

1 **Encapsulation of cesium with a solid waste-**
2 **derived sulfoaluminate matrix: a circular**
3 **economy approach of treating nuclear**
4 **wastes with solid wastes**

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6 Jingwei Li[†], Dong Xu[†], Xujiang Wang[†], Kang Liu^{††}, Yanpeng Mao[†], Mengmeng
7 Wang^{††}, Yun Bai^{†††}, Wenlong Wang^{†*}

8 [†]Shandong Engineering Laboratory for Solid Waste Green Materials, National
9 Engineering Laboratory for Reducing Emissions from Coal Combustion, Engineering
10 Research Center of Environmental Thermal Technology of Ministry of Education,
11 Shandong Key Laboratory of Energy Carbon Reduction and Resource Utilization,
12 School of Energy and Power Engineering, Shandong University, Jinan 250014, China

13 ^{††}State Key Joint Laboratory of Environment Simulation and Pollution Control, School
14 of Environment, Tsinghua University, Beijing 100084, China

15 ^{†††}Department of Civil, Environmental and Geomatic Engineering, University College
16 London, Gower Street, London, WC1E 6BT, UK

17 *** Corresponding Author**

18 **E-mail address:** wwenlong@sdu.edu.cn

19

20 **Abstract**

21 It is of great importance to safely dispose nuclear wastes with the development of
22 nuclear industries. Past approaches to this problem have included immobilizing
23 radioactive cesium in Portland cement-based matrices; however, the leaching rates of
24 cesium are relatively high, especially as the leaching temperature increases. This paper
25 explores a high-efficiency and cost-effective approach for encapsulating cesium using
26 a sulfoaluminate cement (SAC) matrix, which was prepared *via* synergetic use of
27 industrial solid wastes. Leaching results showed that, the apparent diffusion coefficient
28 values of cesium were only $\sim 1.4 \times 10^{-15} \text{ cm}^2/\text{s}$ and $\sim 5 \times 10^{-18} \text{ cm}^2/\text{s}$ at 25 °C and 90 °C
29 leaching conditions, respectively. These values were several orders of magnitude lower
30 when compared with previously reported values, indicating the excellent encapsulation
31 performance of the solid-waste-based SAC for cesium. Moreover, the heavy metals
32 contained in the industrial solid waste were also effectively immobilized. A mechanistic
33 analysis revealed that cesium was encapsulated in the SAC matrices stably by a physical
34 effect. Finally, a life cycle assessment and economic analysis indicated that this
35 approach was environmental-friendly, cost-effective, and energy-saving. This work
36 provides a promising strategy for effective encapsulation of cesium and synergetic
37 treatment of industrial solid wastes.

38 **Keywords:** Cesium; Sulfoaluminate matrix; Industrial solid wastes; Encapsulation;
39 Environmental-friendly

40 **1 Introduction**

41 The safe and harmless disposal of continuously growing nuclear wastes has

42 become an unavoidable problem in the field of energy and environment[1,2]. Take
43 Europe as an example, the estimated amount of nuclear waste in European nuclear
44 facilities during the lifetime of a given reactor is even greater than 6.6 million m³[3].
45 Radioactive cesium (Cs) is one of the most problematic radionuclides contained in
46 nuclear wastes, owing to its high volatility, high mobility and relatively long half-life
47 of approximately ~ 30 years[4]. Although extensive studies have been conducted to
48 understand how to reduce the leachability of radioactive Cs from commonly used
49 Portland cement (PC) matrices, relatively high leaching rates are still reported,
50 especially as the leaching temperature increases[5-8]. Considering the serious
51 environmental impacts of radioactive Cs[9-11], and its safe, long-term immobilization
52 of radioactive Cs under the exothermic conditions present in the repository[12], it
53 remains extremely urgent to develop more efficient immobilization approaches.

54 Recent studies have found that sulfoaluminate cement (SAC) may be a better
55 matrix than PC for the immobilization of radioactive substances[13-17]. For instance,
56 Sun et al.[14] detected both lower cumulative leaching fractions and leaching rates for
57 Cs while using SAC matrices to treat radioactive resins. Relatedly, Coumes et al.[16]
58 found that blending SAC with PC increased the waste loading of low-level radioactive
59 slurries to 56%, and reduced the number packages produced by a factor of 1.8. The
60 superiority of SAC immobilization is primarily attributed to its main hydration
61 product—ettringite ($3\text{CaO}\cdot\text{Al}_2\text{O}_3\cdot 3\text{CaSO}_4\cdot 32\text{H}_2\text{O}$). Ettringite is of particular interest to
62 waste solidification due to its propensity to incorporate mobile ions and produce
63 “crystal interlocking” effect by its needle-like crystal structure[13-18]. However,

64 systematic research into the immobilization characteristics and mechanisms of how
65 SAC interacts with radioactive substances under various conditions remains lacking.
66 Additionally, the shortage of high-grade raw materials for manufacturing SAC along
67 with its high production costs has significantly restricted its production and application,
68 in particular, in nuclear waste treatment[19-21].

69 At the other end of the spectrum, global urban wastes are statistically in the range
70 of 7 to 10 billion tons per annum[22]. However, controlled disposal rates are often well
71 below 50% overall in low-income areas, indicating that innovative resource recovery
72 technology is urgently needed[22]. Previous work from our laboratory showed that the
73 synergetic-complementary use of industrial solid wastes can potentially produce a high-
74 performance SAC[20]. Using this high-performance SAC, products that are
75 economically efficient, environmentally friendly can then be manufactured with great
76 potential for various industrial applications[20,21,23-30]. However, there are few
77 studies that have explored the combination of solid waste-derived SAC matrix and
78 nuclear waste disposal.

79 Presented here is an innovative, technical approach for solidifying nuclear wastes
80 using solid waste-derived SAC. The SAC material was first prepared by synergetic-
81 complementary use of industrial solid wastes, which was then employed to encapsulate
82 a simulated Cs. The leaching kinetics of Cs and the synergetic immobilization
83 characteristics of heavy metals contained in the matrix were investigated. The
84 encapsulation mechanisms of Cs were studied using X-ray diffraction (XRD), X-ray
85 photoelectron spectroscopy (XPS), and electron probe microanalysis (EPMA). Finally,

86 the safety, feasibility, and economics of this approach were assessed by both a life cycle
87 assessment and economic analysis. Collectively, this study showed the coordinated
88 digestion of industrial solid waste and nuclear waste, which supports current trends
89 towards green chemistry and a circular economy.

90 **2 Materials and methods**

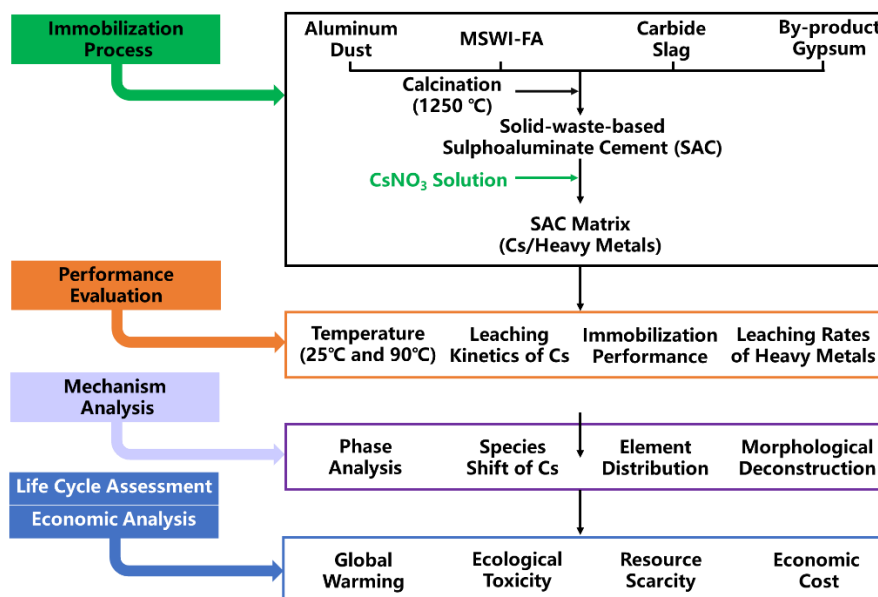
91 **2.1 Materials and reagents**

92 Cesium nitrate (CsNO_3) powder was used as the simulant for radioactive Cs; to
93 prepare it for use in the solidification experiment, it was first dissolved in deionized
94 water according to previously published methods[4,8,31,32]. The chemical reagents
95 used in this study were all of analytical grade and were purchased from Aladdin
96 Biochemical Technology Co., Ltd. De-ionized water was used for the preparation and
97 dilution of all chemical solutions. To prepare SAC, five kinds of industrial solid wastes
98 were used with complementary matching of ingredients. Wastes were obtained as
99 follows: (i) MSWI-FA was obtained from Zichuan Waste Incineration Plant (Shandong,
100 China), (ii) desulfurization gypsum was supplied by Liaocheng Coal-fired Power Plants
101 (Shandong, China), (iii) aluminum dust and (iv) titanium gypsum were both supplied
102 by the XinFa Group (Shandong, China), and (v) carbide slag was obtained from
103 Liaocheng Acetylene Company (Shandong, China). The X-ray fluorescence (XRF) and
104 XRD results for the raw materials are presented in Table S1 and Figure S1, respectively.
105 The concentration distributions of heavy metals in solid wastes are given in Table S2.

106 **2.2 Experimental procedure**

107 The schematic overview of the investigations carried out in this paper is shown in

108 Figure 1. Briefly, two solid-waste-based SACs (M1 and M2) were first prepared *via* a
 109 synergetic-complementary approach (a detailed procedure is provided in Table S3)
 110 using the above mentioned industrial solid waste materials. The mineral compositions
 111 of M1 and M2 are shown in Figure S2. The prepared SAC was then mixed with CsNO₃
 112 solution to prepare a mixed paste with a water-to-binder ratio of 0.3. The Cs
 113 concentration was fixed at 3% of Cs/hardened paste by mass. The fresh paste was then
 114 cast into cylinder molds (internal diameter = 20 mm, and internal height = 18 mm) and
 115 de-molded after 24 h. The de-molded cylinder sample was cured at 95% humidity and
 116 20 ± 2°C for 28 d before the leaching test. The leaching test was conducted according
 117 to ANSI/ANS-16.1- 2003[31,33], and the leaching intervals were set at 2 h, 7 h, 24 h,
 118 2 d, 3 d, 4 d, 5 d, 19 d, 47 d, and 90 d. The leaching characteristics of Cs and the heavy
 119 metals from different SAC matrices (M1 and M2) at different leaching temperatures
 120 (25°C and 90°C) were then investigated. It should be noted that 90°C was employed
 121 here to simulate the high temperature which could potentially occur during the decay
 122 of radionuclides in the nuclear waste repository.



123

124 **Figure 1.** Schematic overview of the investigations undertaken in this study

125 **2.3 Method of evaluating cesium encapsulation**

126 To measure the long-term leaching behavior of Cs, cumulative leaching fraction
127 (*CLF*) and leaching rate (*LR*) were calculated according to the equations defined in the
128 literature as shown below in Eq. (1) and Eq. (2), respectively[14].

$$129 \quad CLF = \left(\frac{\sum A_n}{A_0} \right) \left(\frac{V}{S} \right) \quad (1)$$

$$130 \quad LR = \left(\frac{A_n}{A_0} \right) \left(\frac{V}{S} \right) \left(\frac{1}{t_n} \right) \quad (2)$$

131 In addition, apparent diffusion coefficient (*D*) is calculated according to Eq. (3)
132 which could potentially be used to predict the long-term leaching behavior of Cs[14].

$$133 \quad D = \pi \left(\frac{mV}{2S} \right)^2 \quad (3)$$

134 where A_n is the mass of leached Cs at the n th interval, mg; A_0 is the total original
135 mass of Cs in the specimen, mg; V is the volume of the specimen, cm^3 ; S is the
136 surface area of the specimen, cm^2 ; t_n is the duration of the n th interval, d; m is the
137 slope of the straight line of the plot of $(\sum A_n/A_0)$ versus $(t_n)^{1/2}$.

138 **2.4 Analytical methods**

139 The mass concentrations of Cs and 8 heavy metals (As, Zn, Pb, Cd, Ni, Mn, Cr,
140 and Cu) in the leachates were determined using an inductively coupled plasma optical
141 emission spectroscopy (ICP-OES; PerkinElmer Optima 7000DV, PE, USA). The pH
142 values of all collected leachates at the end of each leaching interval were determined
143 using a conventional pH analyzer (PHS-25, Lei-ci, China). The mineral phases of Cs-
144 doped samples, raw materials, SAC clinkers and SAC hydration products were
145 characterized by X-ray diffraction (XRD; Rigaku Dmax-2500 PC, Rigaku, Japan) using

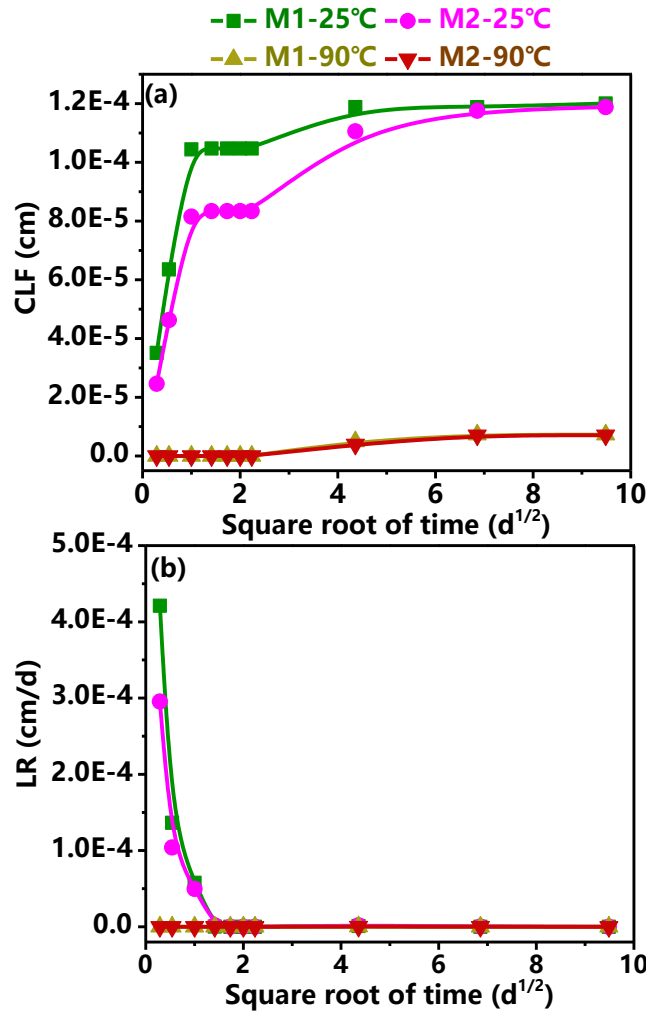
146 Cu-Ka radiation with 50 kV voltage, 100 mA current, and a scanning speed of 2.4°/min
147 over a range of 5°-65°. The morphologies and structures of Cs-doped samples were
148 characterized with scanning electron microscopy coupled with an energy dispersive
149 spectrometer (SEM/EDS; Zeiss Supra 55, Carl Zeiss MERLIN Compact, Germany).
150 The chemical shift of Cs in the Cs-doped samples was analyzed using an X-ray
151 photoelectron spectroscopy analyzer (XPS; AXIS Supra, Shimadzu, Japan). The
152 distributions of Cs and heavy metals in the Cs-doped samples were then characterized
153 using a field emission electron probe microanalyzer (FE-EPMA; JXA-8530F Plus,
154 JEOL, Japan). Life cycle assessment was conducted using SimPro ReCiPe2016 H 1.01
155 model.

156 **3 Results and discussion**

157 **3.1 Leaching characteristics and kinetics of cesium**

158 As shown in Figure 2a, the cumulative leaching fraction (*CLF*) values of Cs⁺ at 90
159 °C for M1-25°C, M2-25°C, M1-90°C, and M2-90°C were 1.20×10^{-4} cm, 1.19×10^{-4} cm,
160 7.26×10^{-6} cm, and 7.06×10^{-6} cm, respectively. The *CLF* values presented here were
161 much lower than the required value of 4×10^{-3} cm as per the GB 14569.1-2011 (Chinese
162 standard for cement waste form)[34,35]. This result indicates that the solid-waste-based
163 SAC has a good effect on immobilizing Cs which can satisfy the requirements for
164 industrial applications. In addition, M2 showed a better immobilizing effect on Cs,
165 which had higher compressive strengths than M1 (as shown in Table S4). This finding
166 implies that high mechanical strength is beneficial to the encapsulation of Cs. Notably,
167 the *CLF* values at 90 °C condition were two orders of magnitude lower than those at

168 the 25 °C condition.



169

170 **Figure 2.** (a) Cumulative leaching fraction, (b) Leaching rate of Cs from the SAC

171 matrices

172 As shown in Figure 2b, the leaching of Cs at 25°C mainly occurred on the first

173 day, with the leaching rate (*LR*) values decreasing quickly in subsequent time points.

174 However, a small amount of Cs also leached beyond day 5. In contrast, no Cs leaching

175 was detected in the first five days at 90°C condition; moreover, the *LR* values

176 remained at very low levels during the entire leaching test. Although Cs leaching was

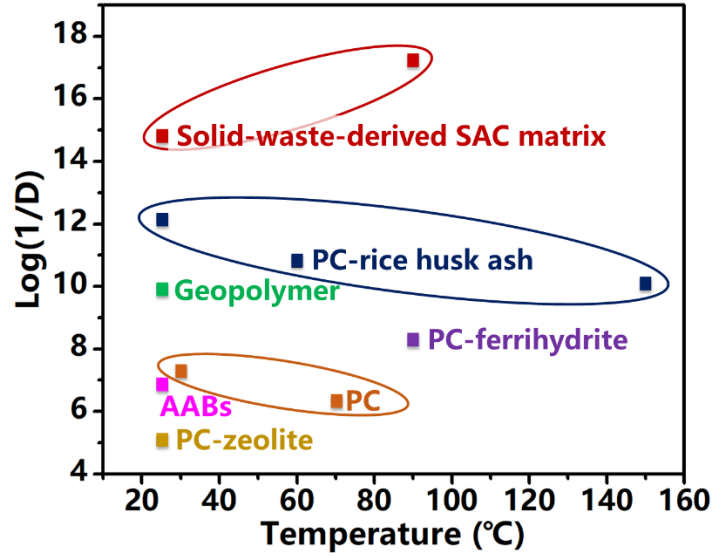
177 detected from days 19-47, the overall leaching amount remained very low.

178 Based on the results presented in Figure 2, it can be concluded that when the SAC
179 matrix was leached at 25°C, an initial fast leaching of Cs occurred during the first period
180 followed by a slow leaching in subsequent periods. However, when the SAC matrix
181 was leached at 90°C, a slow leaching of Cs was observed during entire periods.

182 Given these findings, the leaching patterns are divided into two regions: Region I
183 (2 h-1 d) and Region II (5-90 d). According to work reported in the literature[6], the
184 controlling leaching mechanism is determined by the slope (k) of the linear regression
185 of $\log CLF$ versus $\log t$ (Table S5), with lower k values reflecting lower leaching.
186 In terms of the leaching at 25°C, the k values for Regions I and II were 0.35-0.65 and
187 less than 0.35, respectively. These findings indicated that the corresponding mechanism
188 of Cs leaching from the studied matrices was a diffusion mechanism and a surface
189 wash-off mechanism, respectively[6,14]. In the case of leaching at 90°C, the k values
190 for Region II were less than 0.35, indicating the surface wash-off mechanism dominated
191 the leaching of Cs[6,14]. These results implies that even at 90°C the SAC matrices
192 could still maintain a good encapsulation of Cs.

193 **3.2 Encapsulation performance on cesium**

194 Numerous researches have studied the Cs leachability from various matrices,
195 including PC, SAC, alkali-activated blends (AABs), and geopolymer[5-7,14,31,36-39].
196 Previous studies evaluated the leaching behavior of nuclides from different matrices by
197 calculating the apparent diffusion coefficient (D) using Fick's second law[5,36], where
198 lower D values are related to reduced leaching of Cs from the matrices.



199
 200 **Figure 3.** Comparison of Cs encapsulation performance of the SAC matrix in
 201 this work and the various matrices in previous literatures

202 To intuitively compare the Cs encapsulation performance of the mentioned
 203 matrices, the logarithm of the fractional number of the D values reported in previous
 204 studies and those obtained in current work were calculated using Eq. (3) and plotted
 205 together in Figure 3. As presented, the D values of Cs for M1-25°C, M2-25°C, M1-
 206 90°C, and M2-90°C were calculated to be $1.45 \times 10^{-15} \text{ cm}^2/\text{s}$, $1.42 \times 10^{-15} \text{ cm}^2/\text{s}$, $5.33 \times$
 207 $10^{-18} \text{ cm}^2/\text{s}$, and $5.05 \times 10^{-18} \text{ cm}^2/\text{s}$, respectively. The calculated values of the solid-
 208 waste-based SAC in this work are obviously higher than other materials. This result
 209 showed that the D values in this study were several orders of magnitude lower when
 210 compared with previously reported values despite the different leaching test conditions.
 211 Therefore, the solid-waste-based SAC has clearly demonstrated its capacity in
 212 improving the encapsulation performance on Cs as compared with other studied
 213 materials.

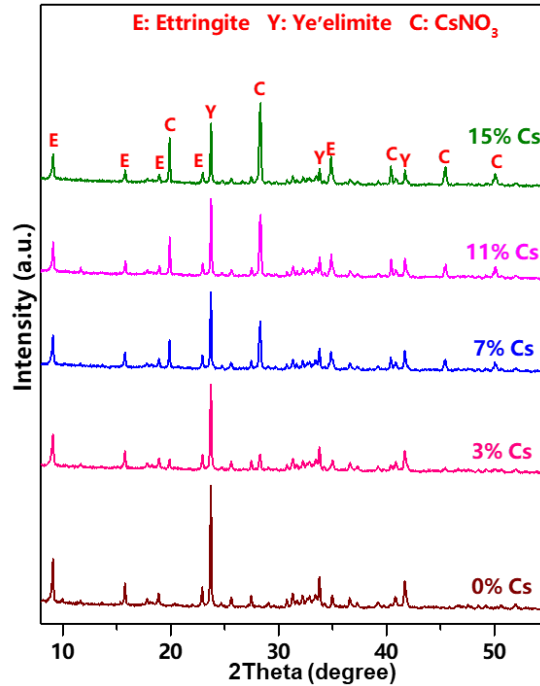
214 As shown in Figure 3, the Cs encapsulation performance of PC-based matrices

215 decreased as the test temperature increased. In El-Dakroury et al.'s study[7], the D
216 values increased from $6.3 \times 10^{-13} \text{ cm}^2/\text{s}$ to $8.1 \times 10^{-11} \text{ cm}^2/\text{s}$ when the leaching
217 temperature changed from 25°C to 150°C . Similar results were also obtained in
218 Papadokostaki et al.'s study on investigating the leachability of Cs from PC-based
219 matrices at different temperatures[5]. However, in the current work, the D values
220 decreased by three orders of magnitude as the temperature changed from 25°C to 90°C ,
221 representing a significant reduction in the leaching of Cs. Therefore, it could tentatively
222 conclude that the solid-waste-based SAC could be a suitable for treating Cs containing
223 wastes at high temperature conditions.

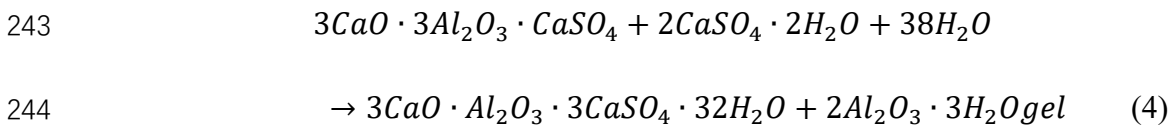
224 **3.3 Mechanism for cesium encapsulation**

225 Figure 4 presents the XRD patterns of Cs-doped samples containing different
226 amounts of Cs at the age of 3 days. It should be noted that higher contents of Cs were
227 doped in these samples in an attempt to facilitate the understanding of the encapsulation
228 mechanisms involved with SAC matrices. The XRD results showed that the appearance
229 of the diffraction peaks of E and Y which could be attributed to the hydration of SAC
230 (Eq. (4)). With the increasing Cs, the main diffraction peaks of CsNO_3 became obvious.
231 No other new peaks appeared, which indicated that the incorporation of Cs in SAC
232 might be a physical effect. This hypothesis could be well corroborated by the study
233 reported by R.O.Abdel Rahman et al.[40], in which they found that Cs existed as free
234 ions in the interstitial pore fluid as well as in the intermolecular channels in ettringite
235 and C-S-H structures, contributing to the physical entrapment of Cs within the cement–
236 bentonite matrices. The XPS spectra of Cs (Figure S3) indicated that Cs also did not

237 undergo any chemical shifts during the SAC hydration process (1h - 3d). This finding
 238 confirmed that the incorporation of Cs in the SAC-based matrix could be a physical
 239 effect.

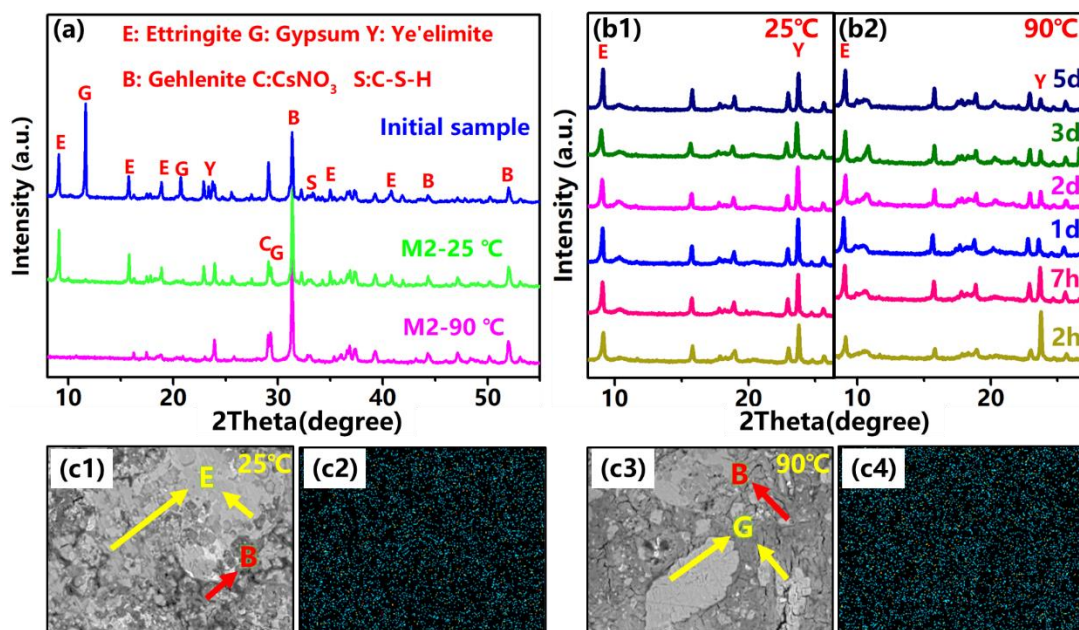


240
 241 **Figure 4.** XRD patterns of Cs-doped samples containing different amounts of Cs at 3d
 242 hydration period



245 The influence of temperature on the Cs encapsulation process was explored
 246 (Figure 5a and Figure 5b). As shown in Figure 5a, remained ye'elimite
 247 ($3CaO \cdot 3Al_2O_3 \cdot CaSO_4$, $C_4A_3\hat{S}$) and gypsum in the initial Cs-doped sample have hydrated
 248 to form ettringite after 90d leaching test at 25°C. The needle-like and prismatic structure
 249 of ettringite in the samples after leaching test at 25°C condition is shown in Figure S4.
 250 Past work has implicated this structure as a causal agent in crystal interlocking[41],
 251 reducing permeability and enhancing the ion encapsulation effects of the matrices.

252 Therefore, the leaching rates of Cs at the 25°C leaching condition decreased rapidly
 253 during the first day, and gradually decreased even further from day 1 to 90. The EDS
 254 data of Cs in Figure S4 also implied that there was almost no selectivity in the
 255 encapsulation positions of Cs in the solid-waste-based SAC.



256
 257 **Figure 5.** (a) XRD patterns of M2 samples before and after leaching test; (b) XRD
 258 patterns of SAC samples curing at 25°C and 90 °C conditions; (c) EPMA mapping of
 259 M2 samples after leaching test

260 Compared with Figure 5b1, the peaks of ye'elimite in Figure 5b2 were notably
 261 decreased from 2 h to 5 d at the 90°C leaching condition, indicating further hydration
 262 of ye'elimite. Past work has also confirmed that increasing curing temperature can
 263 promote ye'elimite hydration[42-44]. The higher early-age pH values (9.5-12) of the
 264 leachates at the 90°C leaching condition compared to those (7.7-11) at the 25°C
 265 leaching condition (Figure S5) also implied the rapid hydration speed of ye'elimite at
 266 the 90°C leaching condition. Meanwhile, C-S-H density in the samples was increased

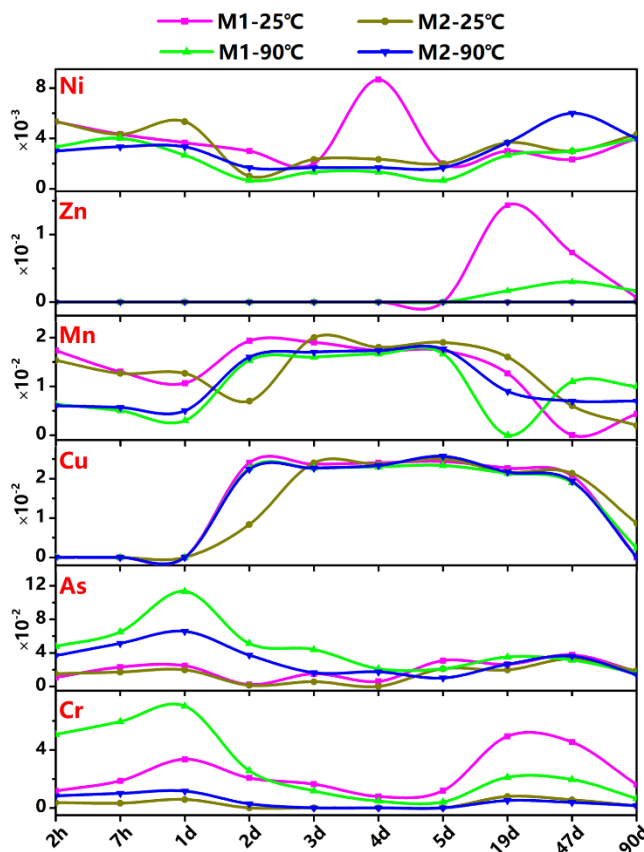
267 with its ongoing hydration at elevated temperatures[45], and its polymerization was
268 increased[46]. Taken together, these results indicated the low leaching of Cs at the early
269 stage of the 90°C leaching condition.

270 However, the ettringite peaks were notably decreased and disappeared after 90d
271 leaching test at 90°C. Previous study found that, ettringite started to convert to AFm
272 ($3\text{CaO}\cdot\text{Al}_2\text{O}_3\cdot\text{CaSO}_4\cdot 12\text{H}_2\text{O}$, monosulfoaluminate) and converted to gypsum and an
273 amorphous phase containing aluminum[47]. The backscattered electron images (Figure
274 5c1 and Figure 5c3) and SEM/EDS results (Figure S4) indicated that, ettringite in the
275 Cs-doped samples decomposed at the 90°C condition, and the remained minerals were
276 mainly gypsum, amorphous phase containing aluminum, some traces of AFm and C-S-
277 H gel. This result is consistent with those from previous studies which showed that
278 ettringite was unstable and decomposed at high temperatures[48-50]. However, it seems
279 the phase change of ettringite did not influence the distribution characteristics of Cs in
280 the samples (Figure 5c2 and Figure 5c4). The remained C-S-H and decomposition
281 products of ettringite probably contributed to the subsequent encapsulation of Cs in
282 SAC-based matrices at 90°C leaching condition.

283 **3.4 Synergetic immobilization effect on incorporated heavy metals**

284 To investigate the synergetic immobilization effects of heavy metals by the solid-
285 wastes-based SAC during the leaching tests, the mass concentrations of heavy metals
286 in the leachates were analyzed (Figure 6). Generally, the M2 matrixes—with its higher
287 compressive strength when compared with M1—had lower leaching of heavy metals.
288 The leached Cr and As concentrations were notably higher at the 90°C condition;

289 comparatively, the leaching concentrations of Ni and Mn were slightly higher at the
 290 25°C condition. The leaching concentrations of Cu were not affected by leaching
 291 temperature; no leached Zn was detected in the early stage at both the 25°C and 90°C
 292 conditions.



293

294 **Figure 6.** Mass concentrations of heavy metals in the leachates (mg/L)

295 The leaching concentrations of Zn, Mn, As, Ni, and Cu at the 25°C and 90°C
 296 conditions were all much lower than the limits specified in the Chinese integrated
 297 wastewater discharge standard GB 8978, U.S. EPA TCLP guidelines, and European
 298 landfill directive for non-hazardous waste (Table S6)[51,52]. The leaching
 299 concentrations of Cr at the 90°C condition were higher than the GB 8978 limit (1.5
 300 mg/L), but lower than the European directive limit (10 mg/L). The leaching
 301 concentrations of Cr at 25°C condition were below the limits referenced in the above

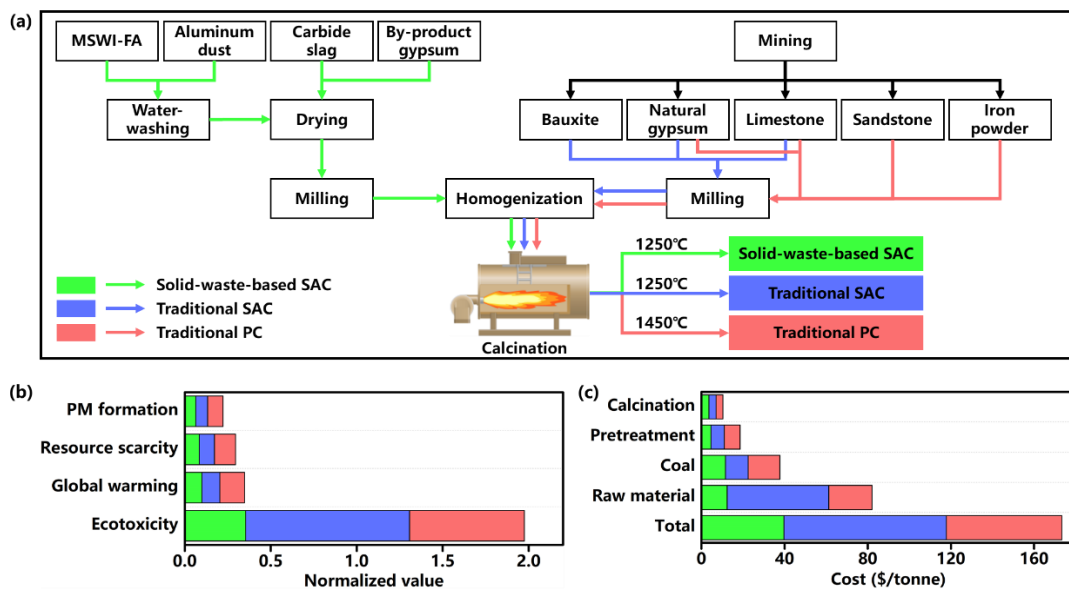
302 standards. The EPMA element mapping images of the minerals in the Cs-doped samples
303 (Figure S6) showed that most elements were enriched in the interstices or tightly
304 combined with elemental Ca or Al. In summary, these results indicated that the solid-
305 waste-based SAC had an efficient and synergetic immobilization effect on most heavy
306 metals. Critically, this effect was observed at both high and low temperature conditions.

307 Cr, Zn, and Mn were the most abundant heavy metals in the solid wastes derived
308 SAC clinkers, which accounted for 1348.3 mg/kg, 826.7 mg/kg, 871.3 mg/kg in M1
309 clinker and 181.0 mg/kg, 925.6 mg/kg, 405.5 mg/kg in M2 clinker, respectively. As
310 shown in Figure S6, most elements of Mn and Zn were enriched in the interstices of
311 Ca- or Al- containing minerals both at 25°C and 90°C conditions, despite of the
312 chemical change of ettringite. These elements were probably incorporated in the SAC
313 clinker during the calcination process and hardly participated in hydration
314 reaction[53,54], which explained the low leaching of Zn and Mn during the leaching
315 tests. Most elements of Cr were enriched in the interstices of the Ca-containing minerals
316 at 25°C condition, but they became evenly distributed in the sample leached at 90°C
317 condition. The decomposition of ettringite at 90°C condition might have led to the
318 release and migration of Cr owing to its high mobility[55]. These results indicated that,
319 the phase transition of SAC clinkers had different effects on the immobilization and
320 migration of various heavy metals.

321 **3.5 Life cycle assessment and economic analysis**

322 Figure 7a contains a simplified flow chart of the production of solid-waste-based
323 SAC, traditional SAC and PC. Compared with traditional SAC and PC, there are clear

324 advantages of producing SAC *via* synergetic-complementary use of industrial solid
 325 wastes, including: (1) reduced raw material costs and energy consumption, (2)
 326 extensive consumption of industrial solid wastes, and (3) products with high-
 327 performance. These features are all associated with potential environmental and
 328 economic benefits that can be analyzed *via* life cycle assessment and economic analysis.



329

330 **Figure 7.** Environmental and economic analyses of the production of solid-waste-based
 331 SAC, traditional SAC and PC: (a) Simplified flow chart; (b) Major environmental
 332 impacts in LCA results; (c) Production costs

333 The three different cements are then modeled assuming that 1 tonne of clinker was
 334 produced for each cement type. The normalization results (Figure 7b) revealed that the
 335 four major environmental impacts were ecotoxicity, global warming, resource scarcity,
 336 and PM formation. The normalized value of ecotoxicity to produce the solid-waste-
 337 based SAC was 62.7% and 46.9% lower than that for traditional SAC and PC,
 338 respectively, indicating that the technical route in this work is much more
 339 environmentally-friendly.

340 Greenhouse gas emission is also an important factor to consider. As shown in
341 Figure 7b, the global warming value resulting from the solid-waste-based SAC
342 production was only 69.5% of that for traditional PC. Moreover, the resource scarcity
343 value for the solid-waste-based SAC was 3.4% and 30.6% lower than that for traditional
344 SAC and PC, respectively. Moreover, the mineral resource scarcity value was only 0.07%
345 and 0.2% that for traditional SAC and PC, respectively. Collectively, these results
346 demonstrated the lower total energy and mineral resource consumption in the
347 production of solid-waste-based SAC. In addition, the PM formation from the solid-
348 waste-based SAC was also lower than that for traditional SAC and PC. Detailed LCA
349 results are provided in the Supporting Information (Figure S7).

350 Production costs were also analyzed; results are shown in Figure 7c. The total
351 production costs for the solid-waste-based SAC, traditional SAC, and PC were \$39.7,
352 \$78.0, and \$55.6 per tonne, respectively. We also observed that the low cost of the raw
353 materials was a key factor in the total cost reduction for the solid-waste-based SAC
354 relative to traditional SAC and PC. Moreover, the cost of water-washing and heating
355 pretreatment process for MSWI-FA and aluminum dust was only \$2.3, which did not
356 cause a significant increase in total cost. Detailed economic analysis results are
357 provided in Table S7.

358 These results indicated that SAC production using industrial solid wastes achieved
359 environmentally friendly nature and large-scale resource utilization of solid wastes.
360 Moreover, their production was associated with significant reductions in the overall
361 environmental burden compared to the traditional approaches[28]. The production cost

362 of solid-waste-based SAC was much lower than that of either traditional SAC or PC,
363 especially in terms of raw material costs. Moreover, solid-waste-based SAC promotes
364 the comprehensive utilization of industrial solid wastes through a circular development
365 approach[21].

366 **3.6 Environmental implications**

367 The safe use of cleaner nuclear energy significantly reduces the consumption of
368 fossil fuels, thereby improving energy efficiency and ensuring a sustainable supply of
369 energy for human society. However, the safe disposal of nuclear waste is an
370 environmental and energy-related problem that the world must face and solve. One such
371 solution to this problem is to use industrial solid wastes to synthesize green materials;
372 these materials are then used for nuclear waste solidification. This approach allows for
373 the safe and cost-effective disposal of nuclear wastes, while also solving the problem
374 of high-value industrial solid waste utilization. Ultimately, it is a sound strategy with
375 great industrial prospects and potential applications. The solid-waste-based SAC matrix
376 prepared in this study exhibited excellent solidification effects on Cs and heavy metals
377 from the perspective of long-term solidification. The technical route has the potential
378 to promote the substantial development of nuclear power and the large-scale utilization
379 of solid wastes; moreover, this approach also promotes the construction of a new
380 industrial chain. Collectively, this work provides a promising pathway to realize the
381 solidification of nuclear wastes and synergetic treatment of industrial solid wastes.

382 **4 Conclusions**

383 The solid waste-derived sulfoaluminate matrix exhibited very effective

384 encapsulation performance for cesium, as well as for the heavy metals introduced from
385 industrial solid wastes. Especially, the cumulative leaching fraction values of cesium at
386 90 °C condition were two orders of magnitude lower than those of 25 °C condition,
387 indicating the better encapsulation performance of the solid waste-derived
388 sulfoaluminate matrix at high temperature.

389 The solidification mechanism of cesium in the studied matrix was found to be a
390 physical encapsulation. The increase of temperature could accelerate the hydration of
391 the remained ye'elimite in the matrices and promote the formation of ettringite, which
392 might contribute to the much lower leaching of cesium at the early stage of the 90 °C
393 condition than that at the 25 °C condition. Despite the decomposition of ettringite at
394 90 °C condition after long-term leaching test, the phase change of ettringite did not
395 influence the effective encapsulation of cesium.

396 The production of solid waste-derived sulfoaluminate matrix could achieve
397 environmentally friendly nature and large-scale resource utilization of industrial solid
398 wastes. This approach of treating nuclear wastes with solid wastes allows for the safe
399 and cost-effective disposal of nuclear wastes, while also help to promote the high-value
400 utilization of industrial solid wastes.

401 **Supporting information**

402 XRD patterns of raw materials (**Figure S1**); XRD patterns of M1 and M2 clinkers
403 (**Figure S2**); XPS spectra of 3% Cs-doped samples hydrated for different durations up
404 to 3d (**Figure S3**); SEM/EDS results of the Cs-doped samples after 90d leaching test
405 (**Figure S4**); pH values of leachates at different time (**Figure S5**); EPMA element

406 mapping images of the minerals in M2 samples after leaching tests (**Figure S6**); LCA
407 results for production of solid-waste-based SAC, traditional SAC and PC (**Figure S7**);
408 Chemical compositions of solid waste raw materials (**Table S1**); Concentrations of 8
409 heavy metals in raw materials and prepared SAC (**Table S2**); Proportions of the solid
410 waste samples in raw meals (**Table S3**); Compressive strengths and setting times of M1
411 and M2 pastes (**Table S4**); k values for controlling leaching mechanism (**Table S5**);
412 Concentrations of heavy metals in different leachate (mg/L) (**Table S6**); Economic
413 comparison of the production of solid-waste-based SAC, traditional SAC and PC
414 (**Table S7**).

415 **Author information**

416 **Corresponding author**

417 Wenlong Wang*

418 **Address:** No.17923 Jingshi Road, Shandong University, Jinan City 250014, China

419 **Tel.:** +86-531- 88399372

420 **E-mail:** wwenlong@sdu.edu.cn

421 **Notes**

422 The authors declare no competing financial interest.

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