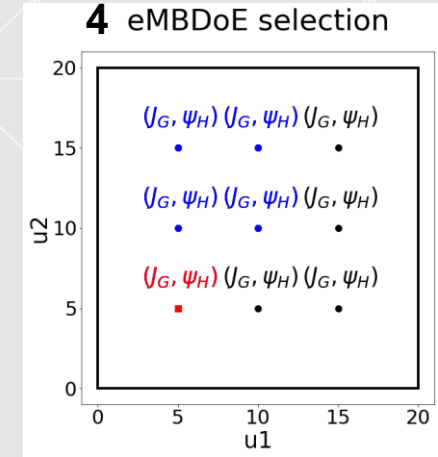
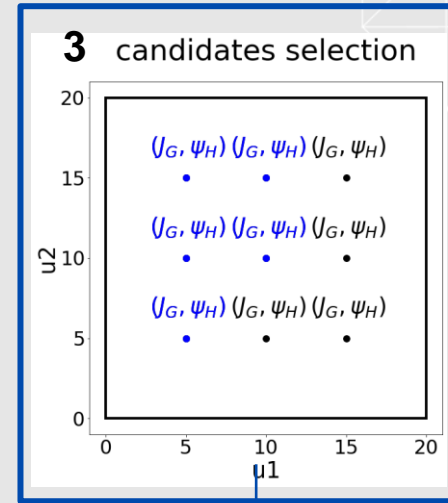
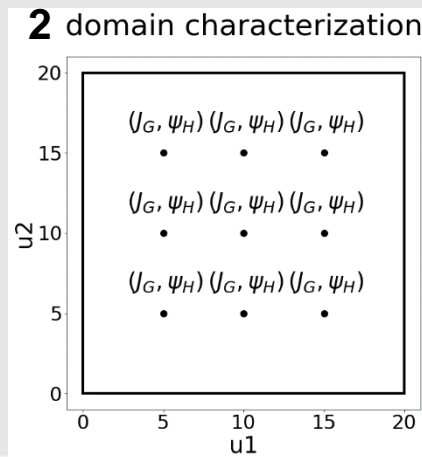
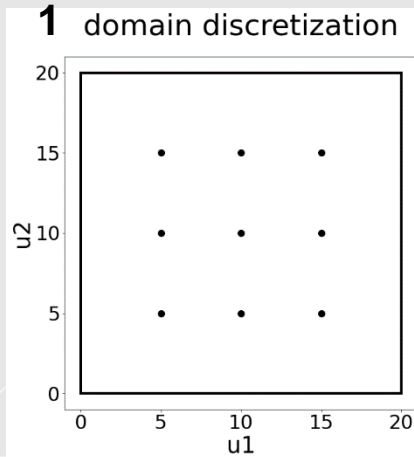
*Potential solution*

Explorative MBDoe based on G-optimality maps (***G-map eMBDoE***)

<sup>1</sup>Cenci, F., Pankajakshan, A., Galvanin, F. (2023), An exploratory model-based design of experiments approach to aid parameters identification and reduce model prediction uncertainty, Computers & Chemical Engineering, 177, 108353, <https://doi.org/10.1016/j.compchemeng.2023.108353>

# Advanced MBDoe techniques

## Explorative MBDoe based on G-optimality maps<sup>1</sup>



### ► Explorative MBDoe based on G-optimality maps (*G-map eMBDoE*)

- **Step 3:** eMBDoE first discriminates points based on a **G-optimality threshold**  $J_G = \sum_{i=1}^{N_y} V_{y,i}$

$$J_G \geq J_{G,\text{thr}} J_{G,\text{max}}$$

$N_y$  number of response variables

$\psi_H$  scalar measure of FIM

- **Step 4:** Then, the experiment with the highest amount of information based on MBDoe-PE design criteria is selected

<sup>1</sup>Cenci, F., Bawa, S., Gavriilidis, A., Facco, P., Galvanin, F. (2023), An exploratory model-based design of experiments technique to aid parameters identification and reduce prediction uncertainty, Computer-Aided Chemical Engineering, 1-6.

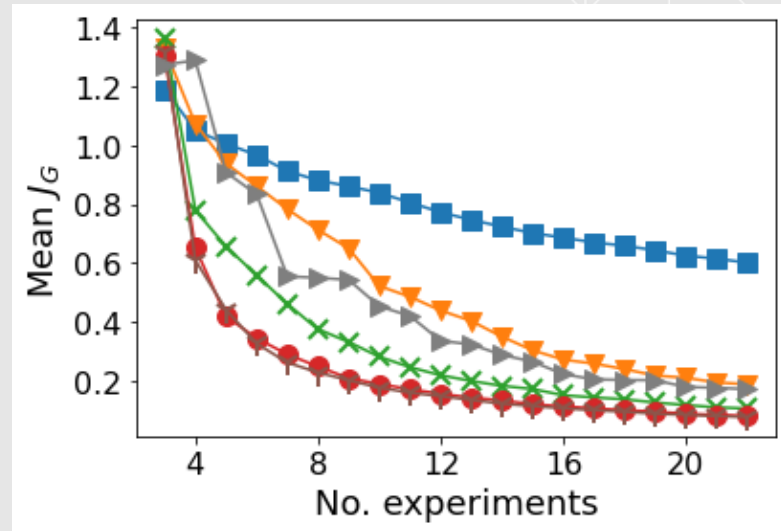
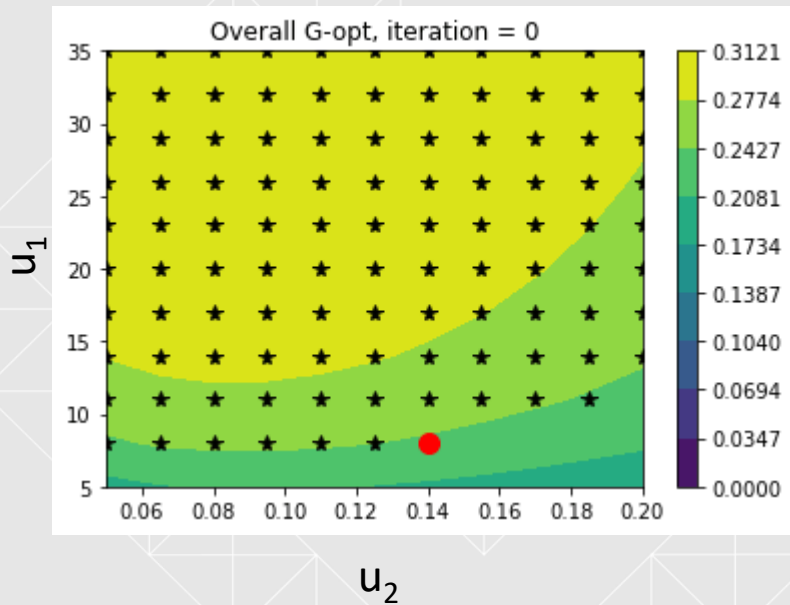
# Advanced MBDoe techniques

Explorative MBDoe based on G-optimality maps<sup>1</sup>



## G-map eMBDoe Settings

- $J_{G,thr} = 0.75$
- D-optimal experimental design

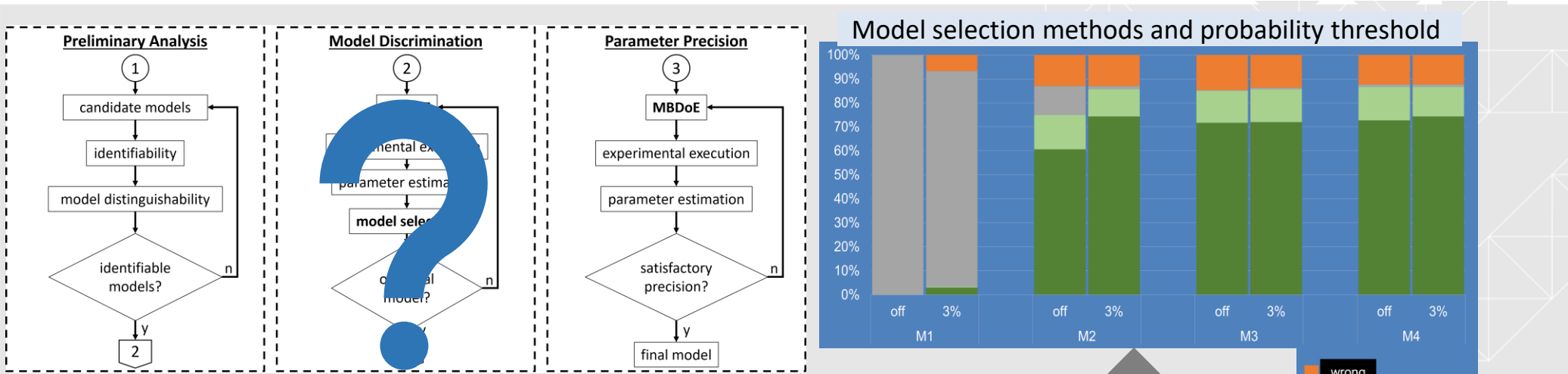


- Efficient reduction of prediction uncertainty in the design space compared to MBDOE and DoE
- Satisfactory estimation of the full set of model parameters, thanks to the MBDoe step 4
- Methods have been developed to automatically adjust the G-optimality threshold

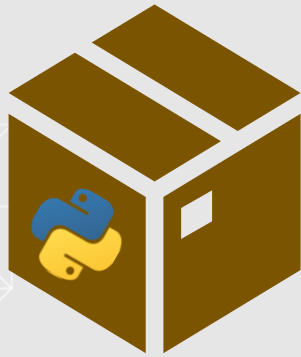
<sup>1</sup>Cenci, F., Bawa, S., Gavriilidis, A., Facco, P., Galvanin, F. (2023), An exploratory model-based design of experiments technique to aid parameters identification and reduce prediction uncertainty, Computer-Aided Chemical Engineering, 1-6.

# Advanced MBDoe techniques

Development of a holistic Python package for optimal selection of experimental design criteria<sup>1</sup>



→ MBDoe-MD: first step towards optimal selection of MBDoe settings



Maerthe Theresa Tillmann, MSc



- Computational tool for Holistic Model Identification (**HoliMI**<sup>2</sup>)
- Different model selection/MBDoe-MD criteria implemented

<sup>1</sup>Tillmann, M. T., Galvanin, F. (2023), Development of a holistic Python package for optimal selection of experimental design criteria in kinetic model discrimination, Computer-Aided Chemical Engineering, 631-636.

<sup>2</sup> <https://github.com/mtt9/HoliMI>

# Case study 1

## Benzoic acid esterification in a capillary microreactor



Benzoic Acid Esterification with Ethanol using Sulfuric Acid (homogeneous)

- Liquid phase reaction
- PTFE capillary reactor
- Online HPLC as measurement system

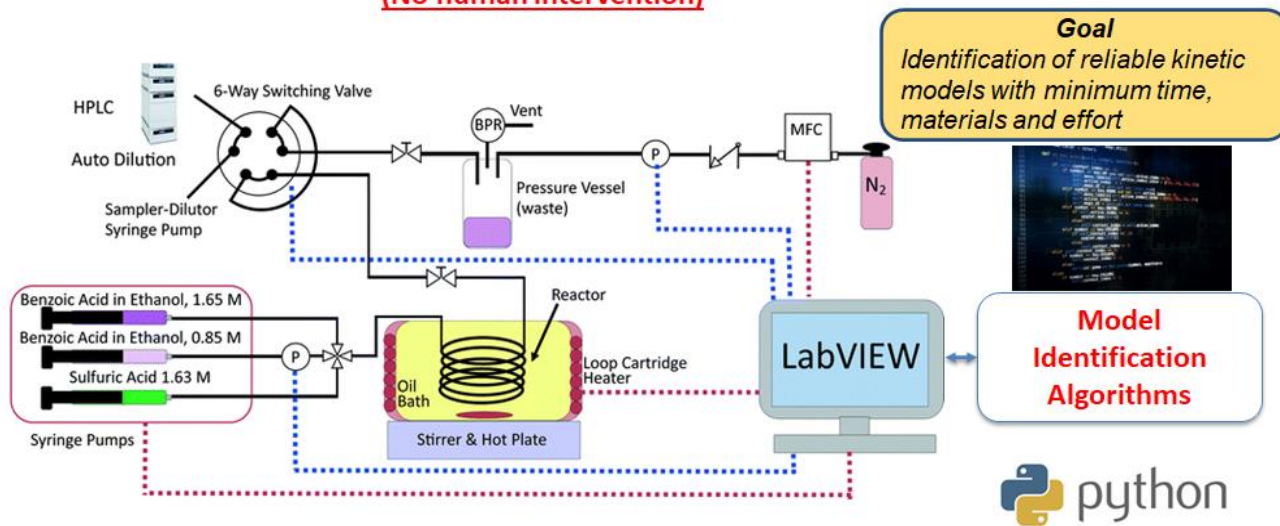
### Objective

- Identify a kinetic model from a sequence of steady state flow experiments

Data fitting results for **two candidate kinetic models** using two identical preliminary steady-state factorial campaigns

Model	$\chi^2$ ( $\chi_{\text{ref}}^2 = 43.7$ )	Result
$r = kC_{\text{BA}}$	16.2	Possible model
$r = kC_{\text{BA}}^2$	156	Reject model

Automated reactor → **Autonomous (self-optimising) reactor**  
(No human intervention)



Design vector in MBDoE

$$\boldsymbol{\varphi} = [T, F, c_{\text{IN}, i}]$$

- Temperature
- Flowrate
- Concentration of benzoic acid in the feed

<sup>1</sup>Waldron, C; Pankajakshan, A; Quaglio, M; Cao, E; Galvanin, F; Gavriilidis, A. (2019) An autonomous microreactor platform for the rapid identification of kinetic models. *Reaction Chemistry and Engineering* 4, 1623. [10.1039/C8RE00345A](https://doi.org/10.1039/C8RE00345A).

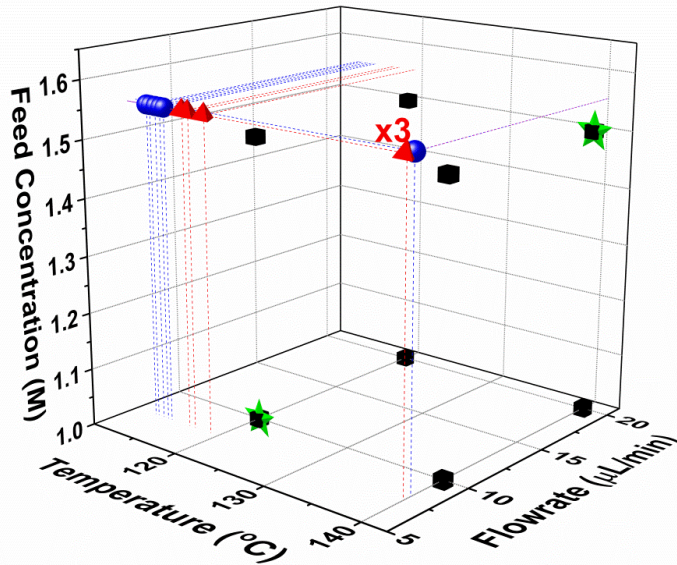
# Case study 1: Benzoic acid esterification in a capillary microreactor

*MBD<sub>oE</sub> VS DoE<sup>1</sup>*

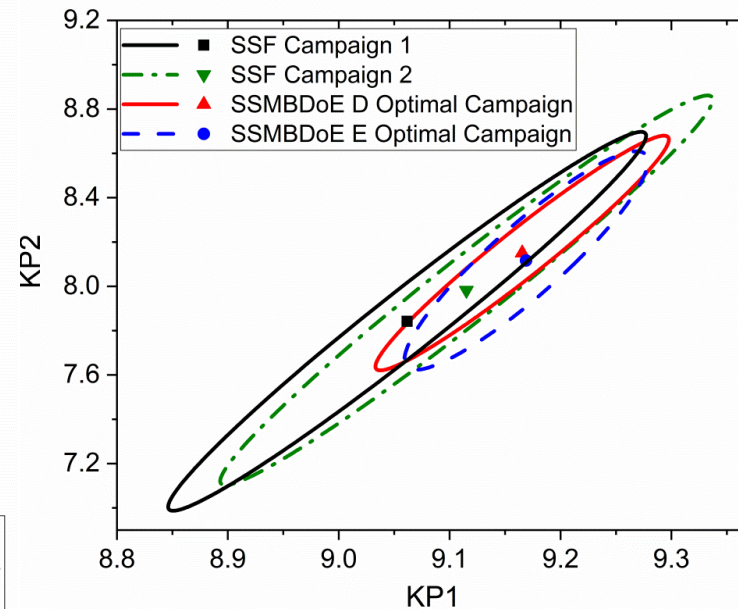
## Steady-State Factorial (SSF) Vs Steady-State MBD<sub>oE</sub> (SSMBD<sub>oE</sub>) campaigns

Uncertainty of parameters KP1 and KP2 for the Steady-State Factorial (SSF) and Steady-State MBD<sub>oE</sub> (SSMBD<sub>oE</sub>) D- and E- optimal campaigns

$$\tau_{BzAcid} = -kC_{BzAcid} \quad k = \exp\left(-KP1 - \frac{KP2 * 10000}{R} * \left[\frac{1}{T} - \frac{1}{T_M}\right]\right)$$



- SSF Campaigns (1 & 2)
- ★ First 2 Experiments Chosen by the User to Initialise SSMBD<sub>oE</sub> Campaigns
- ▲ 6 Experiments Designed by SSMBD<sub>oE</sub> D Optimal Campaign
- 6 Experiments Designed by SSMBD<sub>oE</sub> E Optimal Campaign



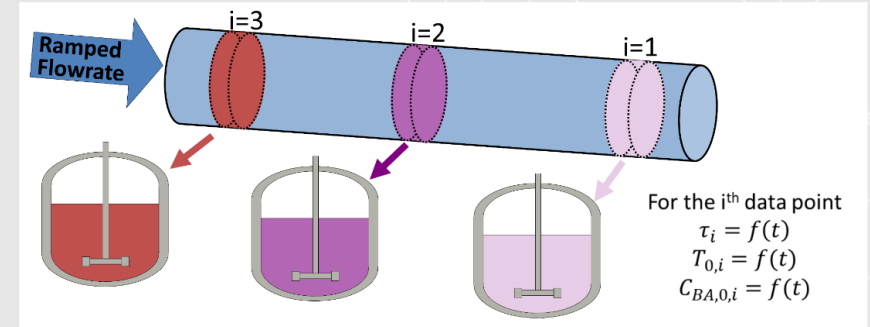
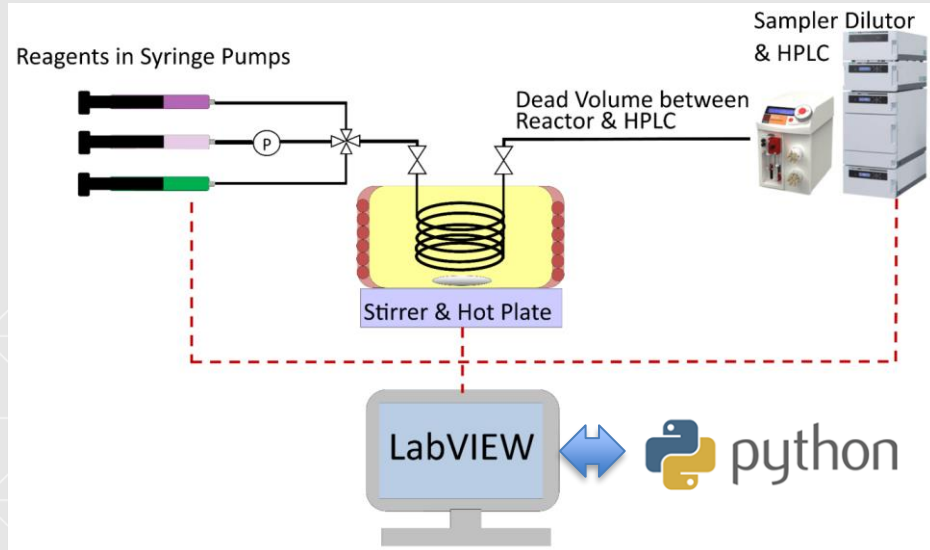
- Steady-state MBD<sub>oE</sub> experiments produced **significantly smaller uncertainty regions** than the ones designed by a full factorial DoE using the **same number of steady-state experiments**

<sup>1</sup>Waldron, C; Pankajakshan, A; Quaglio, M; Cao, E; Galvanin, F; Gavriilidis, A. (2019) An autonomous microreactor platform for the rapid identification of kinetic models. *Reaction Chemistry and Engineering* 4, 1623. [10.1039/C8RE00345A](https://doi.org/10.1039/C8RE00345A).

# Case study 1: Benzoic acid esterification in a capillary microreactor

## Optimal design of transient flow experiments

### Optimal design of transient flow experiments for the Identification of kinetic parameters<sup>1</sup>



$$\frac{dC_{BA,i}}{d\tau} = r_{BA,i} \quad \text{for } i = 1, \dots, N_{sp}$$

$$\frac{dT_i}{d\tau} = -\alpha_T \quad \text{for } i = 1, \dots, N_{sp}$$

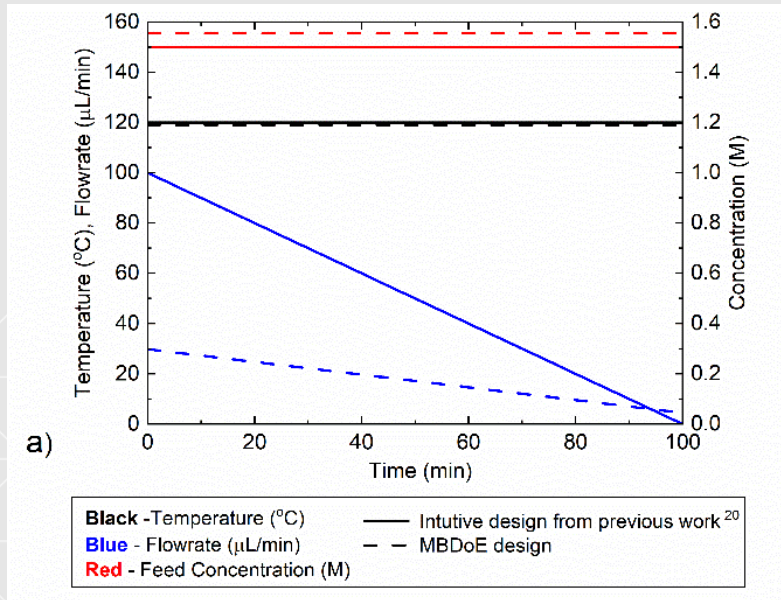
- The transient PFR can be described by a **system of ideal batch reactors**
- Dead volume between end of reactor and sampling needs to be known
- Transient experiments can provide **faster estimation of kinetic parameters**
- **Design vector for MBDoe:**  $\boldsymbol{\varphi} = [T, F, c_{\text{IN, BA}}, \boldsymbol{\alpha}_T, \boldsymbol{\alpha}_V, \boldsymbol{\alpha}_C]$

<sup>1</sup>Waldron, C; Pankajakshan, A; Quaglio, M; Cao, E; Galvanin, F; Gavriilidis, A; (2020) Model-based design of transient flow experiments for the identification of kinetic parameters. *Reaction Chemistry & Engineering*, 5, 112. [10.1039/c9re00342h](https://doi.org/10.1039/c9re00342h).

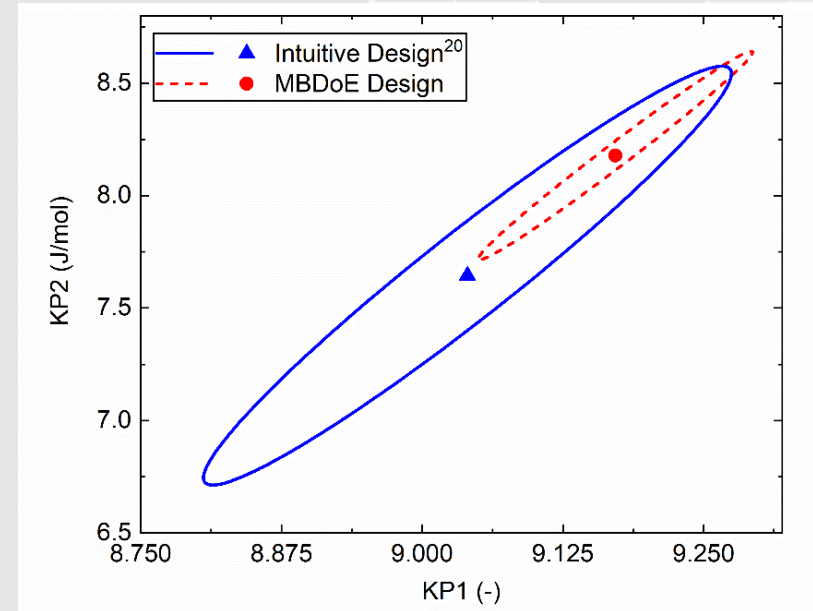
# Case study 1: Benzoic acid esterification in a capillary microreactor

## Optimal design of transient flow experiments<sup>1</sup>

Control variable profiles (temperature, flowrate and benzoic acid inlet concentration) designed **intuitively** and by **MBDDoE**



Confidence ellipsoids of kinetic parameters for transient experiments designed intuitively and by MBDDoE



- **MBDDoE improves significantly the parameter precision obtained from transient experiments**
- Parameter precision obtained in transient from a **single run**:
  - similar to that obtained from **8 steady-state MBDDoE runs**<sup>1</sup>
- ... transient experiments required significantly less time and resources to run!

<sup>1</sup>Waldron, C; Pankajakshan, A; Quaglio, M; Cao, E; Galvanin, F; Gavriilidis, A; (2020) Model-based design of transient flow experiments for the identification of kinetic parameters. *Reaction Chemistry & Engineering*, 5, 112. [10.1039/c9re00342h](https://doi.org/10.1039/c9re00342h).

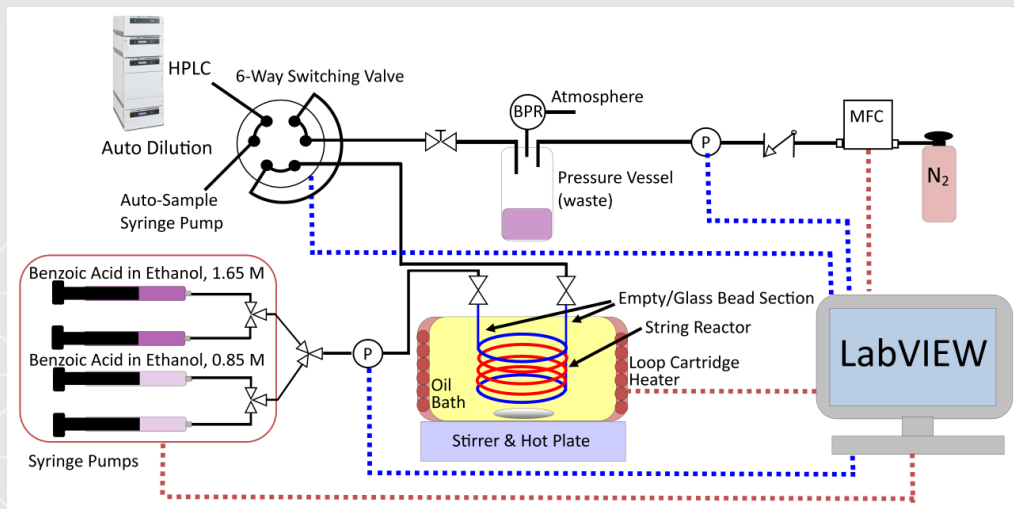


# Case study 1: Benzoic acid esterification in a capillary microreactor

## Closed-loop identification including MBD<sub>oE</sub>-MD and MBD<sub>oE</sub>-PE

### Closed Loop MBD<sub>oE</sub> for Kinetic Model Discrimination and Parameter Estimation<sup>1</sup>

#### Benzoic Acid Esterification on Amberlyst-15 (heterogeneous) with Ethanol



#### Four candidate kinetic models

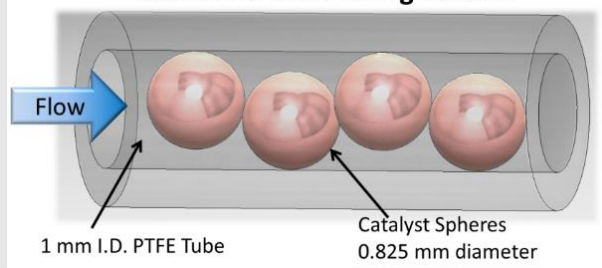
$$r'_{BA} = -kC_{BA}C_{EtOH} \quad (M1)$$

$$r'_{BA} = \frac{-kC_{BA}C_{EtOH}}{(1 + K_W C_W)^2} \quad (M2)$$

$$r'_{BA} = \frac{-kC_{BA}C_{EtOH}}{(1 + K_W C_W + K_{EtOH} C_{EtOH})^2} \quad (M3)$$

$$r'_{BA} = \frac{-kC_{BA}C_{EtOH}}{(1 + K_{BA} C_{BA} + K_{EtOH} C_{EtOH} + K_W C_W + K_{EB} C_{EB})^2} \quad (M4)$$

#### Section of Bead String Reactor



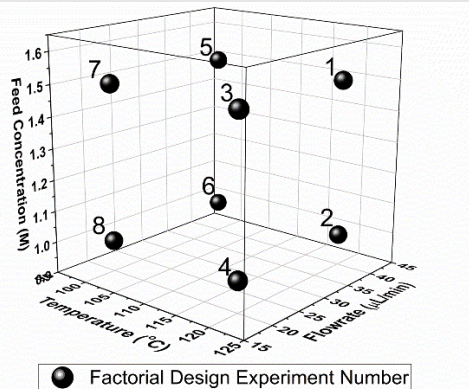
Bead-string reactor offers **small external mass transfer resistance**

<sup>1</sup>Waldron, C; Pankajakshan, A; Quaglio, M; Cao, E; Galvanin, F; Gavriilidis, A; (2019) Closed-Loop Model-Based Design of Experiments for Kinetic Model Discrimination and Parameter Estimation: Benzoic Acid Esterification on a Heterogeneous Catalyst. *Industrial & Engineering Chemistry Research*, 58, 2216. [10.1021/acs.iecr.9b04089](https://doi.org/10.1021/acs.iecr.9b04089).

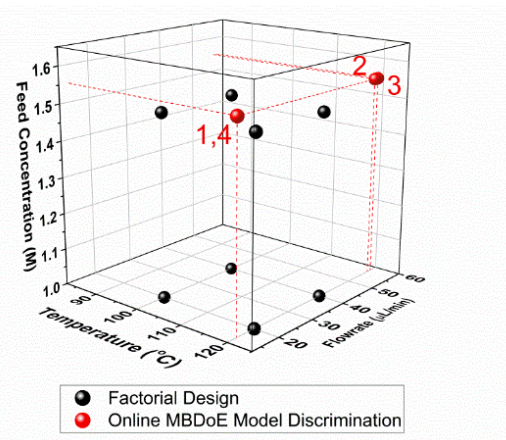
# Case study 1: Benzoic acid esterification in a capillary microreactor

## Closed-loop identification including MBDoe-MD and MBDoe-PE

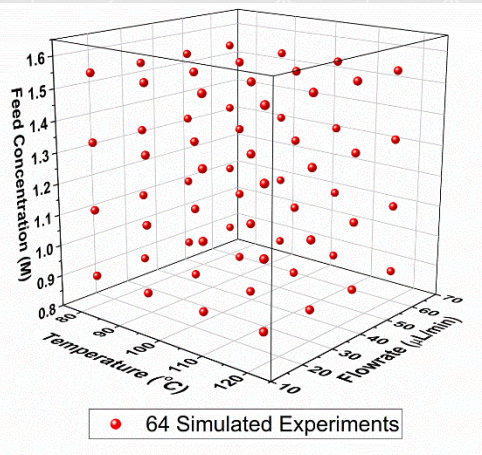
### Closed Loop MBDoe for Kinetic Model Discrimination and Parameter Estimation



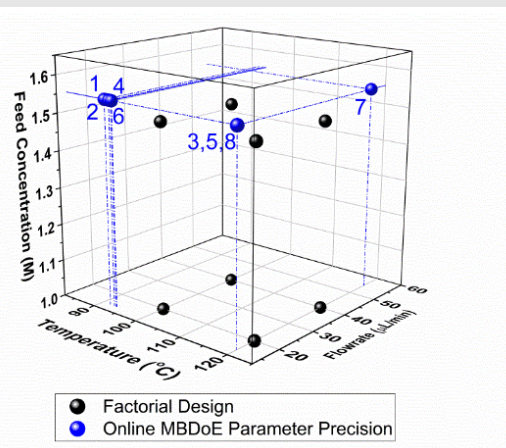
1. 8 steady-state experiments designed by a full factorial DoE method  
M1, M2, M3, M4



3. MBDoe-designed discriminating experiments (MBDoe-MD)  
M2



2. 64 simulated experiments to test practical model identifiability based on rank of FIM  
M1, M2



4. MBDoe designed experiments for improved parameter precision (MBDoe-PE)  
M2

# Case study 1: Benzoic acid esterification in a capillary microreactor

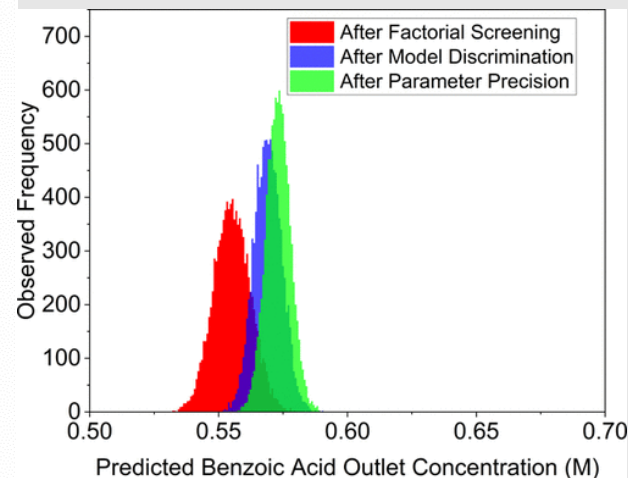
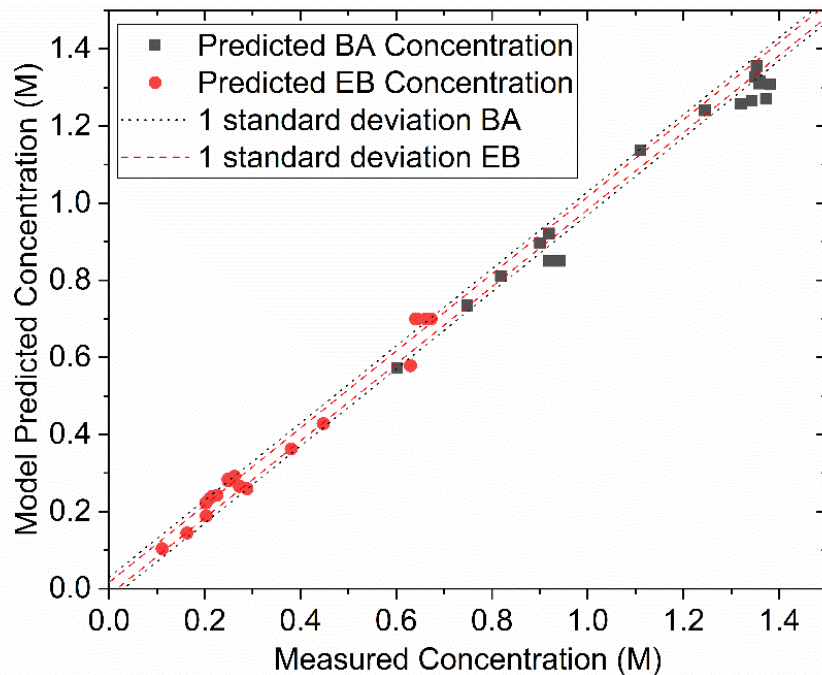
*Closed-loop identification including MBDoe-MD and MBDoe-PE*

## Identified (apparent) kinetic model (Model 2)

$$r'_{BA} = \frac{185.3 \exp\left(-\frac{68\,800}{RT}\right) \times C_{BA} C_{EtOH}}{(1 + 0.53 C_W)^2}$$

- Bead string reactor provided plug flow behaviour with efficient mass transfer
- The methodology proposed **minimized the number of experiments** required for kinetic model identification
- **It prevents the use of nonidentifiable models**
- MBDoe-MD distinguished between two candidate models
- MBDoe-PE improved parameter precision
- All kinetic experiments were **completed in 3 days**

... against **2 weeks** for a full factorial DoE!

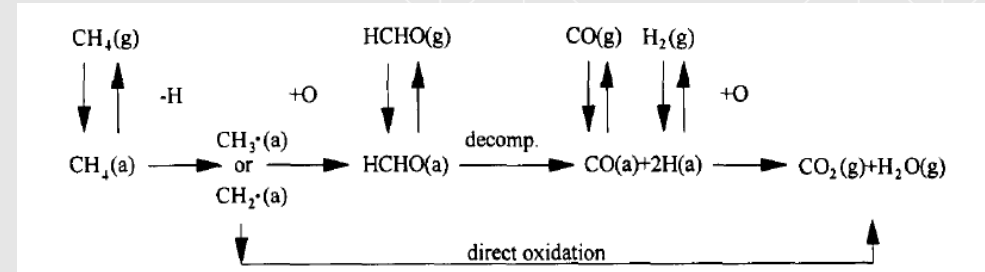
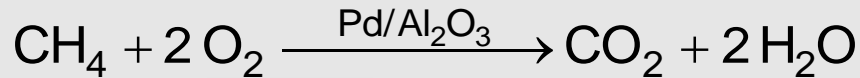


# Case study 2: Catalytic methane oxidation

## Catalytic methane oxidation in flow microreactor systems

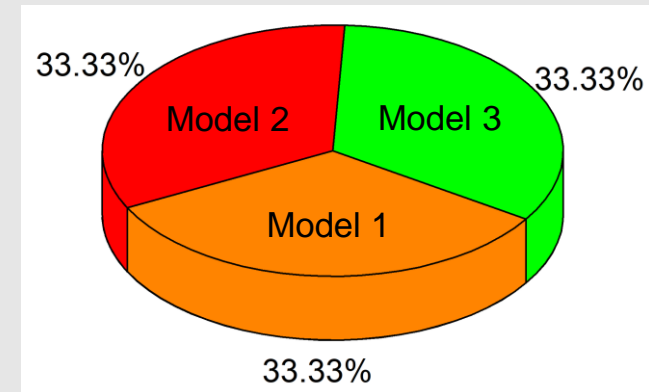


Overall chemical reaction of methane oxidation over Pd/Al<sub>2</sub>O<sub>3</sub> catalyst<sup>1</sup>:



Three candidate kinetic models are considered for the methane oxidation reaction after a screening and identifiability study based on 12 candidate models <sup>2</sup>

Model	Rate law
Model 1	$r_{\text{CH}_4} = kP_{\text{avg}}y_{\text{CH}_4}$
Model 2 (LH)	$r_{\text{CH}_4} = \frac{k_r K_{\text{CH}_4} P_{\text{CH}_4} \sqrt{K_{\text{O}_2} P_{\text{O}_2}}}{\left(1 + K_{\text{CH}_4} P_{\text{CH}_4} + \sqrt{K_{\text{O}_2} P_{\text{O}_2}}\right)^2}$
Model 3 (MVK)	$r_{\text{CH}_4} = \frac{k_1 k_2 P_{\text{CH}_4} P_{\text{O}_2}}{k_1 P_{\text{O}_2} + 2k_2 P_{\text{CH}_4} + (k_1 k_2 / k_3) P_{\text{O}_2} P_{\text{CH}_4}}$



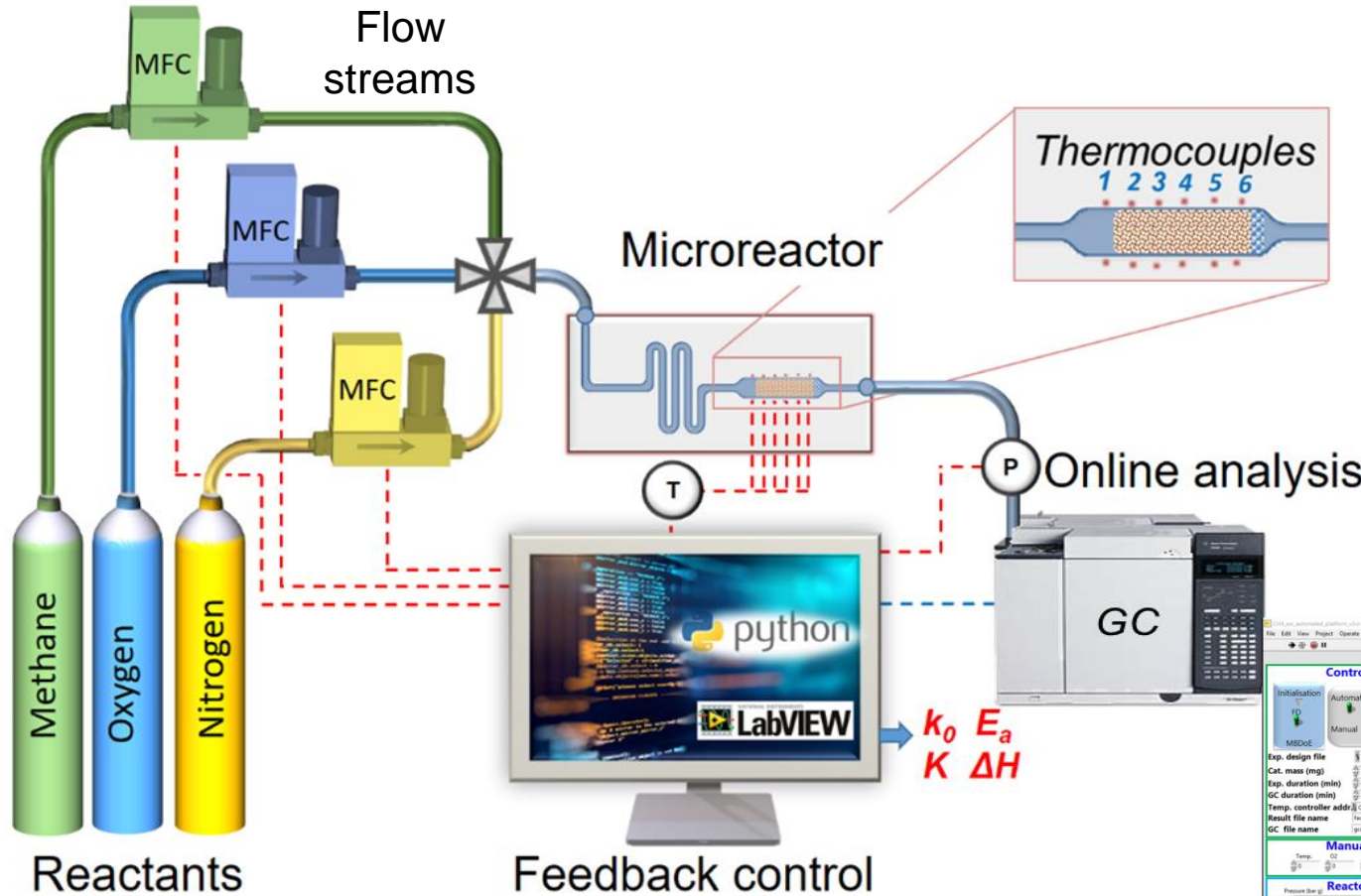
Initial probability of model correctness

<sup>1</sup>J. H. Lee, D. L. Trimm (1995), Catalytic combustion of methane, Fuel Processing Technology 42, 339.

<sup>2</sup>S. G. Bawa, A. Pankajakshan, C. Waldron, E. Cao, F. Galvanin, A. Gavriilidis (2023). Chemistry-Methods, 3, 1.

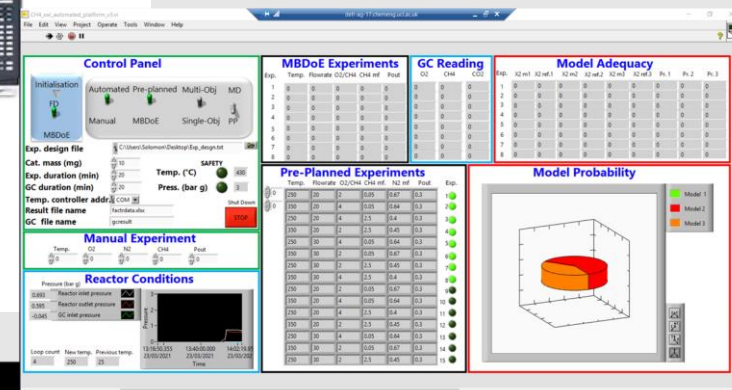
# Case study 2: catalytic methane oxidation

The platform – microreactor technology



## Reactor Setup

- Silicon-glass reactor
- 10 mg of 5 wt.% Pd/Al<sub>2</sub>O<sub>3</sub>
- $\pm 3$  °C axially at 400 °C
- Online analysis by GC



<https://www.youtube.com/watch?v=kMCtQqbPixk>

# Case study: catalytic methane oxidation

## LabView Graphical User Interface and digital twin



File Edit View Project Operate Tools Window Help

Control Panel

Initialisation  
FD  
MBDoe

Automated Pre-planned Multi-Obj MD  
Manual MBDoe Single-Obj PP

Exp. design file C:\Users\Solomon\Desktop\Exp\_desgn.txt

Cat. mass (mg) 10 SAFETY  
Exp. duration (min) 29 Temp. (°C) 430  
GC duration (min) 29 Press. (bar g) 3  
Temp. controller addr. COM Shut Down  
Result file name factrdata.xlsx  
GC file name GC20210716R STOP

Manual Experiment

Temp. O2 N2 CH4 Pout  
0 0 0 0 0

Reactor Conditions

Pressure (bar g)  
-0.77 Reactor inlet pressure  
-0.771 Reactor outlet pressure  
-0.77 GC inlet pressure

Loop count New temp. Previous temp.  
0 35.2 230

14:37:07.765 00:00:00.000 11:08:08.88  
28/07/2021 29/07/2021 29/07/2021  
Time

MBDoE Experiments

Exp.	Temp.	Flowrate	O2/CH4	y_CH4
1	0	0	0	0
2	0	0	0	0
3	0	0	0	0
4	0	0	0	0
5	0	0	0	0
6	0	0	0	0
7	0	0	0	0
8	0	0	0	0

GC Reading

O2	CH4	CO2
0	0	0
0	0	0
0	0	0
0	0	0
0	0	0
0	0	0
0	0	0
0	0	0
0	0	0
0	0	0

Model Adequacy

Exp.	X2 m1	X2 ref.1	X2 m2	X2 ref.2	X2 m3	X2 ref.3	Pr. 1	Pr. 2	Pr. 3
1	0	0	0	0	0	0	0	0	0
2	0	0	0	0	0	0	0	0	0
3	0	0	0	0	0	0	0	0	0
4	0	0	0	0	0	0	0	0	0
5	0	0	0	0	0	0	0	0	0
6	0	0	0	0	0	0	0	0	0
7	0	0	0	0	0	0	0	0	0
8	0	0	0	0	0	0	0	0	0

Pre-Planned Experiments

Temp.	Flowrate	O2/CH4	y_CH4	Exp.
0	0	0	0	1
0	0	0	0	2
0	0	0	0	3
0	0	0	0	4
0	0	0	0	5
0	0	0	0	6
0	0	0	0	7
0	0	0	0	8
0	0	0	0	9
0	0	0	0	10
0	0	0	0	11
0	0	0	0	12
0	0	0	0	13
0	0	0	0	14
0	0	0	0	15

Model Probability

Model 1  
Model 2  
Model 3

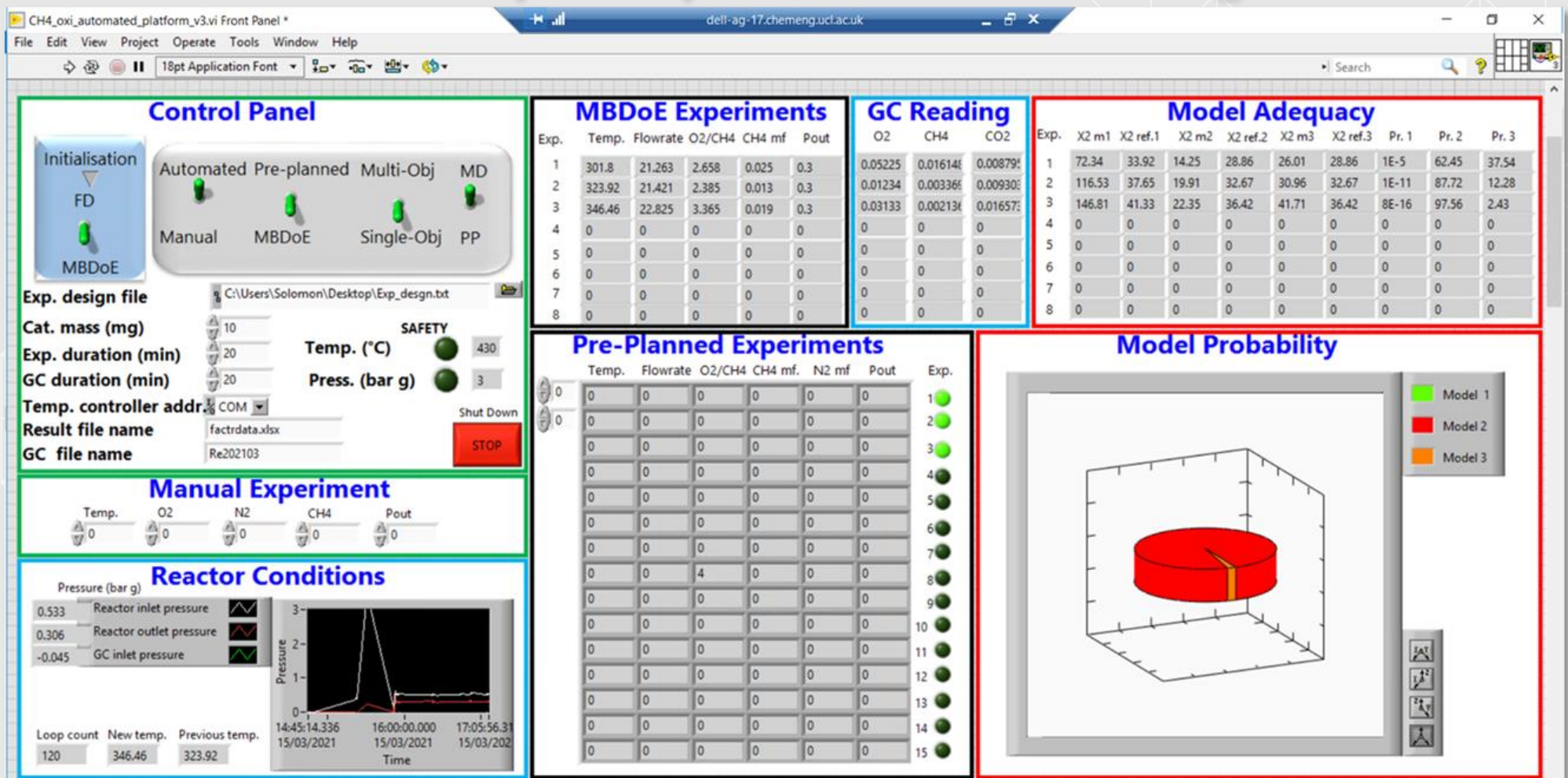
MBDoE: Model-based design of experiments MD: Model discrimination PP: Parameter precision Pr: Probability m: Model ref: Reference X2: Chi-square

# Case study: catalytic methane oxidation

LabView Graphical User Interface and digital twin



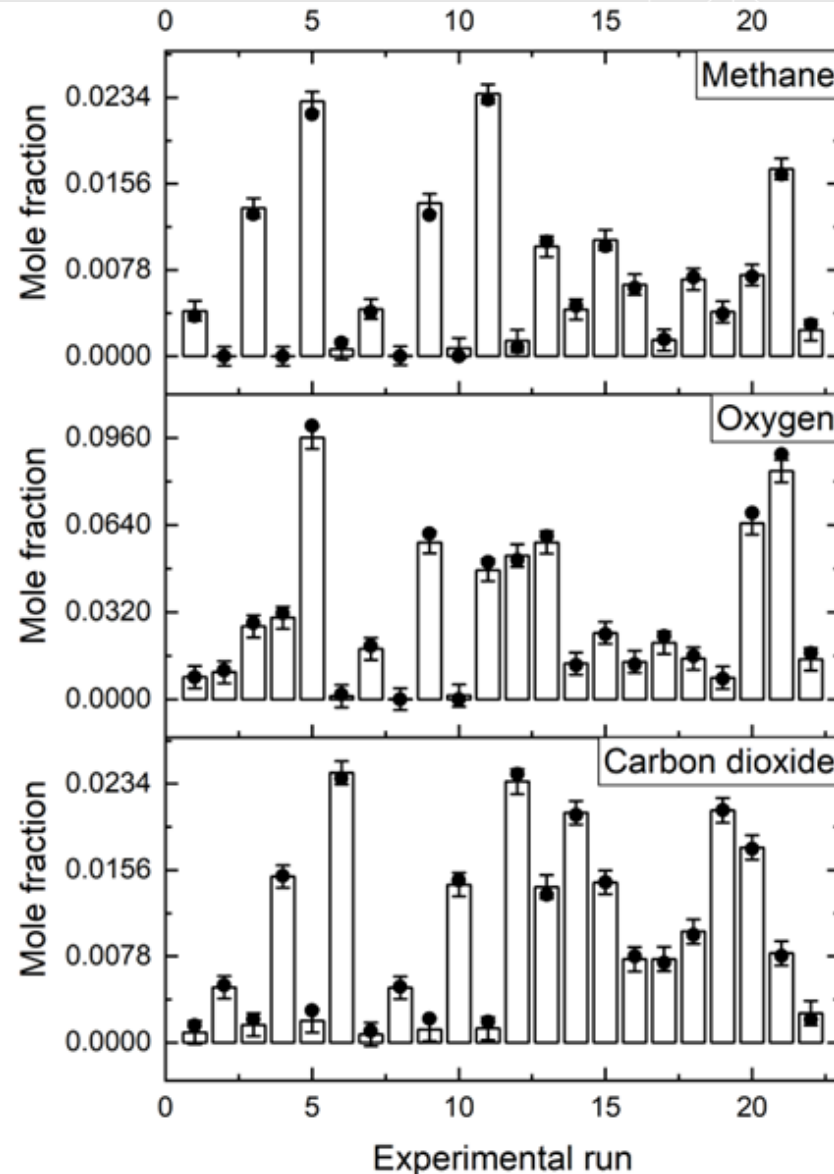
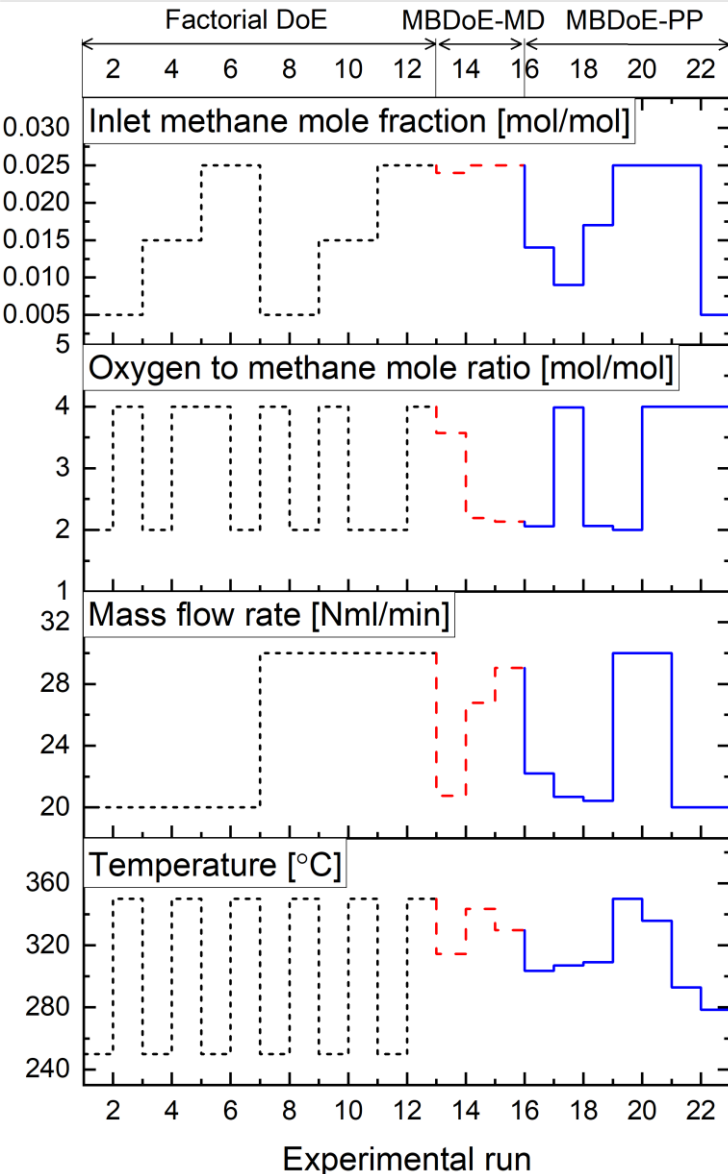
## Probability not to reject kinetic model after MBDoe\_3



<https://www.youtube.com/watch?v=kMCtQqbPixk>

# Case study: catalytic methane oxidation

Results from the autonomous platform: inputs/outputs



## Campaign for kinetic model validation:

1. Preliminary set of DoE experiments for pre-screening
2. MBDoE-MD runs
3. MBDoE-PE runs



- Switch between steps 2) and 3) dictated by the **best model probability (>95%)**
- **STOP** when parameters are all precisely estimated (**t-test satisfied**)

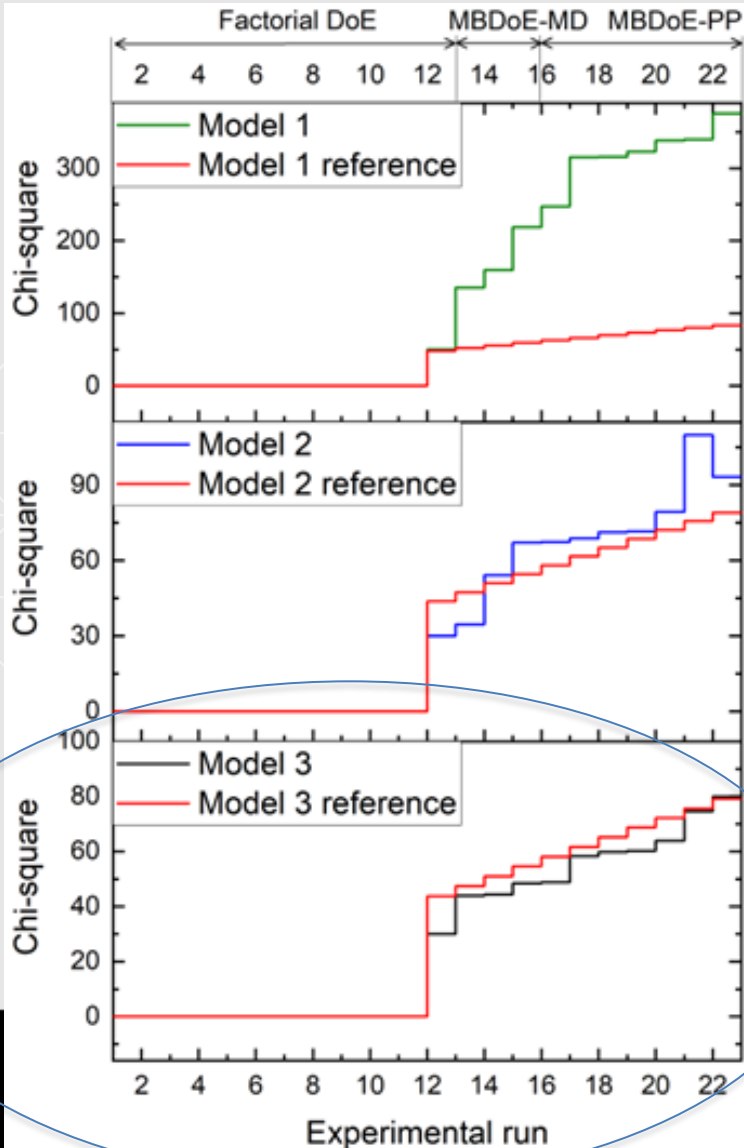


# Case study: catalytic methane oxidation

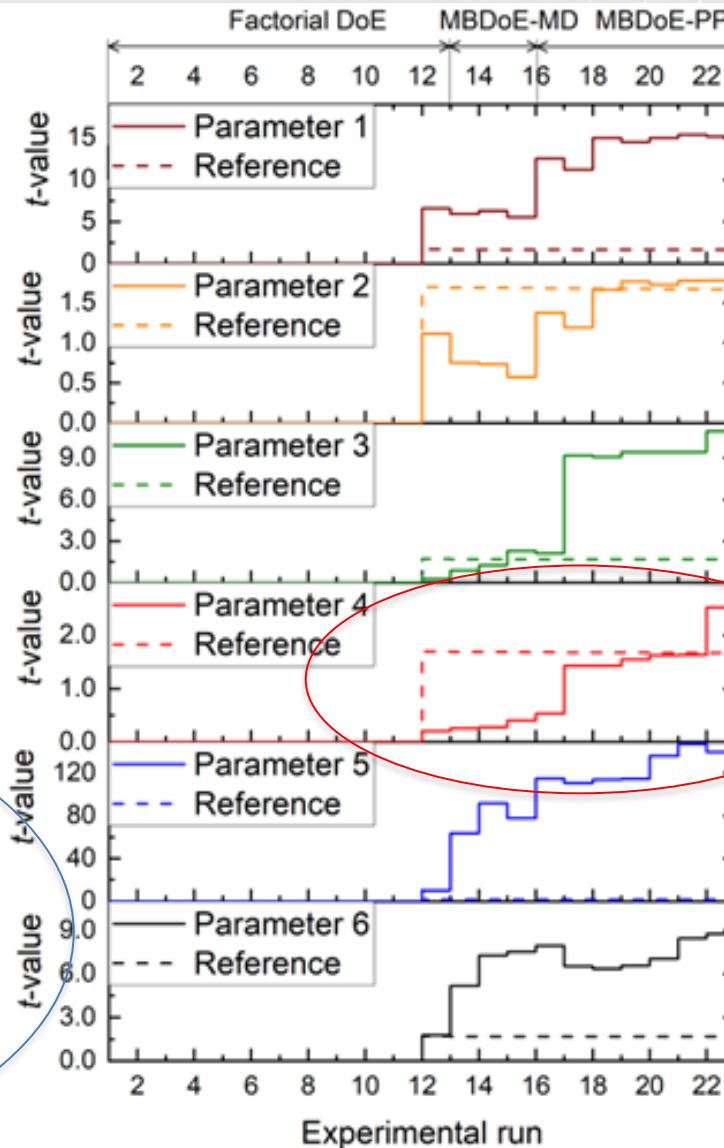
Results from the autonomous platform: model calibration



## Model Adequacy



## Parameter precision (Model 3)



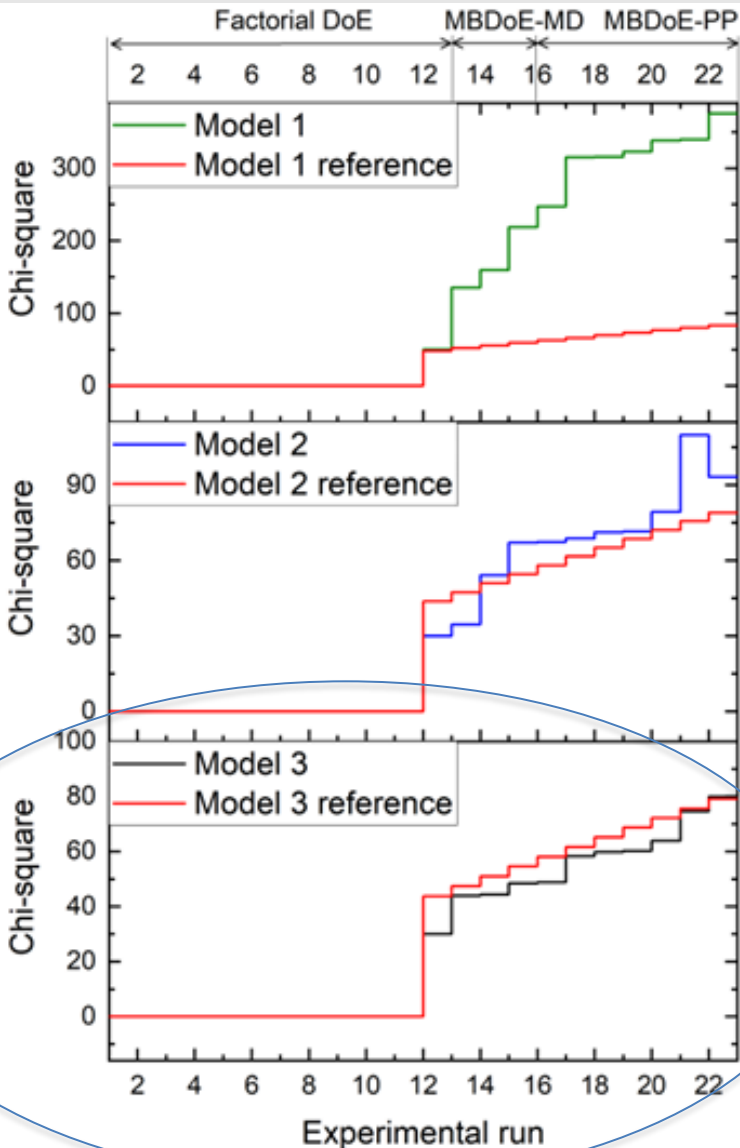
- **Only 4 MBDoe-MD experiments** required for model discrimination!
- Additional **6 experiments** needed for a precise estimation of kinetic model parameters

# Case study: catalytic methane oxidation

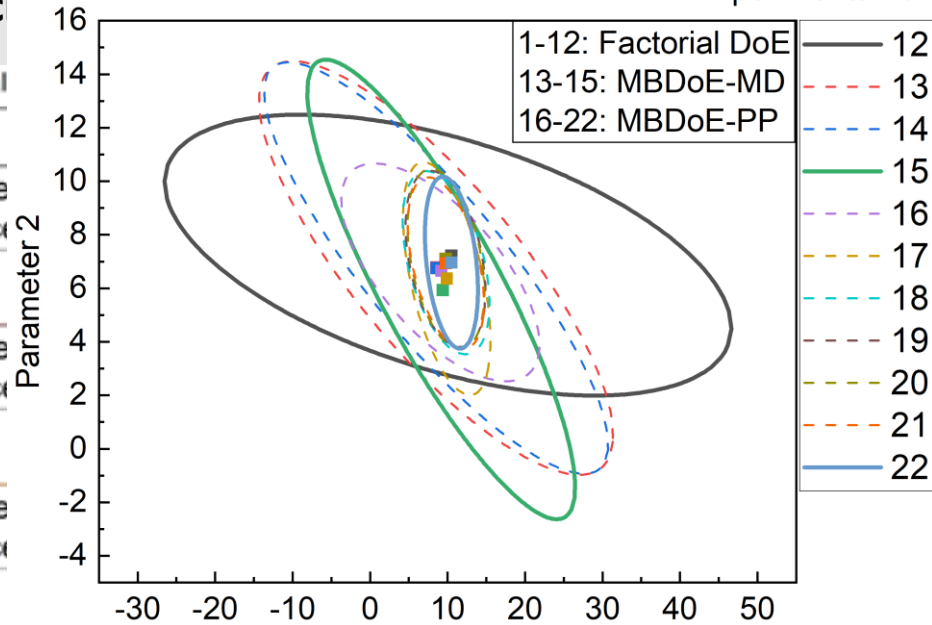
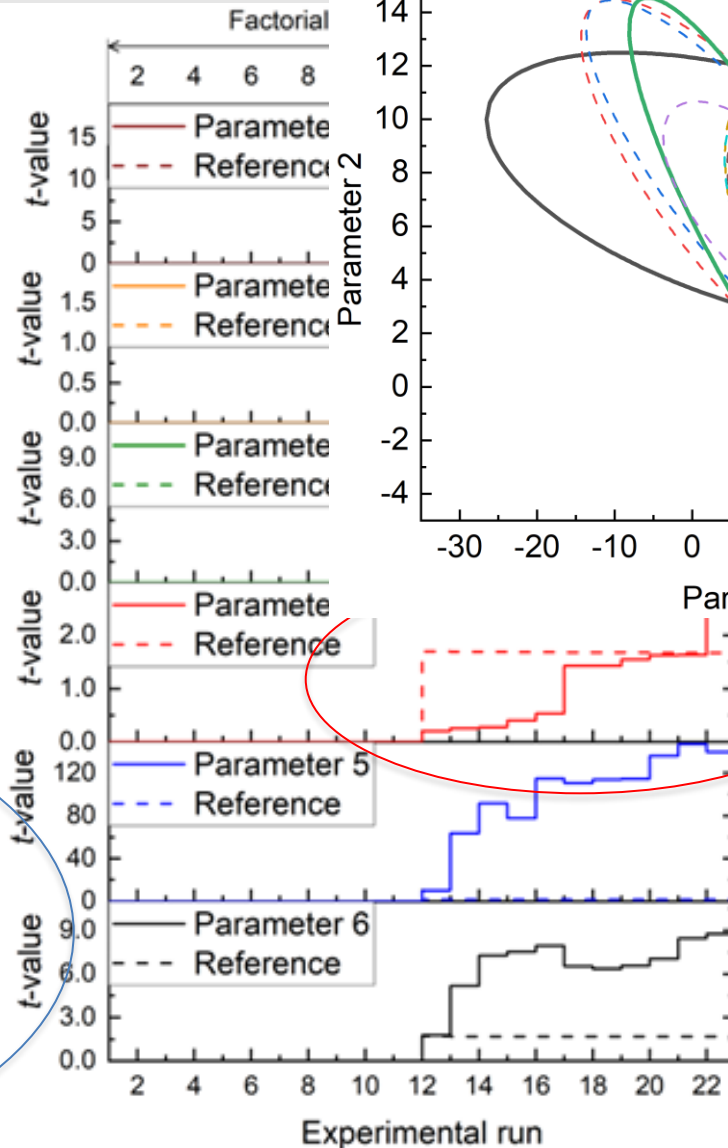
Results from the autonomous platform: model calibration



## Model Adequacy



## Parameter prec



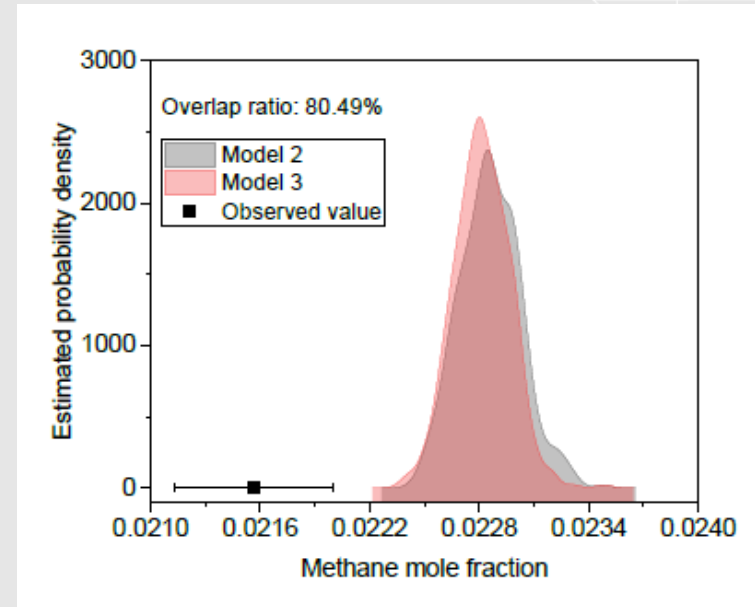
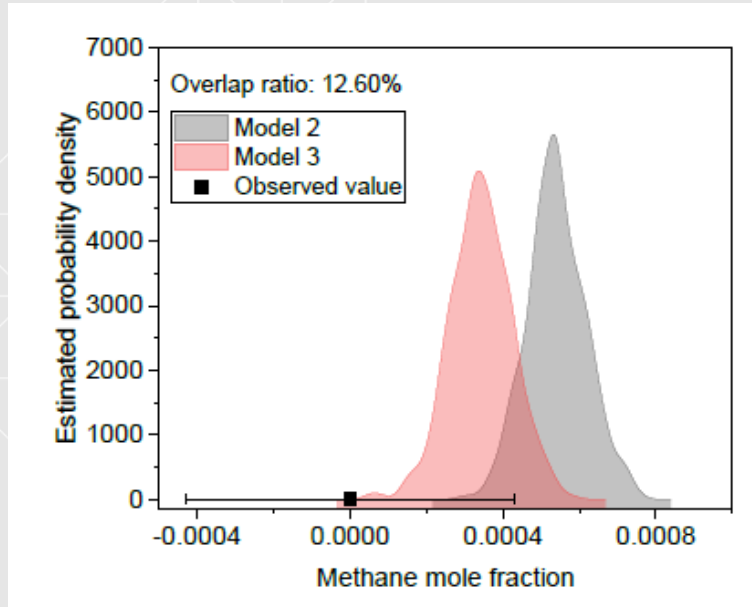
# Case study: catalytic methane oxidation

*The problem of practical model distinguishability<sup>1</sup>*

Results can be analysed retrospectively

- **Probability density plots of model responses**
- **Overlap ratio**

Arun Pankajakshan  
Research Assistant



“Easily” distinguishable models

Challenging model discrimination

<sup>1</sup>Pankajakshan, A., Bawa, S., Gavriilidis, A., Galvanin, F. (2023). Autonomous kinetic model identification using optimal experimental design and retrospective data analysis: methane complete oxidation as a case study. Reaction Chemistry & Engineering (in press).

# Machine Learning (ML)-Assisted Model Identification

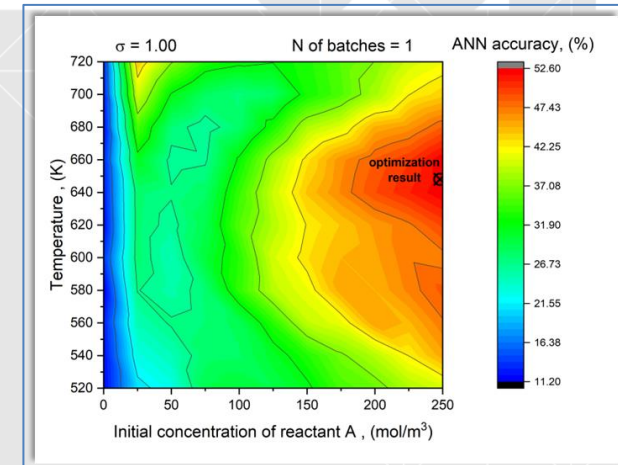
## Goals and features



Integration of machine learning (ML) techniques and MBDoE:

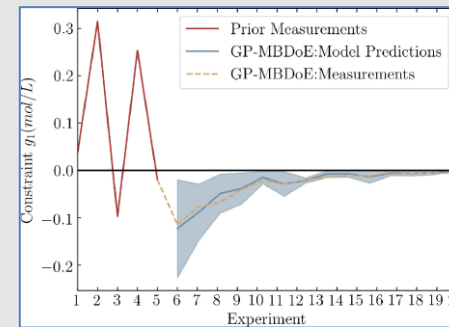
### 1. To assist **model discrimination and selection**

**Optimal Experimental Design for Kinetic Model Recognition Using Artificial Neural Networks (ANNs)<sup>1,2</sup>**



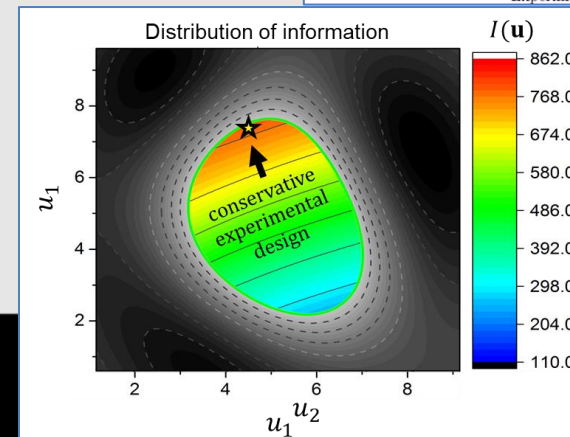
### 2. To efficiently design experiments under **uncertain scenarios**

**Safe model-based design of experiments using Gaussian processes<sup>3</sup>**



### 3. To identify design regions of model reliability

**Machine Learning (ML)-Assisted Model Reliability Mapping<sup>4</sup>**



<sup>1</sup> Quaglio et al., (2020), Computers & Chemical Engineering 135, 106759

<sup>2</sup> Sangoi et al. (2022), CACE, 49, 117

<sup>3</sup> Petsagkourakis, P., Galvanin, F. (2021), Computers & Chemical Engineering 151, 107339

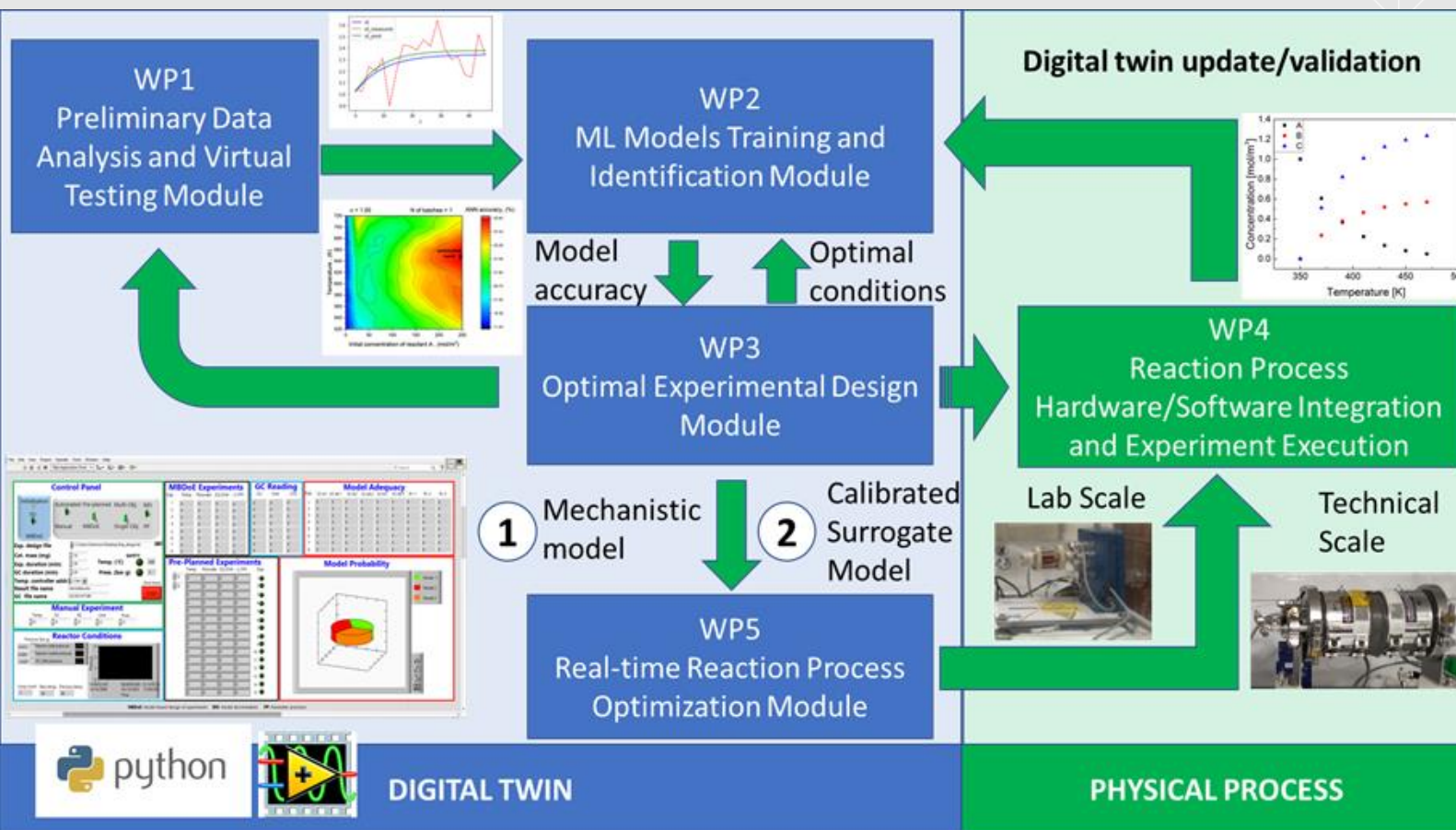
<sup>4</sup> Quaglio et al. (2018), Chemometrics and intelligent laboratory systems 172, 58

# Machine Learning (ML)-Assisted Model Identification

*ML-assisted digital twin platform for real-time optimisation of reaction systems*

**GOAL: Coupling physics-informed ML and optimal experimental design algorithms for reaction optimisation<sup>1</sup>**

PI: Federico Galvanin  
f.galvanin@ucl.ac.uk



**EPSRC**  
Engineering and Physical Sciences Research Council



**JM Johnson Matthey**  
Inspiring science, enhancing life

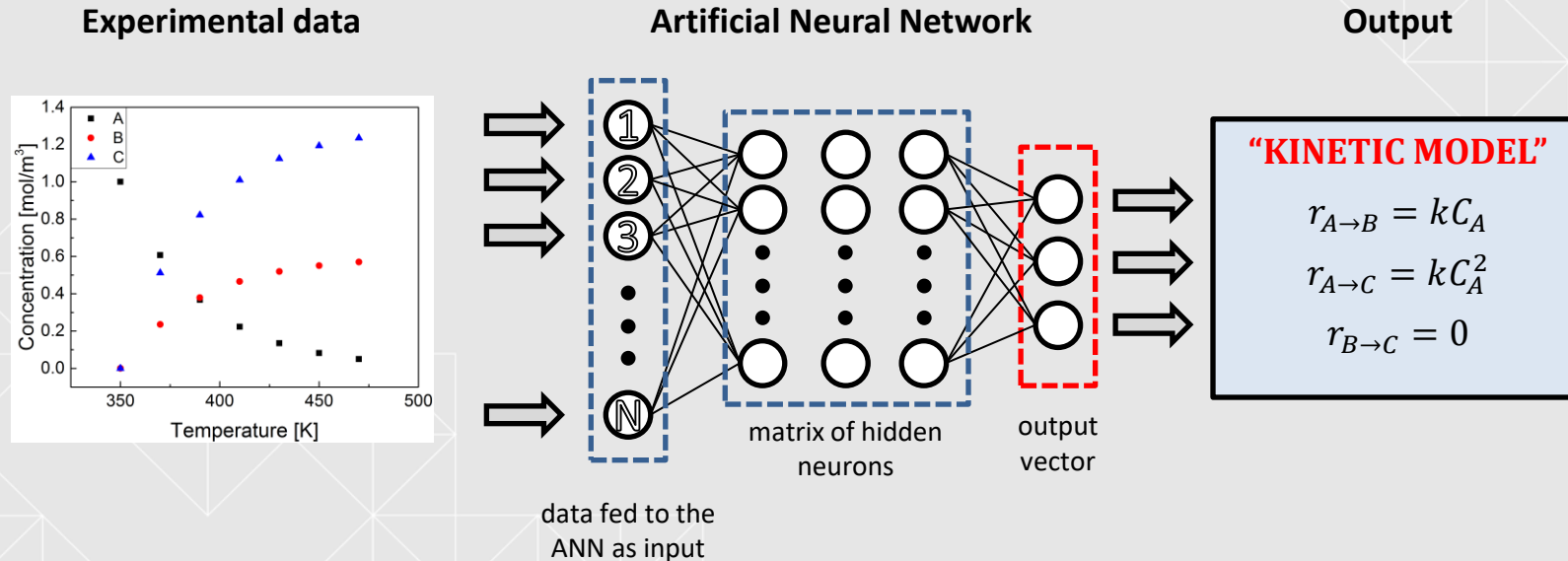


**BASF**

<sup>1</sup><https://gow.epsrc.ukri.org/NGBOViewGrant.aspx?GrantRef=EP/X024016/1>

# Kinetic Model Recognition using ANNs

## Proposed approach



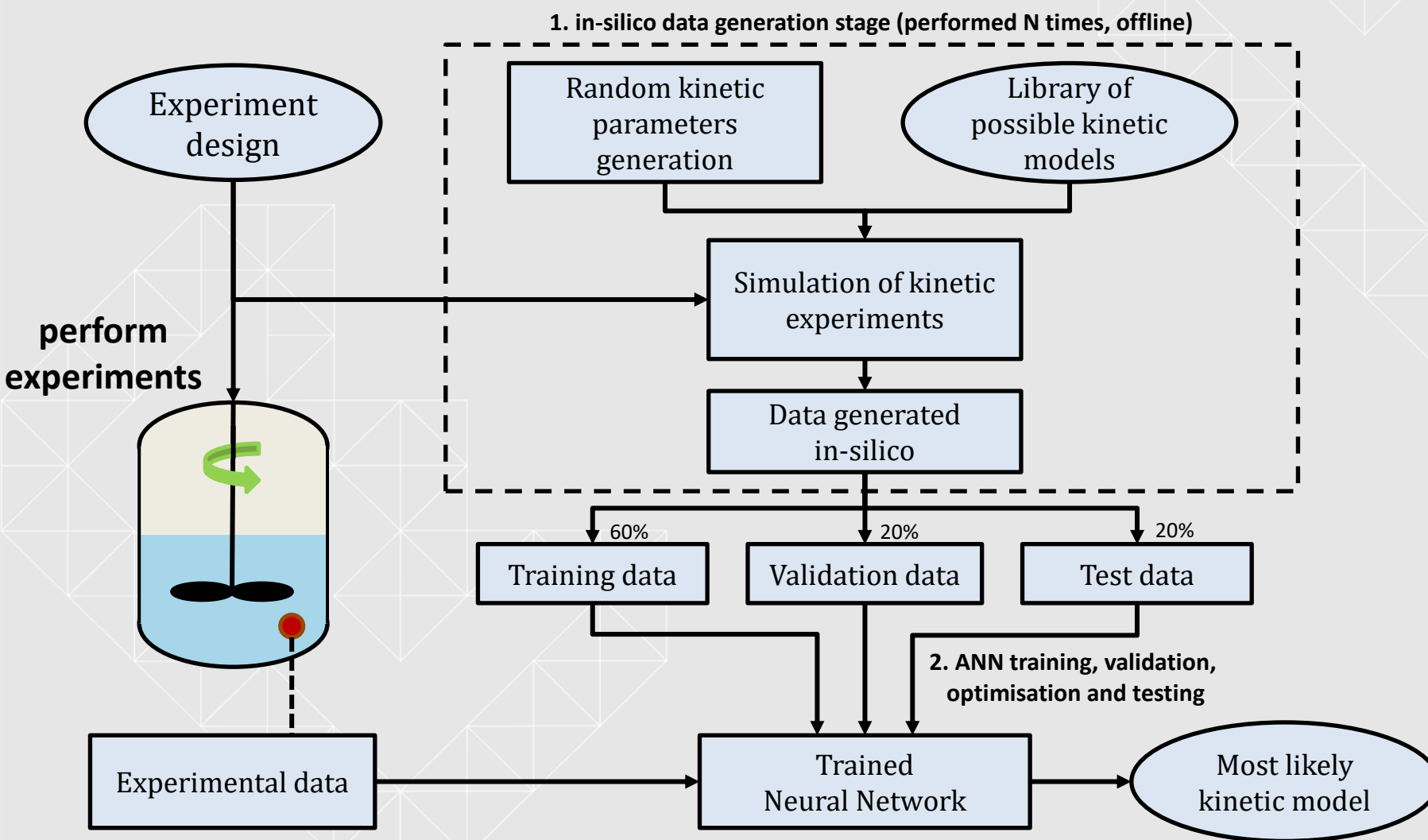
In the proposed approach, ANNs are used to model the **cognitive processes** of the **scientist's brain** rather than building a black-box representation of the physical system.

# Kinetic Model Recognition using ANNs<sup>1</sup>

Proposed approach



UCL

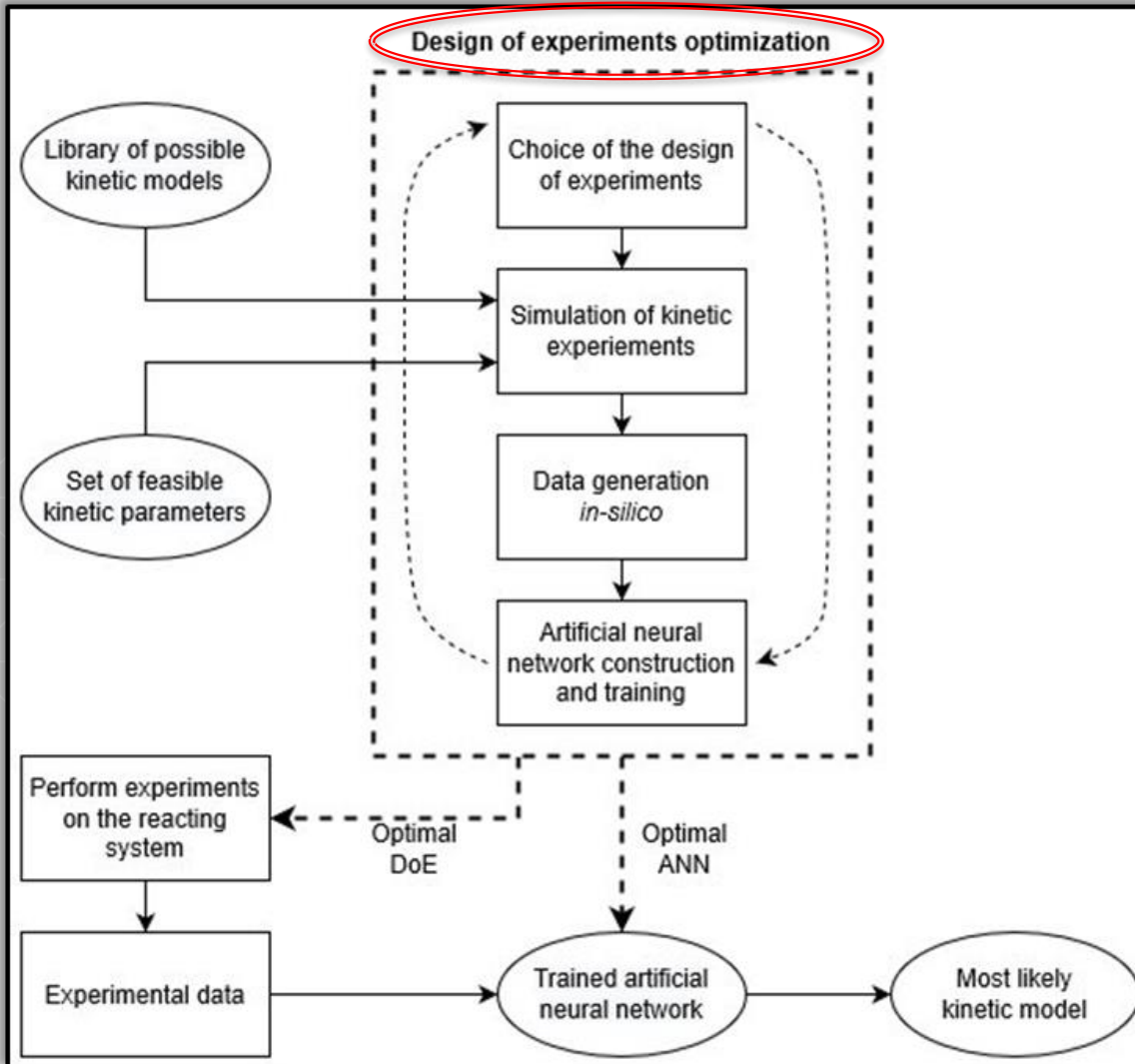


<sup>1</sup>Quaglio, M., Roberts, L., Jaapar, M., Dua, V., Galvanin, F. (2020). An artificial neural network framework for classifying chemical reaction types from experimental data. *Computers and Chemical Engineering.*, 135, 106759.



# ANNs-based Optimal Experimental Design

## Proposed procedure



<b>Input layer size:</b>	3 x (total number of samples)
<b>One hidden layer:</b>	100 nodes activation function = <i>rectified linear unit</i>
<b>Output layer:</b>	8 nodes, corresponding to each kinetic model activation function = <i>softmax</i>
<b>Accuracy:</b>	$\frac{\text{number of kinetic models correctly classified}}{\text{total number of kinetic models in the test set}}$

- **Objective function used in the optimal DoE: ANN test-accuracy**
- A **differential evolution algorithm (DEA)<sup>1</sup>** is chosen for the optimization  
→ population-based algorithm inspired by the evolutionary theory

<sup>1</sup>Storn R., Price K. (1997). Differential evolution – a simple and efficient heuristic for global optimization over continuous spaces”, Journal of Global Optimization, 11, 4, 341-359. DOI: 10.1023/A:1008202821328

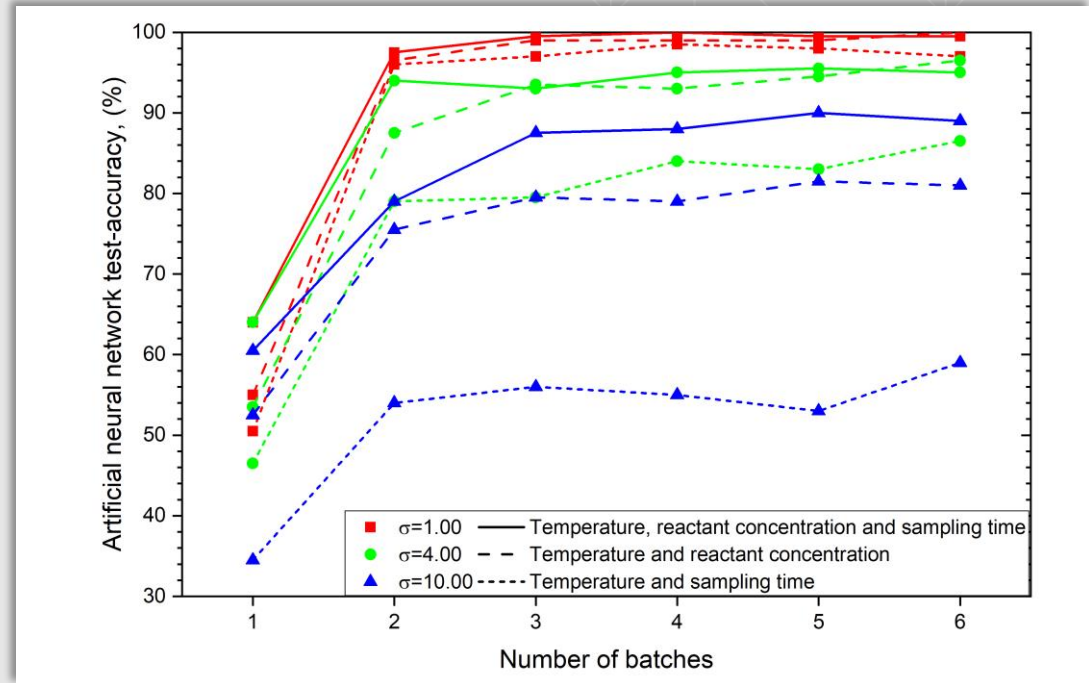
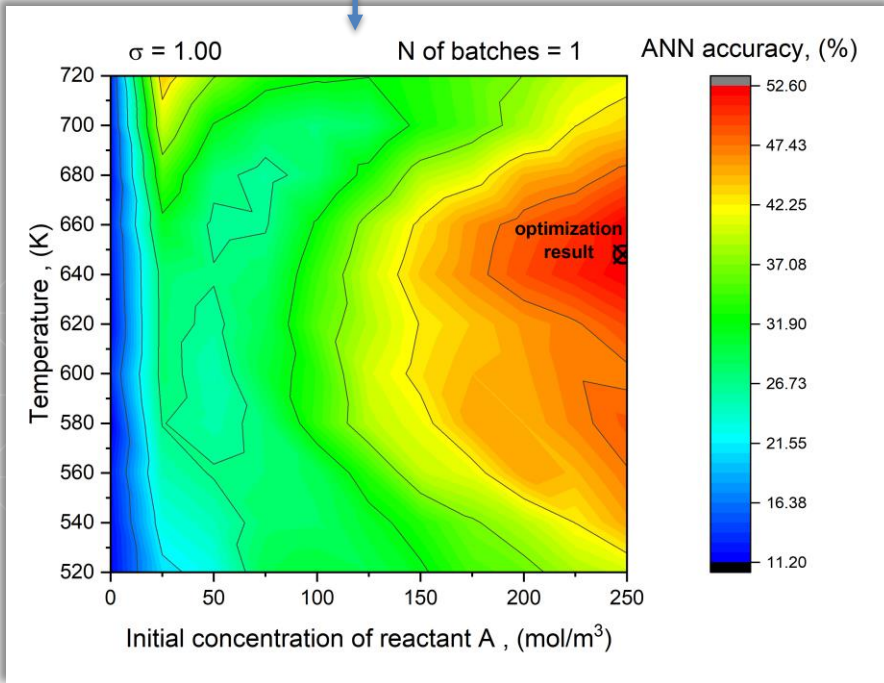


# ANNs-based Optimal Experimental Design

## Effect of design variables on ANN accuracy



Effect of **temperature** and **reactant A concentration** on ANN accuracy (1 sample)<sup>1</sup>

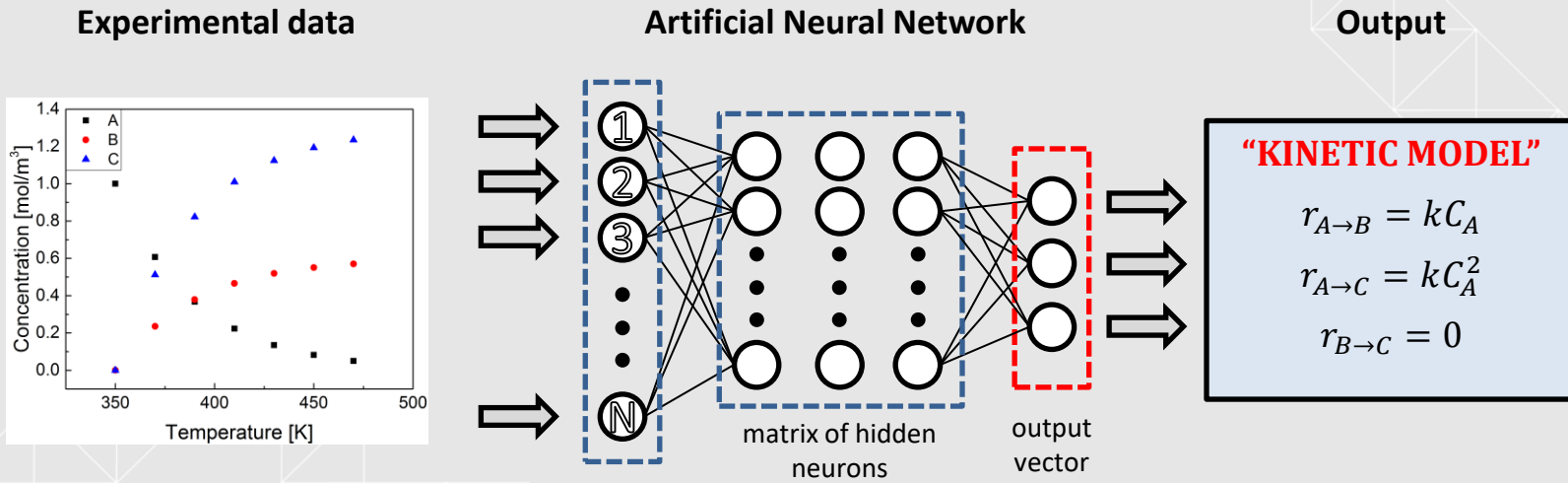


- **Very high accuracy** achieved with limited number of experiments in **low noise scenarios**
- **High accuracy achieved (close to 90%)** when temperature, reactant concentration and sampling time are optimised even in the most uncertain measurements scenario

<sup>1</sup>Sangoi, E., Quaglio, M., Bezzo, F., Galvanin, F. (2022). Optimal Design of Experiment Based on Artificial Neural Network Classifiers for Fast Kinetic Model Recognition. In: 14th International Symposium on Process Systems Engineering (PSE 2021, Kyoto).

# ANN-based Optimal Design Vs MBDoe-MD

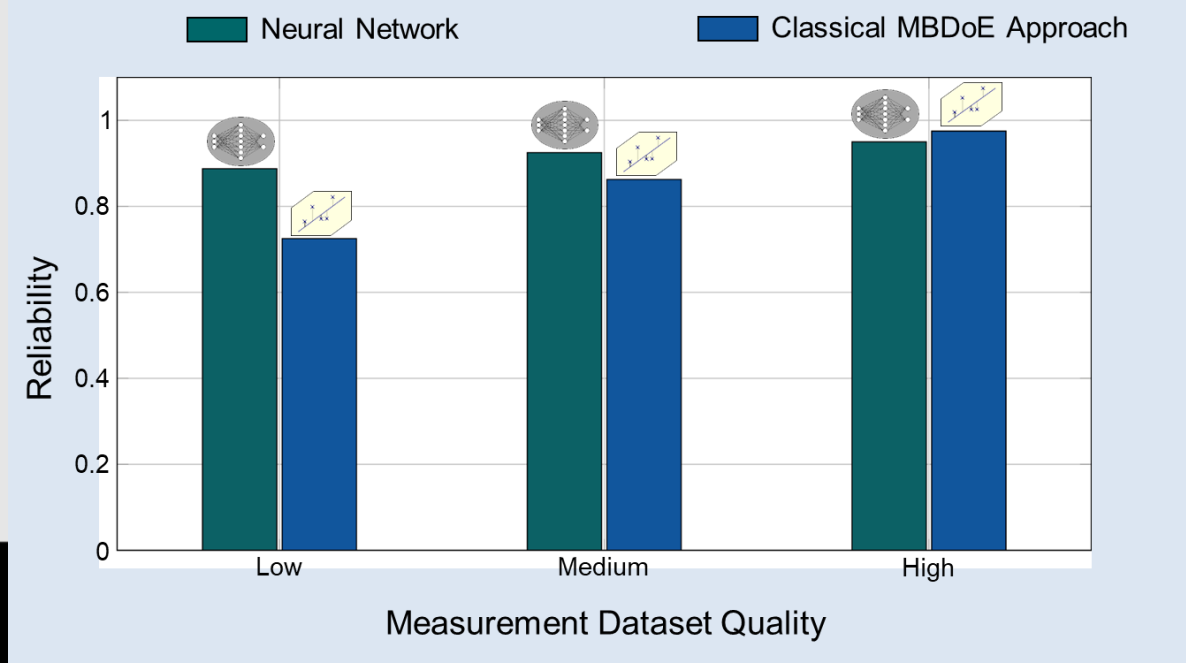
Effect of dataset quality on discrimination performance<sup>1</sup>



data fed to the ANN as input



What if this approach is **compared to a standard MBDoe approach** for model discrimination?



<sup>1</sup>N. Riske (2021). Mechanistic Model Discrimination Using Model-Based Design of Experiments and Artificial Neural Networks (Master's Thesis).

# ML-Assisted Reliability Mapping

Domain of applicability VS Domain of model reliability

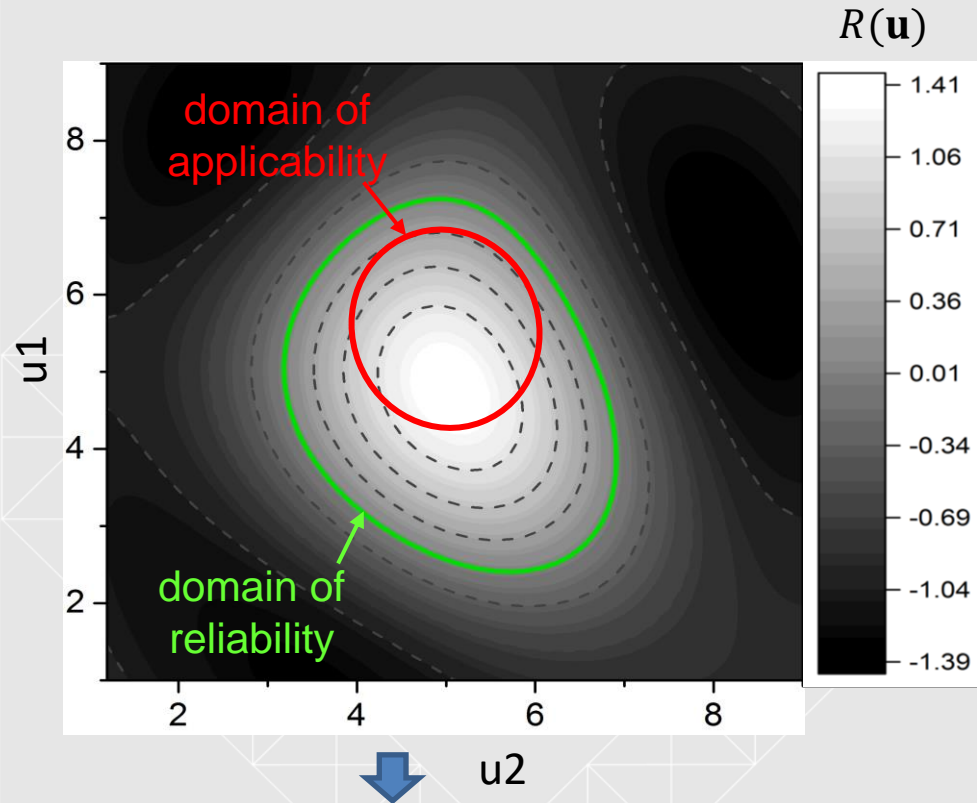
**Domain of applicability** Vs  
**Domain of reliability**



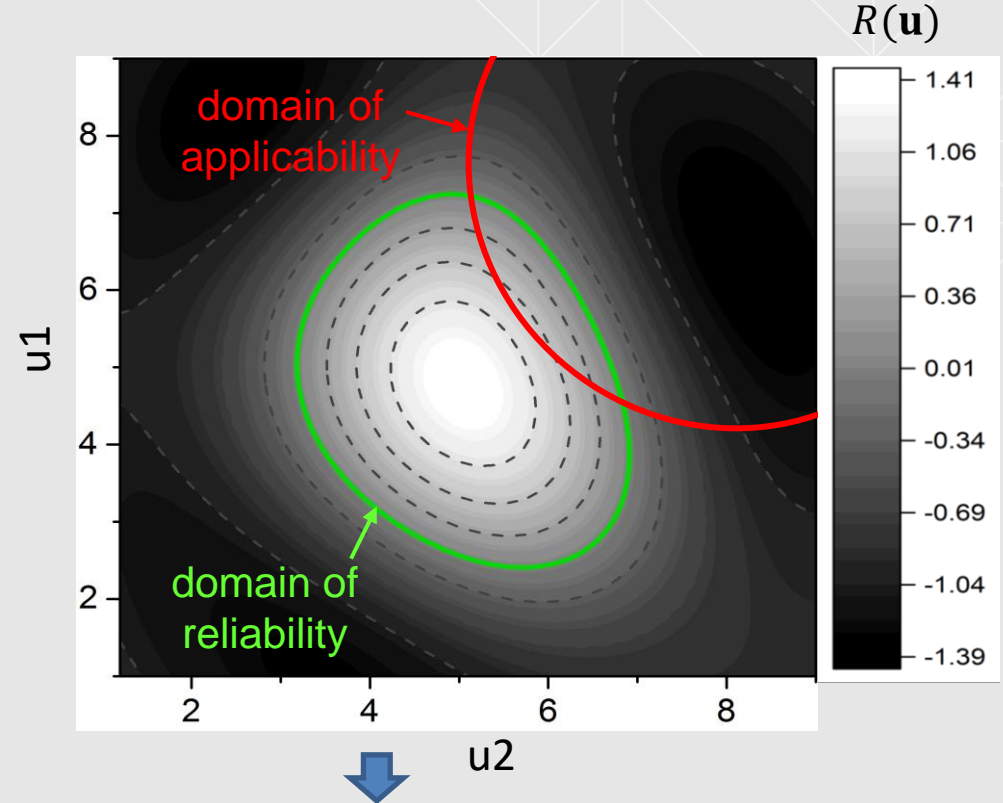
We need to identify where the model is reliable in the **design space**



This affects **all** the model-based activities



MODELLING ASSUMPTIONS ARE APPROPRIATE FOR THIS SPECIFIC APPLICATION



MODELLING HYPOTHESES MUST BE REFORMULATED

# ML-Assisted Reliability Mapping

## Constrained Model-Based Design of Experiments

What will happen if the model is not reliable in the experimental design?

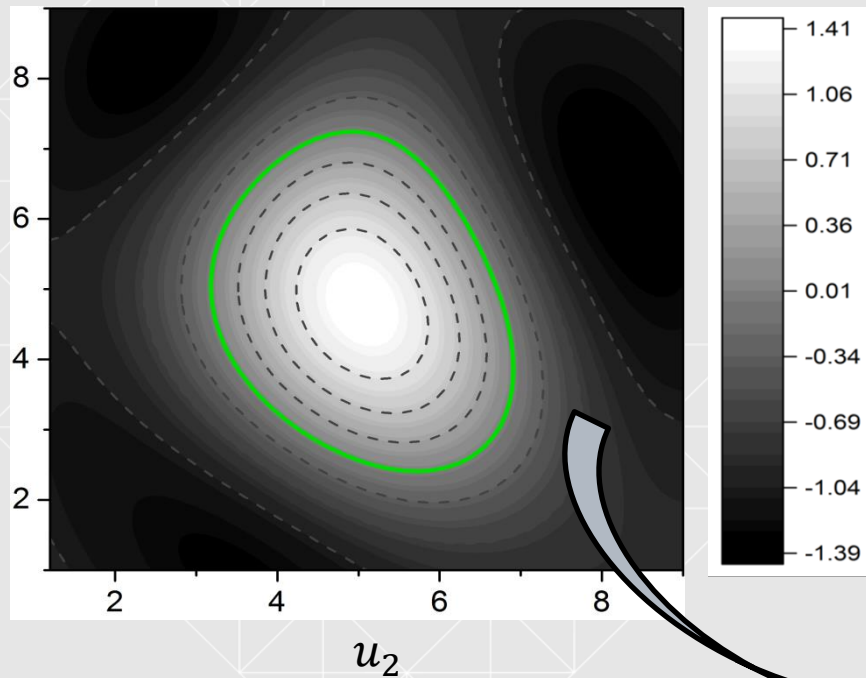
→ **Local mismatch on information prediction**

Solution: we can predict **where** the model is reliable (i.e. regions of reliability in the design space)

→ **reliability maps using Model-Based Data Mining (MBDM)<sup>1</sup>**

Reliability map<sup>1</sup>

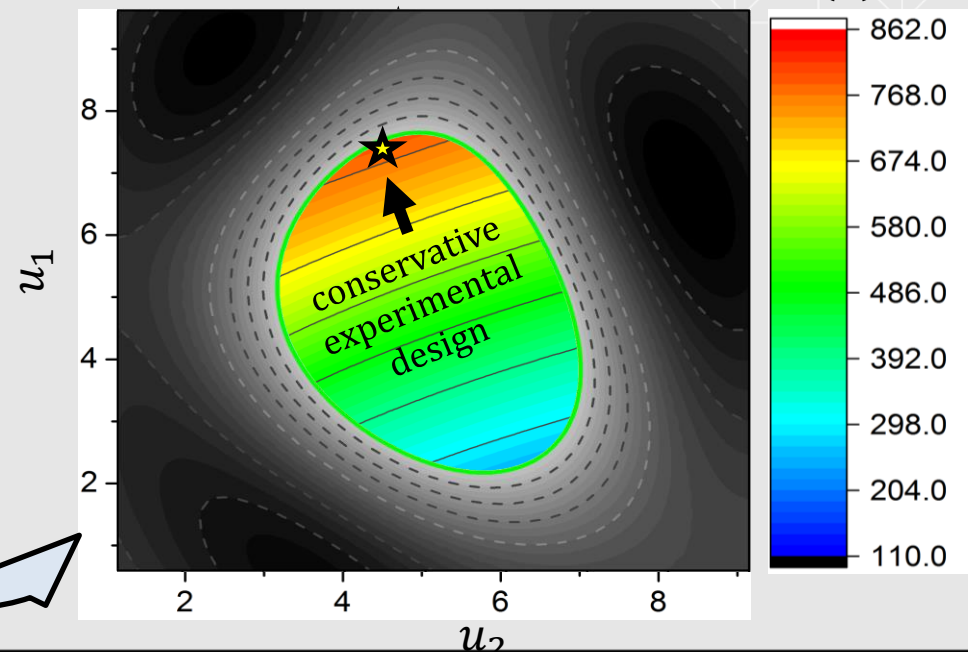
$R(\mathbf{u})$



Experimental design is constrained to conditions at  $Reliability(\mathbf{u}) > 0$

Distribution of information

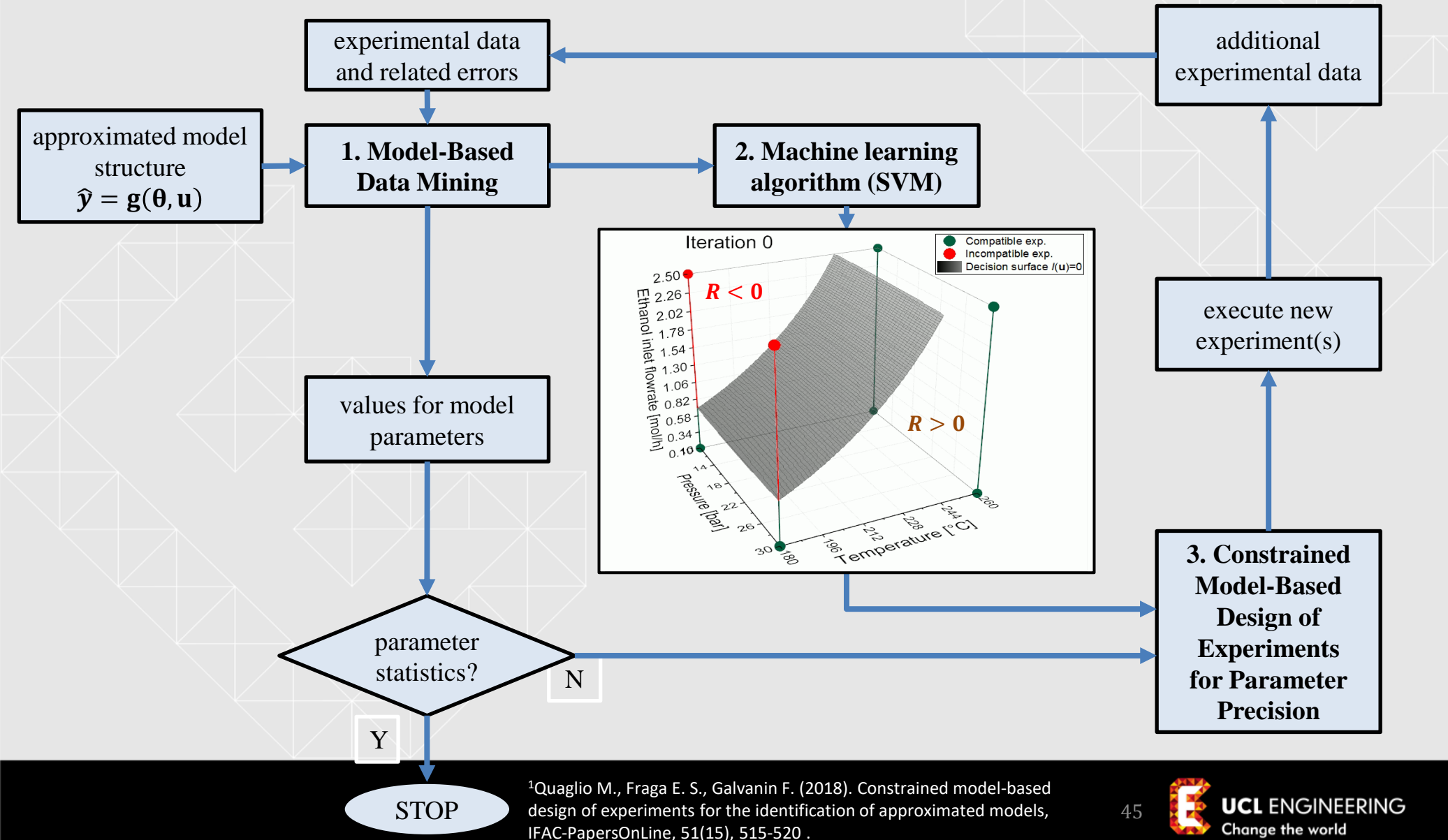
$I(\mathbf{u})$



<sup>1</sup>Quaglio M., Fraga E., Cao E., Gavriilidis A. and Galvanin F. (2017). A model-based data mining approach for determining the domain of validity of approximated models. *Chemometrics and Intelligent Laboratory Systems*, 172, 58-67

# ML-Assisted Reliability Mapping

Constrained MBDoe: iterating kinetic model identification procedure<sup>1</sup>



<sup>1</sup>Quaglio M., Fraga E. S., Galvanin F. (2018). Constrained model-based design of experiments for the identification of approximated models, IFAC-PapersOnLine, 51(15), 515-520 .



# Final remarks

- **Identification of kinetic models in Autonomous Reaction Platforms**
  - Fast identification of kinetics integrating i) **model discrimination** (MBD<sub>oE</sub>-MD); ii) **parameter precision** (MBD<sub>oE</sub>-PE); ii) **joint MBD<sub>oE</sub>-MD/MBD<sub>oE</sub>-PE**
  - Algorithms used in **online applications** and **cloud-based services (EDAS)**
  - **Online tracking of model adequacy** for mechanistic understanding
  - Techniques developed to handle practically non-identifiable («sloppy») models
  - Exploratory MBD<sub>oE</sub> based on G-optimality (**G-map eMBD<sub>oE</sub>**) now integrated
- **Kinetic model recognition using ANNs**
  - Possibility to leverage ML to identify the model structure
    - **ANN-based optimal experimental design**
  - Trade-off between noise and number of measurements to be carefully evaluated by design
- **ML-Assisted Model Reliability Mapping**
  - Systematic approach to model building using ML techniques
  - Integration in autonomous platforms





# Future works

- **Identification of kinetic models in Autonomous Reaction Platforms**
  - Integration of tools for **online model diagnostics**<sup>1</sup>
  - Integration of **ANN-based model identification framework** in autonomous platforms, and potential combination with MBD<sub>oE</sub>
  - Integration of **generative algorithms for model identification**
    - > **SINDY**<sup>2</sup> integration
  - Integration of new MBD<sub>oE</sub> techniques including **exploratory MBD<sub>oE</sub>**<sup>3</sup>
  - Integration of **optimization-free methods** for online MBD<sub>oE</sub><sup>4</sup>
  - Application to **large reaction networks systems**
  - **Application to flexible reaction systems (Taylor Vortex reactors)**

Wenyao Lyu  
PhD student



Andrea Friso  
PhD Student



<sup>1</sup>Quaglio, M., Fraga, E. S. & Galvanin, F. (2020), A diagnostic procedure for improving the structure of approximated kinetic models. Computers & Chemical Engineering, 133, 106659.

<sup>2</sup>Brunton, S. L., Proctor, J. L. & Kutz, J. N. (2016), Discovering governing equations from data by sparse identification of nonlinear dynamical systems. Proceedings of the national academy of sciences, 113, 3932.

<sup>3</sup>Cenci, F., Pankajakshan, A., Galvanin, F. (2023), An exploratory model-based design of experiments approach to aid parameters identification and reduce model prediction uncertainty, Computers & Chemical Engineering, 177, 108353, <https://doi.org/10.1016/j.compchemeng.2023.108353>

<sup>4</sup>Friso, A., Galvanin, F. (2023), An optimization-free Fisher information driven approach for online design of experiment, Computer-Aided Chemical Engineering, 52, 13.

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Andrea Friso



# EPSRC

Engineering and Physical Sciences  
Research Council

- EP/R032807/1 “Cognitive chemical manufacturing”
- EP/V050796/1 “Fully Automated Platforms for Drug Nanocrystals Manufacturing via Continuous-Flow, Data-Driven Antisolvent Crystallization
- EP/X024016/1 “Development of a machine learning assisted digital twin platform for real-time optimization of reaction systems under uncertainty”

## MSc Students

Maerthe Theresa Tillmann

# *Thank you for listening!*



# Selected publications



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