

Modulation of elasto-inertial transitions in Taylor-Couette flow by small particles

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| Abstract: | Particle suspensions in non-Newtonian liquid matrices are frequently encountered in nature and industrial applications. We here study the Taylor-Couette flow (TCF) of semi-dilute spherical particle suspensions (volume fraction ≤ 0.1) in viscoelastic, constant viscosity liquids (Boger fluids). We describe the influence of particle load on various flow transitions encountered in TCF of such fluids, and on the nature of these transitions. Particle addition is found to delay the onset of first and second order transitions, thus stabilising laminar flows. It also renders them hysteretic suggesting an effect on the nature of bifurcations. The transition to elasto-inertial turbulence is shown to be delayed by the presence of particles, and the features of elasto-inertial turbulence (EIT) altered, with preserved spatio-temporal large scales. These results imply that particle loading and viscoelasticity, which are known to destabilize the flow when considered separately, can on the other hand compete with one-another and ultimately stabilize the flow when considered together. |
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Modulation of elasto-inertial transitions in Taylor-Couette flow by small particles

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Particle suspensions in non-Newtonian liquid matrices are frequently encountered in nature and industrial applications. We here study the Taylor-Couette flow (TCF) of semi-dilute spherical particle suspensions (volume fraction ≤ 0.1) in viscoelastic, constant viscosity liquids (Boger fluids). We describe the influence of particle load on various flow transitions encountered in TCF of such fluids, and on the nature of these transitions. Particle addition is found to delay the onset of first and second order transitions, thus stabilising laminar flows. It also renders them hysteretic suggesting an effect on the nature of bifurcations. The transition to elasto-inertial turbulence is shown to be delayed by the presence of particles, and the features of elasto-inertial turbulence (EIT) altered, with preserved spatio-temporal large scales. These results imply that particle loading and viscoelasticity, which are known to destabilize the flow when considered separately, can on the other hand compete with one-another and ultimately stabilize the flow when considered together.

Key words: Suspension, Elasto-inertial turbulence, Viscoelasticity, Taylor-Couette

1. Introduction and background

Particle suspensions in non-Newtonian liquids are frequently encountered in nature and industrial applications, such as cement, toothpaste, 3D printing material or drilling muds, (Ovarlez *et al.* 2015; Dagois-Bohy *et al.* 2015; Fang *et al.* 2017; Liu *et al.* 2015). Multiple non-linear effects, such as non-linear dynamic behaviour of the liquid phase, fluid-particle and particle-particle interactions, can co-exist in such systems giving rise to complex rheology and macroscale flow dynamics. Significant efforts have been made in recent years to derive constitutive equations to accurately describe the physical properties of these complex fluid systems (Morris 2020; Yang & Shaqfeh 2018*a,b*; Gillissen & Wilson 2019). However, experimental data is still needed to better understand the effects of such complex particle suspensions on the stability and transitions in macroscale flows, in order to link microscopic and macroscopic behaviour.

For that purpose, one can advantageously use the "hydrogen atom" of fluid mechanics

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38 (Fardin *et al.* 2014), Taylor-Couette flows (TCF): the flow developing between two
39 concentric cylinders at least one of which is rotating. This simplified geometry is widely
40 used in rheometry and also to investigate stability and transitions in various fluids,
41 including for example non-Newtonian polymeric solutions (see e.g. Martínez-Arias &
42 Peixinho (2017); Cagney *et al.* (2020); Dutcher & Muller (2013); Lacassagne *et al.* (2020,
43 2021) among many others), and particle suspensions in Newtonian solvents (Majji &
44 Morris 2018; Majji *et al.* 2018; Ramesh *et al.* 2019; Ramesh & Alam 2020; Morris 2020;
45 Gillissen & Wilson 2019; Gillissen *et al.* 2020). This last topic has recently benefited
46 from a set of comprehensive experimental studies describing the effects of low particle
47 concentrations on mixing in TCF (Rida *et al.* 2019; Dherbécourt *et al.* 2016), TCF
48 dynamics of dense particle suspensions with sedimentation and re-suspension (Saint-
49 Michel *et al.* 2017, 2019), and the effects of intermediate particle concentrations on high
50 order flow transitions (Majji & Morris 2018; Majji *et al.* 2018; Ramesh *et al.* 2019;
51 Ramesh & Alam 2020; Dash *et al.* 2020; Baroudi *et al.* 2020). As part of the latter, it has
52 been shown that the presence of particles globally tends to destabilise the flow (Majji
53 *et al.* 2018; Ramesh *et al.* 2019; Dash *et al.* 2020), as predicted by modelling approaches
54 (Gillissen & Wilson 2019). It was also found to promote additional non-axisymmetric flow
55 states (Ramesh *et al.* 2019; Dash *et al.* 2020) and the co-existence of flow states (Majji
56 *et al.* 2018; Ramesh & Alam 2020; Dash *et al.* 2020), thus altering the common Couette
57 Flow (CF) - Taylor Vortex Flow (TVF) - Wavy Taylor Vortex flow (WTVF) transition
58 encountered in TCF of Newtonian fluids with the inner cylinder only rotating.

59 When considering TCF of polymer solutions, it has been consistently shown that their
60 non-Newtonian features also tend to destabilize the base and first order laminar flows
61 (Cagney *et al.* 2020; Lacassagne *et al.* 2021), give rise to additional flow states (see
62 e.g. Dutcher & Muller (2013); Lacassagne *et al.* (2020); Groisman & Steinberg (1996)),
63 and transition to low Re turbulent-like states such as elastic (Groisman & Steinberg
64 2004) or elasto-inertial turbulence (Dutcher & Muller 2013; Lacassagne *et al.* 2020,
65 2021). However, it was recently highlighted experimentally that various non-Newtonian
66 features of the same fluid may not combine towards destabilizing the flows, but rather
67 compete, with shear-thinning mediating elasto-inertial transitions (Cagney *et al.* 2020;
68 Lacassagne *et al.* 2021). Questions then arise when considering TCF of suspensions in
69 non-Newtonian fluids. Are the two complex features of the fluid, namely elasticity and
70 the presence of particles, expected to act in synergy to destabilise the flow? Will the
71 presence of particles mediate elasto-inertial instabilities? To address these questions,
72 we here study the TCF of semi-dilute mono-disperse spherical particle suspensions
73 (polymethylmethacrylate particles, GoodFellow, United Kingdom, $0.01 \leq \phi \leq 0.1$, with
74 ϕ the particle volume fraction) in a viscoelastic, fluid with constant shear-viscosity (Boger
75 fluid made of polyacrylamide dissolved in a water glycerol mixture as in Lacassagne *et al.*
76 (2020)), the density of which matched that of the particles ($\rho = 1198 \text{ Kg.m}^{-3}$)

77 2. Experimental details

78 The steady-shear rheology of suspensions was measured using an ARES rheometer
79 (TA Instruments) equipped with a Couette geometry (1 mm gap). Characterisation was
80 systematically performed on the Boger matrix itself and on the particle suspension in
81 Boger fluid, before and after the Taylor-Couette experiments (the exact same sample
82 as that used for the TCF experiment). This last step allowed us to verify that the
83 samples did not experience polymer degradation during the experimental protocol.
84 Additional characterisation of the water-glycerol mixture with and without particles
85 were also performed separately. Examples of viscosity curves are reported in figures 1

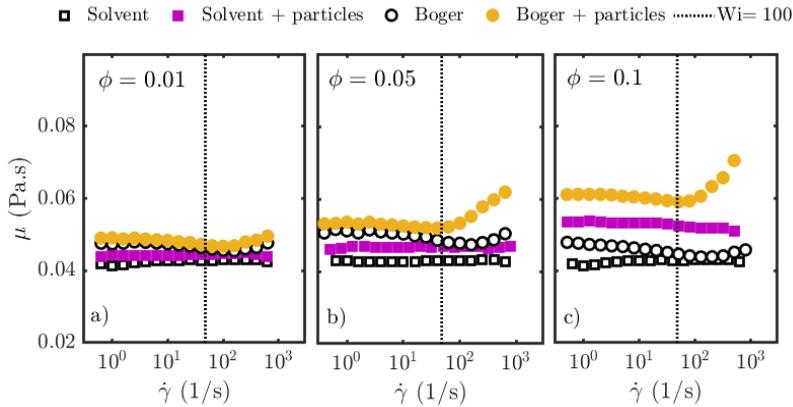


Figure 1: Steady shear viscosities, for particle-loaded solvent and particle-loaded Boger fluid, for all three values of ϕ , together with systematic characterisations of particle-free solvent and Boger matrix. Vertical dashed lines are plotted at $Wi=100$.

86 a to c. The suspensions in Boger fluids (full circles) exhibited constant viscosity for a
 87 wide range of shear-rates. An increase in viscosity was observed for shear rates above
 88 100 s^{-1} which could not be ascribed to inertial instabilities (which generally do not
 89 occur when the inner cylinder is fixed, as was the case here), but rather to purely elastic
 90 instabilities. The dashed lines in figure 1 highlight that this apparent thickening only
 91 occurs when the Weissenberg number exceeds 100 ($Wi = t_e \dot{\gamma}$, where $\dot{\gamma}$ is the strain rate
 92 and t_e is the relaxation time), in agreement with the results of Schaefer *et al.* (2018) at
 93 similar curvatures. A similar behaviour was also observed for particle free Boger fluids
 94 (empty circles on all sub-plots in figure 1), and for additional measurements performed
 95 with a plate-plate geometry (not reported here, see also Groisman & Steinberg (2004))
 96 confirming this hypothesis. The effective viscosity was then taken as the average viscosity
 97 value on the plateau region of the curve. Values for this average viscosity are reported
 98 in table 1, averaged on all tests at similar ϕ . Oscillatory-shear measurements performed
 99 with the same rheometer and geometry showed that the addition of particles did not
 100 modify the elastic and storage moduli G' and G'' of the liquid. The apparent elastic
 101 time-scale of the Boger fluid, which was estimated from the crossover point between G'
 102 and viscosity corrected G'' curves as detailed in Lacassagne *et al.* (2020), was thus not
 103 altered by the presence of particles and found equal to $t_e = 0.21 \text{ s}$.

104 The Taylor-Couette flow cell is displayed in figure 2 and is similar to the one used in
 105 Cagney *et al.* (2020); Lacassagne *et al.* (2020, 2021) (the reader may refer to those works
 106 for further details). The axial length was $H = 135 \text{ mm}$, and the inner and outer radii
 107 were $r_i = 21.66 \text{ mm}$ and $r_o = 27.92 \text{ mm}$, respectively. This corresponds to a gap width
 108 of $d = 6.26 \text{ mm}$, a radius ratio of $\eta = r_i/r_o = 0.776$, curvature ratio $\epsilon = d/r_i = 0.289$
 109 and an aspect ratio $AR = H/d = 21.56$ (figure 2), which places the setup in the large
 110 gap and high curvature limits. The particle nominal diameter was $d_p = 48 \mu\text{m}$. The
 111 gap to particle diameter ratio was $d/d_p = 131$, well in the small particle limit. Three
 112 types of experiments were performed: ramp-up (RU, acceleration of the inner cylinder),
 113 ramp-down (RD, deceleration) and steady state experiments (STS, constant rotation
 114 speed of the inner cylinder recorded for a given time span). RU and RD tests allowed the
 115 flow transitions and instabilities to be characterised over a continuous range of cylinder
 116 rotation speed and the nature of the bifurcations to be discussed. STS tests allowed a

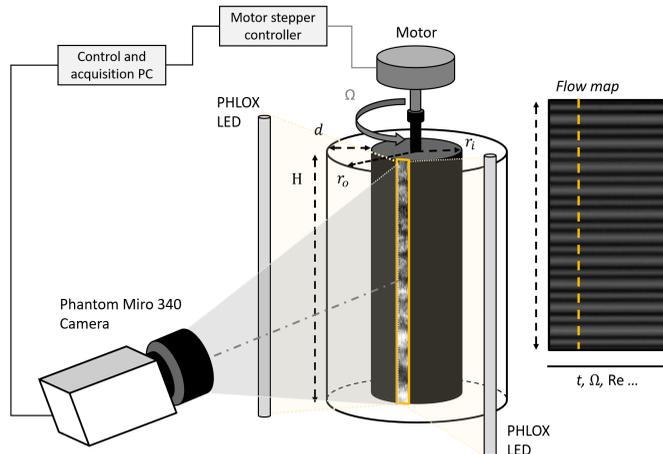


Figure 2: Schematic of the experimental set-up showing the Taylor-Couette cell, visualisation arrangement, and flow map construction.

117 specific flow state to be examined with greater temporal resolution. The rotation speed of
 118 the inner cylinder, Ω , and the co-responding Reynolds number defined as $Re = \rho \Omega r_i d / \mu$
 119 were the main control parameters in the experiments. The particle Reynolds number,
 120 $Re_p = \rho \Omega r_i d_p / \mu$, was $Re_p \ll Re$ and $Re_p \sim \mathcal{O}(1)$ at maximum Ω . Two other non-
 121 dimensional groups can be used to describe the experiments: the Weissenberg number,
 122 defined with respect to the average strain rate across the fluid, $Wi = t_e \Omega r_i / d$, and the
 123 Elastic number $El = Wi / Re$ which does not depend on Ω but solely on fluid properties. El
 124 ranged from 0.21 at $\phi = 0$ (see also Lacassagne *et al.* (2020)) to 0.28 at $\phi = 0.1$, due to
 125 the change in viscosity (see table 1). Acceleration or deceleration of the inner cylinder was
 126 performed in a quasi-steady fashion (with the non-dimensional rate $\Gamma_0 < 1$ as defined in
 127 table 1, see also Dutcher & Muller (2009); Lacassagne *et al.* (2021)). The flow structure
 128 was captured by adding a very small quantity (volume fraction of the order of 10^{-4} , with
 129 negligible effect on the flow (Gillissen *et al.* 2020)) of reflective flakes to the fluid (Pearl
 130 lustre pigments, L.Cornelissen & Son, United Kingdom) illuminating using a white light
 131 source (PHLOX, France) and imaging using a high speed camera (Phantom Miro 340,
 132 Vision Research, US) as detailed in previous works (Gillissen *et al.* 2020; Cagney *et al.*
 133 2020; Lacassagne *et al.* 2021) (see figure 2).

134 The acquisition frequency was chosen, such that it was sufficiently high to capture all
 135 frequencies of the flow while allowing the experiment to be recorded in a single run, con-
 136 sidering the limitations of camera memory. The recording frequencies and experimental
 137 parameters used with each working fluids for RU and RD experiments are summarized
 138 in table 1. STS experiments were recorded at a higher frequency than RU and RD
 139 experiments, 1000 fps. Flow maps and frequency maps were constructed with the protocol
 140 described in Lacassagne *et al.* (2021).

141 3. Results and discussion

142 3.1. Overview and transitions

143 The data presented in this section relates only to Boger fluids with particle loading.
 144 A sample transition sequence for $\phi = 0.1$ is presented in figure 3, where a) is the flow

| ϕ | μ (Pa s) | N_{RU} | N_{RD} | Γ_0 | f_{acq} (fps) |
|--------|-----------------|----------|----------|------------|--------------------|
| 0 | 0.0475 | 6 | 6 | 0.30 | 90 |
| 0.01 | 0.0494 | 6 | 5 | 0.35 | 200 |
| 0.05 | 0.0565 | 4 | 4 | 0.35 | 200 |
| 0.10 | 0.0627 | 7 | 4 | 0.31 | 180 or 250 |

Table 1: Summary of experimental parameter for ramp-up (RU) and ramp-down (RD) experiments. N_{RU} and N_{RD} correspond to the number of repeated experiments for RU and RD, respectively. $\Gamma_0 = \frac{dRe}{dt^*} = \frac{\rho^2 r_i d^3}{\mu^2} \frac{d\Omega}{dt}$ is the non-dimension acceleration rate, with $t^* = t/t_v$ the time scaled by the viscous time-scale $t_v = \rho d^2/\mu$.

map (Re-space diagram) for $\phi = 0.1$ during a RU experiment, b) is the corresponding frequency map, and c) and d) are flow maps from STS experiments performed at $Re=133$ and $Re=200$, respectively. e) shows frequency spectra extracted from b) and corresponding to flow states described in c) and d). Finally, f) and g) display flow and frequency maps corresponding to a) and b) but for a RD experiment. A visual difference in flow transitions between RU and RD can be noted, and will be discussed later.

In CF the time-space diagrams (a,f) are homogeneous, with all flakes oriented in the azimuthal direction. When TVF arises, the flakes orientation in relation to Taylor Vortices gives rise to a banded structure. CF (or TVF) are steady in time and not associated with any characteristic frequencies on the frequency map (figure 3 b,g), other than the inner cylinder rotation frequency, that is captured by the method. The end of CF is identified from the flow maps when spatial structures appear.

In the rotating spiral waves (RSW) regime, a base TVF structure is visible, but additional patterns appear due to axial non-axisymmetric elastic waves spiralling either upward or downward (Lacassagne *et al.* 2020) (figure 3 a, c, f). This results in additional and distinct ridges on the frequency maps (figure 3 b,g) that do not depend on Re , from the onset of which the critical Re for transition from/to RSW can be detected. The existence of TVF (that can be quite difficult to capture, see figure 3 a) thus spans from the appearance of spatial structures to the appearance of these ridges. They correspond to the temporal frequencies of RSW, i.e of the primary elastic instability, and their frequency scales as $f^k = k \times f_e$ with $f_e = 2c_e/\lambda$ the elastic frequency, $\lambda \simeq d$ a spatial wavelength, and $c_e = \sqrt{\mu/(\rho t_e)}$ the elastic wave celerity. The two first f^k frequencies are illustrated by horizontal dashed lines in figure 3 b and 3 g. Vertical dashed lines in figure 3 e for $Re=133$ denote the peaks corresponding to horizontal lines in figure 3 b. The related k values are reported in the figure caption.

Finally, in the elasto-inertial turbulence domain (EIT), the random alignment of flakes with a set of various spatial flow structures translates into an increasingly chaotic intensity signal and space-time plot (figure 3 a, d, f). The distinct peaks in the frequency maps that were present in RSW gradually merge into continuous spectra (figure 3 b, g, e). EIT thus consists in the appearance of spatial and temporal chaos on top of the organised TVF structure, through RSW and the multiplication of vortex merging and splitting events. Critical Re for RSW \leftrightarrow EIT transitions are identified from the frequency maps (figure 3b, g), when secondary RSW peaks can no longer be distinguished. Note that some of the spectral signature of RSW may persist into the EIT regime in the form of a consistent smoother peak (see figure 3 g), $Re>170$).

In RD experiments, an additional flow state is encountered in the form of upward spiralling vortices, and labelled SVF for Spiral Vortex flow (see figure 3 f). A summary

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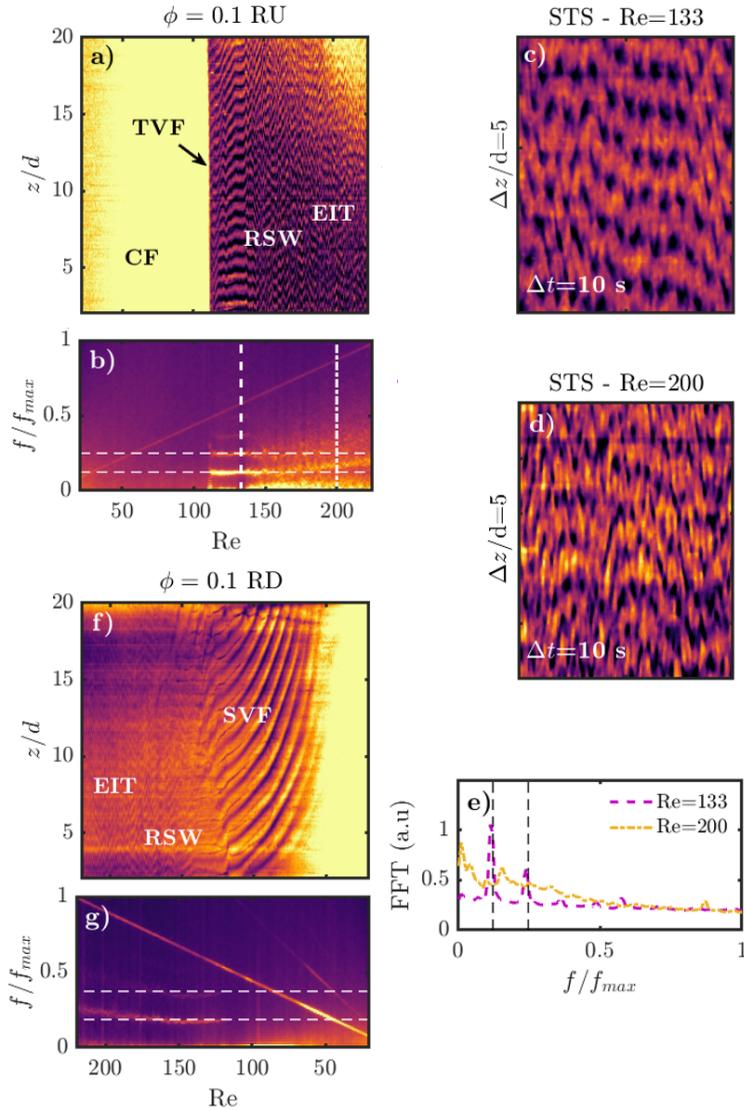
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Figure 3: Example of ramp-up (RU, a,b), steady state (STS, c,d), and ramp-down experiments (RD,f,g) for a $\phi = 0.1$ fluid (false colors). a,f) are Re-space diagrams (flow maps), b,g) are frequency maps, c) and d) are space time diagrams at fixed Re, and e) shows temporal spectra extracted from the b) frequency map at Re corresponding to c) and d). Horizontal dashed lines in b) and g), and vertical dashed lines in e) denote elastic wave frequencies $f^k = k \times f_e$ with $k = [\frac{1}{3}, \frac{2}{3}]$ and $k = [\frac{1}{2}, 1]$ for the two first peaks in RU (b,e) and RD (g) respectively.

182 of critical Re for transitions is provided in figure 4 for RU and RD experiments (sub-
 183 figures a and b, respectively). The experiments were repeated at least four times (see
 184 table 1) and excellent consistency on the succession of flow states was encountered. The
 185 reported visualisations correspond to single experimental runs, but critical Re values are

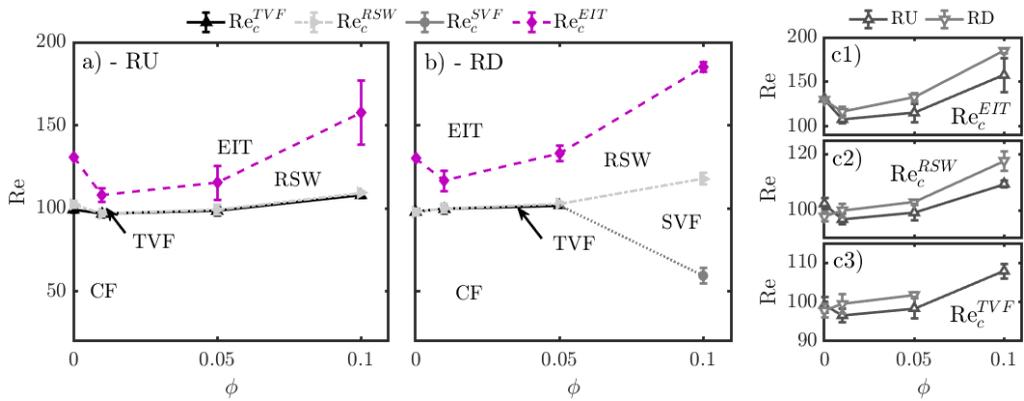


Figure 4: Critical Re - ϕ maps for transitions to TVF, RSW, EIT and SVF in RU (a) and RD (b) experiments. Hysteric behaviours are illustrated for transitions to/from EIT, RSW and TVF in sub-figures c1, c2 and c3, respectively (triangles pointing upwards for RU, downwards for RD).

186 averaged over all repeats, and the standard deviations over critical Re provide error bars
 187 for figure 4.

188 It can be seen that the addition of particles initially decreases the critical Re for the
 189 $CF \rightarrow TVF$ transition at the lowest particle volume fraction, but as ϕ is increased above
 190 0.01, the critical Re increases, stabilising the flow. The same trend is observed in figure 4
 191 b) for the RD experiments for $\phi < 0.1$. Note that in Newtonian suspensions, the addition
 192 of particles in the same volume fraction range mostly leads to a minor destabilisation
 193 of the CF with respect to TVF (Majji *et al.* 2018; Ramesh *et al.* 2019; Gillissen &
 194 Wilson 2019). The opposite trend observed here must therefore be attributed to the
 195 combination of particles and viscoelastic fluid matrix; while both properties in isolation
 196 tend to destabilise CF compared to the Newtonian case, they have the opposite effect
 197 when combined.

198 For the $\phi = 0.1$ RD experiments, SVF is observed at Re values much lower than the
 199 critical Re for CF - TVF transition in RU. This new state is illustrated in the flow map
 200 and corresponding frequency map of figure 5. It appears to co-exist with RSW in the
 201 Re range from 120 to 140 (figure 5 a), close-up in 5 b)). We also note that SVF is not
 202 associated with any spectral signature on its own: the frequency map in the Re range of
 203 20-120 is similar to that expected for TVF (figure 5 c)). Such spiralling behaviour was
 204 previously reported in particle suspensions in Newtonian fluids in RD (Majji *et al.* 2018)
 205 but also RU (Ramesh *et al.* 2019; Ramesh & Alam 2020), sometimes inter-penetrating or
 206 co-existing with other flow states (Majji *et al.* 2018; Ramesh & Alam 2020; Majji *et al.*
 207 2018). The fact that the new state is found only in RD tests suggests a modification of
 208 the nature of primary instabilities in particle loaded Boger fluids at non-dilute volume
 209 fractions ($\phi \geq 0.05$). SVF is unlikely to be caused by buoyancy or particle migration
 210 effects, since it arises when ramping down from chaotic states (EIT-RSW) in which
 211 particles are expected to be well mixed by strong axial flow velocity fluctuations. The co-
 212 existence of flow states, which was already observed for particles in Newtonian solvents
 213 (Ramesh *et al.* 2019; Ramesh & Alam 2020; Dash *et al.* 2020), is for the first time reported
 214 here for particle suspensions in Boger fluids.

215 The higher order transition to RSW (4 a and b) arises very soon after the onset of
 216 TVF (Lacassagne *et al.* 2020). After a slight destabilisation at $\phi = 0.01$, a stabilising

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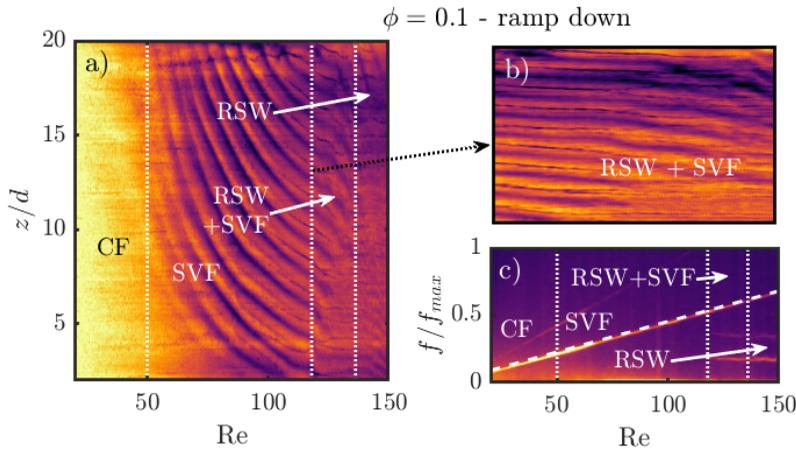


Figure 5: Illustration of the SVF state for RD experiments at $\phi = 0.1$, on the flow map (a) and frequency map (c) (focus from figure 3 f and g). Vertical dotted lines highlight transitions from RSW, RSW+SVF, SVF and CF from right to left (decreasing Re). A close-up of the frequency map in the coexisting state range RSW+SVF is provided in sub-figure b (Re axis ranging from 118 to 136, z/d axis from 5 to 20).

217 effect by particle addition is again reported, with critical Re values increasing with ϕ .
 218 RD results in figure 4 b) follow the same trend. Averaging on all experiments, TVF has
 219 a very narrow Re range of existence $\Delta Re_{TVF} \sim 1$ with yet $\Delta t_{TVF} > 10 \times t_e$. It is the
 220 first in a series of transitions leading to more complex flow states. In some higher ϕ cases,
 221 TVF can sometimes not be seen clearly (figure 3 a) and the primary transition could be
 222 either $CF \leftrightarrow TVF$ or $CF \leftrightarrow RSW$ within the margin of error of this study. The results thus
 223 suggest that increasing particle concentration reduces ΔRe_{TVF} , promoting CF-RSW as
 224 the primary instability upon particle addition. However a precise understanding of this
 225 effect calls for a more accurate investigation in the $Re = [100-120]$ range.

226 For the RSW to EIT transition, the trends for critical Re are globally similar to those
 227 previously reported for transition to RSW, i.e. a destabilisation by $\phi = 0.01$ followed
 228 by a stabilisation both in RU and RD cases, upon increased ϕ . This non-monotonic
 229 trend is more pronounced for the $RSW \leftrightarrow EIT$ transition compared to those observed for
 230 lower order transitions. The combined effects of particles and viscoelasticity, which would
 231 have been expected to separately lead to earlier second order flow transitions, here again
 232 appear to delay transition to chaotic patterns.

233 3.2. Effect of particle loading on RSW and EIT properties

234 The effects of particle loading on EIT features can be characterised using spatio-
 235 temporal flow properties at a constant Reynolds number. Figure 6 shows two dimensional
 236 FFTs in time and space of STS experiments. Peaks of such spectra correspond to
 237 dominant time and length-scales of the flow. RSW is described by a set of discrete and
 238 identifiable peaks in space but also in time (see for example figure 6 c). On the other
 239 hand, EIT displays a broadband behaviour characteristic of a turbulent state, with no
 240 distinct peak (see e.g. figure 6 b). The temporal spectra projected on upper-right panels
 241 allow to distinguish between RSW (clear temporal peak, c) and EIT (no clear temporal
 242 peak, a,b,d). Figure 6 shows that the collapse of RSW spectra into broadband EIT, which
 243 occurs as Re is increased, is delayed by the increase in ϕ . In the $\phi = 0.01$ case (top line)

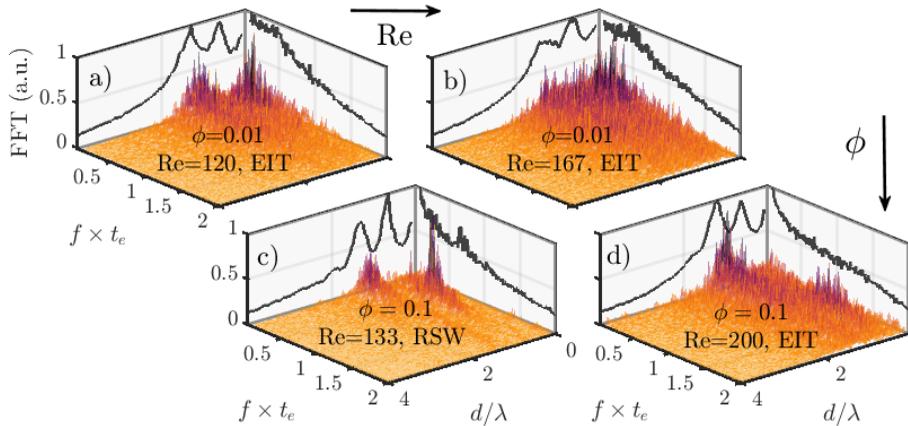


Figure 6: Two dimensional FFTs (time and space) of STS experiments for $\phi = 0.01$ (a,b) and $\phi = 0.1$ (c,d). Top left and top right panels on each sub-figure display mean spectra in the frequency and space dimensions, respectively. The spatial wavelength axis is scaled by the gap size d and the temporal frequency axis by $1/t_e$.

244 Re=167 (b) already corresponds to a turbulent signature without peaks, while for $\phi = 0.1$
 245 (bottom line), peaks are still visible at Re=200 (d), although they are less distinct than
 246 at Re=133 (c). In other words, the presence of particles delays the transition to EIT,
 247 as previously observed, but also preserves the large scale spatial structure of RSW into
 248 EIT.

249

3.3. Hysteretic behaviour

250

At $\phi = 0$, critical Re for CF-TVF and TVF-RSW transitions are higher for RU
 251 experiments than for RD experiments (see figure 4 c2 and c3). This is the signature
 252 of a (moderately) sub-critical bifurcation (Martínez-Arias & Peixinho 2017). Particle
 253 addition reverses the hysteresis; even at the lower ϕ values, the critical Re values in RD
 254 experiments become larger than those found in RU tests, for both transitions. The flow
 255 transitions back to lower order states at higher Re that are seen in the RU tests, and the
 256 difference in critical Re values due to this reversed hysteretic behaviour increases with
 257 the order of the transition (larger for RSW-EIT transition than for CF-TVF transition),
 258 and with increasing ϕ .

259

The origin of such a reversed hysteretic behaviour may, at first, be attributed to elastic
 260 or inertial particle migration. Indeed, particles migrating away from the inner cylinder
 261 in CF during RU tests would induce lower inner viscosity and higher Re, leading to a
 262 lower apparent critical Re in ramp up compared to the ramp down case where particles
 263 are expected to be evenly dispersed and the viscosity homogeneous. This is in qualitative
 264 agreement with a similar reverse hysteresis observed by Ramesh *et al.* (2019) for the
 265 CF-TVF primary transition in Newtonian particle suspensions, suggesting that inertial
 266 migration may play a role. Moreover, the shortest time-scale at which elastic migration
 267 effects would arise, estimated according to the modelling of D'Avino *et al.* (2017), is found
 268 to be of about 50 s, comparable to and even shorter than the typical times particles spent
 269 in CF during a RU experimental protocol. Thus, elastic migration may also be at play
 270 when considering primary instabilities.

271

However, a stronger reversed hysteresis is observed for higher order RSW \leftrightarrow EIT tran-
 272 sition, for which particles are expected to be well mixed in both states, which suggests

that migration alone cannot explain the observed hysteretic phenomena. This new and striking result suggests that the particles act on elasto-inertial patterns with mechanisms other than migration, and more importantly that this action corresponds to a damping or attenuation of elasto-inertial features. Recent findings on local stress concentration and elastic thickening (see e.g. Yang & Shaqfeh (2018*a,b*)) in particles suspended in viscoelastic media might further explain this macroscopic behaviour.

4. Summary and conclusion

The results reported in this work show that particle addition to Boger fluids can significantly affect the elasto-inertial transitions and patterns in TC flow. Firstly, it tends to globally stabilise flow states with respect to the first and second order transitions, and delays the onset of elasto-inertial turbulence, thus stabilizing flows (after a small destabilisation in very dilute suspensions). Secondly, it modifies the spectral signature of EIT, by promoting energy concentration in large scale steeper peaks. Finally, it modifies the nature of flow transitions, with a reverse hysteresis behaviour and the occurrence of SVF in RD experiments.

All the previous observations underpin a damping of elastoinertial features by the presence of particles: a delay of their onset with increasing ϕ , a reduction of EIT chaotic features at constant Re for increased ϕ , and their reduction leading to a reverse hysteretic behaviour. An explanation for this could be that of an elastic thickening mechanism, that is to say an increase in viscosity associated with polymer-particle interactions. This phenomenon is due to the local elongation of polymer chains in inter-particle gaps, where strong shear or strain rates can be encountered; this leads in turn to strain hardening, a local increase in extensional viscosity (see for example Yang & Shaqfeh (2018*a,b*)) and a global increase in shear-viscosity.

Combining the presence of particles and viscoelasticity, which on their own would be expected to lead to flow destabilisation does not necessarily lead to stronger destabilisation. On the contrary, the destabilising effect of one complex fluid property may be cancelled out or reversed by the presence of another such property, as has recently been illustrated for the competition between shear-thinning and viscoelasticity (Lacassagne *et al.* 2021). Future work on this topic should in our opinion be focused on bridging the gap between local observation at the particle scale (Yang & Shaqfeh 2018*a,b*) and global flow characterisation in complex conditions and with non-negligible inertia. Further large scale experiments with various polymer chain extensional properties, together with the measurement of the shear-and strain rates in particle-free or particle loaded RSW and EIT flows, could bring further understanding on the role of extensional or elastic thickening. Practical considerations and industrial applications might also call for studies of particle suspensions at higher volume fractions, or higher blockage ratio (lower d_p/d ratio) for which particle particle interactions may become dominant (Royer *et al.* 2016).

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Declaration of interests

The authors report no conflict of interest.

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