COMMUNICATIONS



# 3D printed reactors and Kessil lamp holders for flow photochemistry: design and system standardization

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Received: 14 September 2022 / Accepted: 22 June 2023 © Crown 2023

#### Abstract

A low-cost 3D printed standardized flow-photochemistry setup has been designed and developed for use with a pressuredriven flow system using photochemistry lamps available in most laboratories. In this research, photochemical reactors were 3D printed from polypropylene which facilitated rapid optimization of both reactor geometry and experimental setup of the lamp housing system. To exemplify the rapidity of this approach to optimization, a Kessil LED lamp was used in the bromination of a range of toluenes in the 3D printed reactors in good yields with residence times as low as 27 s. The reaction compared favorably with the batch photochemical procedure and was able to be scaled up to a productivity of 75 mmol  $h^{-1}$ .

#### Highlights

- We demonstrate the rapid optimization of 3D printed polypropylene reactors for flow photochemistry.
- We show that the reactors can be used with a standardized 3D printed Kessil lamp set up.

• We show how the system can be used in an exemplary photochemistry reaction for the bromination of a range of toluenes and that it can be easily scaled.

Keywords 3D Printing · Additive manufacturing · Flow chemistry · Photochemistry · Fluidics

## Introduction

Photochemical reactions have received growing interest in the literature as a result of the fact that the use of light allows for greater selectivity in activation of catalysts, especially when combined with an appropriate and finely tuned combination of wavelength and photocatalyst. Recent research in the area includes selective modification of biological molecules [1, 2], tandem reactions using multiple catalysts [3, 4] and phototelectrochemistry [5]. Although there have been many novel transformations and photocatalysts developed, there remains a fundamental problem with variation in the reports of these reactions due to the plethora of light sources and experimental setups which has led to the introduction of a number of different reported set-ups and equipment [6–13]. The issue of repeatability is receiving attention in the literature along with the often-overlooked aspect of treating light as a "reagent" [14].

Along with the increase in photochemistry publications over the last decade, the application of photochemistry to continuous flow has also received significant attention due to the significant benefits that it offers [15–19]. These include improved irradiation of the reaction mixture due to a shorter path length in flow reactors compared to batch vessels; improved reaction selectivity; fast heat exchange (important in removing heat generated by light); fast mixing of reagents and fast quenching of reactive intermediates; multiphase chemistry and easier scale-up of reactions. The direct comparison of reaction efficiency with batch is discussed in the literature and highlights the need for more research in this area and a greater understanding of the experimental setups, particularly the power and wavelength of the light source [20].

Due to the fact that much of recent research in photochemical methods involves lower energy visible light, inexpensive and readily available LED lamps have frequently been used in undergraduate laboratory experiments [21–24]. As flow chemistry is increasingly taught in practical courses,

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the move to flow photochemistry is made simpler by the availability of these lamps which can be used with existing flow equipment and transparent tubing. In addition, some groups have detailed construction of in-house developed photochemistry apparatus [23, 25] and 3D printed reactors for use in practical classes [21].

As a result of the challenges in standardizing and reporting on photochemical setup and reactions in flow chemistry, combined with our research into rapid prototyping and equipment development using 3D printing, we sought to develop a standardized housing for readily available LED lamps that could be used in combination with 3D printed flow photochemistry cells [26–30].

The aim of this was to introduce a low cost, small footprint system that could be combined with existing laboratory equipment to allow researchers to investigate photochemical reactions in flow. The use of 3D printing meant that we could develop a bespoke add-on to our existing 3D printed pressure driven flow chemistry equipment for the optimization of photochemical reactions. The circular shape of our existing previously reactors, [30] meant that these would be of a suitable standard size for LED array lamps in order to maximise irradiance as they were already circular and so would match the irradiance output from a Kessil A160WE tuna blue lamp (440 nm). The proposed set-up was therefore designed to integrate with our pressure driven continuous flow system and the photochemistry set up could be simply added to the system as shown below (Fig. 1). The aim was to utilize and optimize our existing circular disk reactors (CDRs) for flow photochemistry and to develop a suitable 3D printed housing to hold a Kessil lamp above the reactor where the distance could be easily optimized (Fig. 1).

#### **Results and discussion**

We selected a simple benzylic bromination reaction to assess the applicability of our pressure driven flow photochemistry system to demonstrate exemplification and act as a standard for comparison [31] (Scheme 1).

We initially focused on stereolithography (SLA) 3D printing for reactor production due to the transparent nature of resultant prints. However, our initial experience with using 3D printed SLA photochemical reactors was problematic as the heat given off from the lamp causing expansion and cracking of the reactor. Although polypropylene (PP) has been shown to have good transparency to near-UV light [32], we believed that the walls of our previously reported CDR could be easily narrowed to allow more light to reach the reaction. We first selected a Kessil lamp spacer distance of 25 mm in order to provide a suitable distance for further optimization studies (Fig. 2).

Initially, a 0.25 M acetonitrile solution of methyl hydrocinnamate and NBS were passed through the photo-CDR at 1.0 mL/min, affording the brominated product with no starting material observed (Table 1). Increasing the concentration to 0.5 M and reducing the residence time from 2.3 min to 26 s resulted in a small decrease in conversion. An increase in concentration above 0.5 M was not considered due to the poor solubility of succinimide which

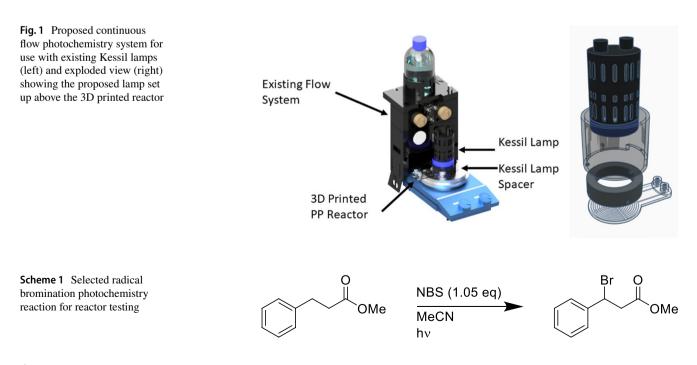
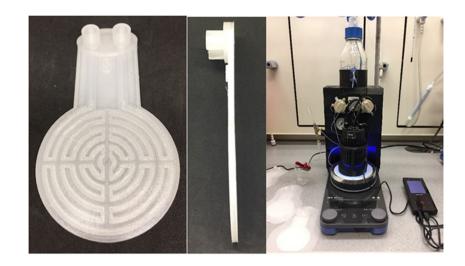


Fig. 2 Circular disc reactor (CDR) adapted for photochemistry (left and middle image); Initial setup of realized flow photochemical apparatus (right image)



could impede the flow through the capillary and therefore affect the flow rate. In terms of balancing reaction efficiency, the reactor time, and to allow for visualization of changes, we elected to carry out the reaction at a flow rate of 5 mL/ min in order to increase reaction throughput and to minimize formation of trace dibrominated products. To obviate any impedance of flow rate after each run, the capillary was simply removed and back-flushed with acetone after each reaction [30].

At this stage, trace amounts of dibrominated product could be observed in the <sup>1</sup>H NMR spectrum of the crude material and so, we decided to optimize the distance of the lamp from the reactor. The spacer was designed to sit directly on top of the reactor to give a more reliable distance between the lamp and the reaction. Lamp stands with a range of distances (Table 2) were 3D printed as well as an external collar (Supplementary information) to prevent the operator being exposed to light emitted from the photo-CDR and hotplate underneath. The efficiency of the bromination reaction was evaluated at 6 different distances (Table 2). Although the trend observed was as expected, 3D printing of the spacers allowed optimization to be carried out quickly and demonstrates the benefits of such an approach, which given the significant implications on photon flux, is often lacking in the literature. It was decided that a distance of 30 mm was to be used

so that any improvements in reaction efficiency due to subsequent modifications would be discernable and we could examine the isolated effect of distance on the yield of the reaction analogous to batch reactions which are often carried out in the absence of reflective sources and without distance quantification.

Following the optimization of reaction distance, as can be seen in Fig. 3, the photochemistry reactions were subsequently conducted at 0.5 M concentration and with the CDR situated directly on top of an IKA RCT Digital magnetic stirrer hotplate which has a reflective surface. The effect of this was compared to an older more tarnished hotplate resulting in less than half the conversion. Whereas the mirror directly underneath the CDR had an improvement, the effect of a reflective surface around the inside of the lamp holder had a greater effect on the reaction conversion. The combination of both mirror and reflective lamp stand resulted in complete conversion (Table 3 and Supplementary information).

Due to the ease with which new reactor designs can be prepared using 3D printing, we next sought to optimize the CDR internal dimensions. A range of reactor designs were printed to investigate the effect of channel width and height as well as the thickness of polypropylene above and below the reactor channels as well as reproducibility of design (R3

Table 2 Distance optim	nization
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Table I Initial results						
Entry	Concentration	Flow Rate (mL/min)	t (sec)	Conv. (%)		
1	0.25	1.01	137	100		
2	0.5	1.01	137	98		
3	0.5	1.90	73	99		
4	0.5	5.40	26	90		

Entry	Distance (mm)	Flow Rate (mL/ min)	t (sec)	Conv. (%)
1	50	5.10	27.2	2
2	40	5.19	26.7	31
3	30	5.15	26.9	69
4	20	5.10	27.2	88
5	15	5.09	27.2	100
6	10	5.09	27.2	100

**Fig. 3** 3D printed lamp holder for distance optimization (shown with reflective internal surface)



and R4) enabling variations in thickness and residence time to be explored (Fig. 4 and Supplementary Information for their respective sizes and channel diameters).

Given the observation that reflection of light from underneath the CDR is beneficial, it is not surprising that the thickness of polypropylene above the CDR channels has less of an effect on the reaction efficiency. This can be observed by the conversion achieved using reactor R12 which had twice the thickness of polypropylene above and below any of the adapted CDRs but with a larger internal volume where the channel depth was 1.50 mm versus the narrower examples which ranged from 0.75 mm to 1 mm. From the results, there is a correlation between conversion and the area of the reactor channel cross-section with reactors 5 and 6 having smaller cross sections of 1.13 mm<sup>2</sup>, a low yield of 39% was obtained. When the cross sectional area was increased to 3.5 mm<sup>2</sup> for reactors 2 and 10, the yield increased to 98% and 91% respectively. However, the use of a larger reactor volume and therefore longer residence time is more likely the simpler explanation for the observed increases in reaction conversion as we can observe that the increased residence time in each reactor gives a strong correlation to the yield (Table 4).

With the optimized conditions and selection of photo-CDR - R2 as the optimal reactor, we turned our attention to the reaction of a series of toluene substrates (Table 5).

Table 3 Reactor housing optimisation

Material	HPLC Conversion (%)
RCT Digital	67 (average, $n=4$ )
Old RCT Basic	31
Black card	8
Mirror	70
Internal Reflective Lamp Holder (with black card underneath)	87
Mirror+Reflective Lamp Holder	100

Reactions were carried out using a Kessil A160 WE tuna blue lamp using reactor 2 at a concentration of 0.5 M and run at a flow rate of 5.05 mL/min to give a range of benzyl bromides in good yields and high selectivities. However, for more challenging benzyl bromides a higher residence time was required to obtain analogous yields which we attributed to increased heating via exposure to the Kessil lamp as noted by previous authors [31]. When a longer residence time (3 min) was required (method B – 0.5 M, flow rate of 1.0 mL/min), the benzyl bromide was often

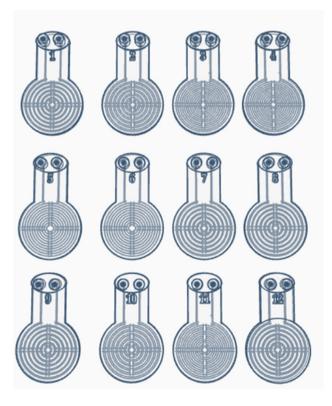


Fig. 4 Designs of flow paths used for the 3D printed reactors (reactors R1-R12)

Table 4Reactor optimizationresults

Reactor No	Surface area (mm <sup>2</sup> )	Cross sec- tion area (mm <sup>2</sup> )	Reac- tor vol. (cm <sup>3</sup> )	Flow Rate (mL/min)	Residence time (sec)	Conv. (%)
R1	2.31	3.00	2.31	5.15	27	86
R2	2.69	3.50	2.69	5.05	32	98
R3	3.01	2.81	2.26	5.15	26	88
R4 (same as R3)	3.01	2.81	2.26	5.19	26	87
R5	2.01	1.13	1.51	5.05	18	39
R6	2.01	1.13	1.51	5.03	18	39
R7	2.31	3.00	2.31	5.22	27	56
R8	2.31	2.25	1.73	5.16	20	32
R9	2.31	3.00	2.31	5.15	27	66
R10	2.69	3.50	2.69	5.18	31	91
R11	3.01	2.81	2.26	5.11	32	85
R12 (thick-walled reactor)	2.31	4.50	3.47	5.04	41	100 (by NMR)

isolated with small amounts of the dibrominated product, but this could be easily overcome by using the short residence time of method A affording only monobrominated products (Table 5).

One of the well-known advantages of flow chemistry is that scale-up of the reaction can be easily achieved by running the reaction continuously for a longer period of time. An additional benefit with regards to photochemistry in flow, is that the reactor dimensions and lamp setup can be optimized for a particular reaction as this dictates the amount of irradiance the reaction solution receives. Conversely, scaling a batch photochemical reaction would require a larger vessel that would suffer from poor penetration of light and over-irradiation [33].

To adapt our pressure driven flow system to accommodate large volumes, an additional Duran pressure bottle was used in place of one of the solvent loops (Fig. 5 and Supplementary Information). The air pressure feed from the pressure control module was split between the larger solvent reservoir bottle on the top of the flow system and the smaller reagent bottle on the side. Once all tubing was primed with solvent, the tube feeding line B was manually switched from the solvent reservoir bottle to the reagent bottle. This meant that there would be no air in the system and the plug of reactant solution could be easily flushed through in its entirety by switching the flow to line A once the reagent bottle had emptied (Fig. 5 and Supplementary Information).

In the first instance, the reaction was attempted with 50 mL of a 0.5 M solution of reactants. As mentioned above, the capillary resistor was routinely flushed with acetone to remove any insoluble succinimide after each reaction. Unfortunately, this meant that when attempting to scale-up the reaction at the same concentration, it resulted in a reduction in flow rate over time as succinimide precipitated out from the reaction from 5 mL/ min to 1.6 mL/min. The flow rate would return to normal after flushing of the capillary with acetone but this was clearly not a practical solution for an extended run. This issue was solved by halving the concentration so that the succinimide would remain in solution. When the same reaction was attempted with 50 mL of a 0.25 M solution (10-min total run-time), the flow rate was unchanged during the reaction and the product benzyl bromide was isolated in 89% yield, corresponding to a 78 mmol  $h^{-1}$ throughput.

In order to illustrate the benefits of conducting photochemical reactions in flow over batch, a comparison was carried out, where a solution of reactants were irradiated under the same conditions. As with the flow procedure, a 0.5 M solution of methyl hydrocinnamate and NBS in acetonitrile was placed in a 2–5 mL microwave vessel (Biotage) and irradiated at a distance of 30 mm. An aliquot taken after 27 s showed 36% conversion by HPLC, clearly demonstrating the benefits of continuous flow photochemistry. 
 Table 5
 Reaction Scope

	$R^2$	NBS (1.05 eq) MeCN hv			Br
	R <sup>1</sup>			Ĺ	$R^2$
Entry	Product	Method	Residence Time	Yield (%)	R <sup>··</sup> Bromination ratio (Mono:Dibrominated)
1	Br O OMe	A	31 s	89	100:0
2	O	A	32 s	55	100:0
3	CI	A	32 s	60	100:0
4	Br	A	31 s	71	100:0
5	Br	A	31 s	62	100:0
6	Br	A	30 s	<2	100:0
7		В	2.7 min	60	94:6
8	Br	В	2.6 min	36	100:0
9	Br Br	В	2.9 min	75	93:7
10	Cl Br	В	2.7 min	82	93:7
11	Br	В	2.7 min	92	89:11
12	O <sub>2</sub> N	В	2.7 min	83	90:10
13	EtO <sub>3</sub> S	В	2.8 min	73	93:7



Fig. 5 Increased scale set-up, showing the arrangement of tubing to allow for increased volumes of reagents to pass through the system

## Conclusion

We have developed an inexpensive and adaptable photochemistry apparatus to be used with our pressure-driven flow chemistry system. Optimization of a bromination reaction was carried out using 3D printed polypropylene circular disc reactors that were adapted for photochemistry. The reaction proceeded well with a residence time of only 27 s. We were able to show the benefit of 3D printing polypropylene reactors for photochemistry and the ability to modify reaction paths for optimization. Scale-up of the photochemical bromination was carried out successfully with a throughput of 78 mmol h<sup>-1</sup>. Whilst the system that we have reported is designed for use with Kessil lamps, it can easily be adapted for use with others. The effect of temperature on the reaction is currently being investigated and will be reported in due course.

Supplementary Information The online version contains supplementary material available at https://doi.org/10.1007/s41981-023-00278-w.

Acknowledgements The authors acknowledge funding from Zurich Insurance for the work carried out in this study which was given to fund MRP and collaboration with IKA in the development of the IKA FLOW continuous flow system. **Open Access** This article is licensed under a Creative Commons Attribution 4.0 International License, which permits use, sharing, adaptation, distribution and reproduction in any medium or format, as long as you give appropriate credit to the original author(s) and the source, provide a link to the Creative Commons licence, and indicate if changes were made. The images or other third party material in this article are included in the article's Creative Commons licence, unless indicated otherwise in a credit line to the material. If material is not included in the article's Creative Commons licence and your intended use is not permitted by statutory regulation or exceeds the permitted use, you will need to obtain permission directly from the copyright holder. To view a copy of this licence, visit http://creativecommons.org/licenses/by/4.0/.

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