

# Applications of MBDoE techniques to a cloud-based platform for automated chemical manufacturing in flow reactor systems

Emmanuel Agunloye<sup>a</sup>, Panagiotis Petsagkourakis<sup>a</sup>, Muhammad Yusuf<sup>b</sup>, Ricardo Labes<sup>b</sup>, Thomas Chamberlain<sup>b</sup>, Frans L. Muller<sup>b</sup>, Richard A. Bourne<sup>b</sup>, and Federico Galvanin<sup>a\*</sup>

<sup>a</sup>Department of Chemical Engineering, University College London, Torrington Place, London, WC1E 7JE, United Kingdom

<sup>b</sup>School of Chemical and Process Engineering, University of Leeds, Leeds, LS2 9JT, United Kingdom

\*corresponding author: f.galvanin@ucl.ac.uk

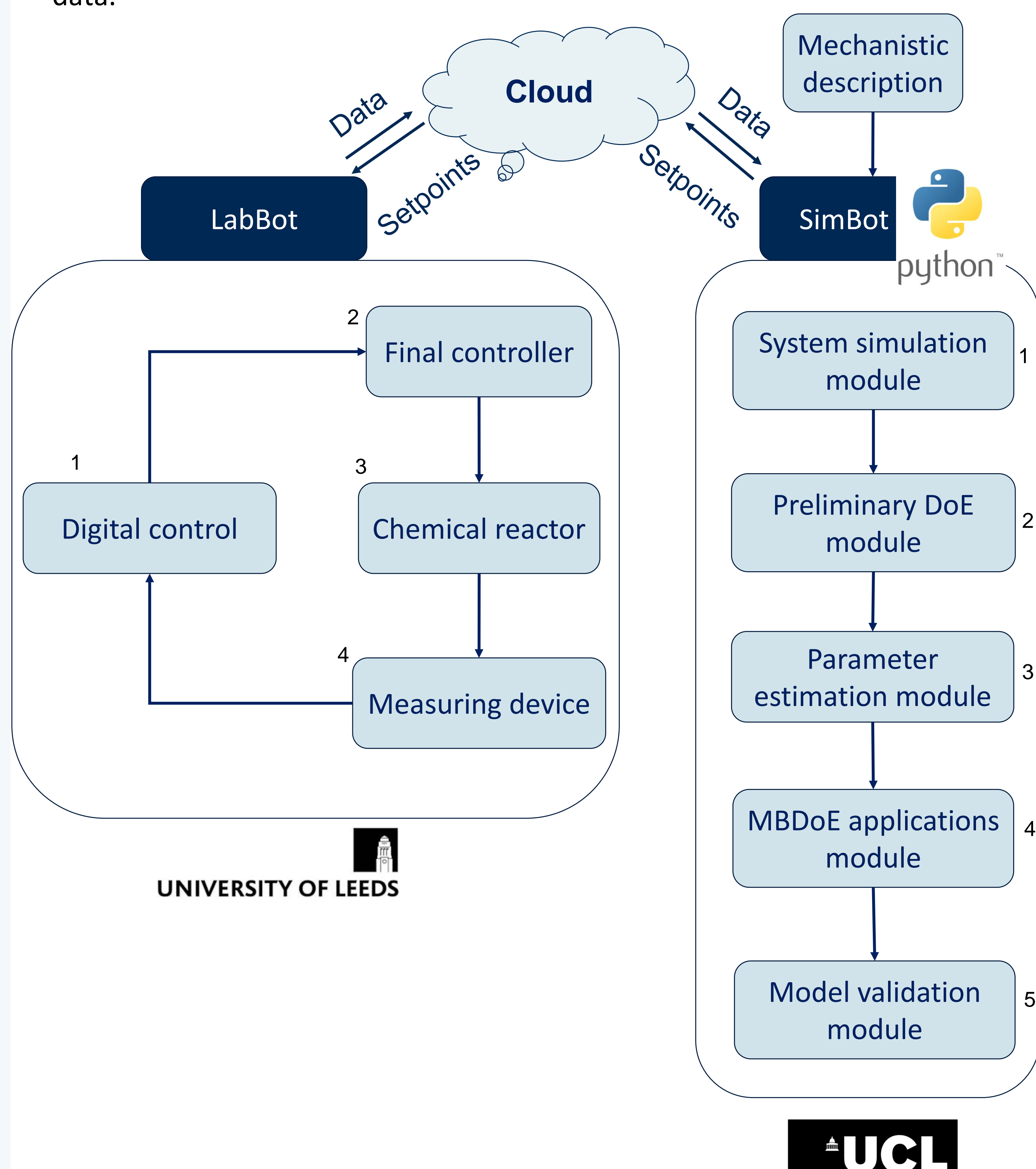


## ? Introduction and Motivation

- Industry 4.0 has birthed a new era for the chemical manufacturing sector, transforming reactor design and automating process control [1].
- Towards autonomous chemistry development, on-demand manufacturing, and real-time optimization, we have developed a **cloud-based platform driven by model-based design of experiment (MBDoE)**, an optimal experimental design algorithm, to coordinate remotely the LabBot, a smart flow reactor, situated at the University of Leeds.
- The platform has modelled and enriched two pharmaceutically-relevant case studies: nucleophilic aromatic substitution and homogeneous amide formation.

## Methodology

- Figure 2.1 illustrates the communication within the cloud-based platform.
- The MBDoE algorithm is Module 4 within the Python-coded SimBot software that computes and sends experimental designs while the LabBot – the experimental setup with 4 compartments – executes and sends experimental data.



### Simbot modelling and optimisation structure

- Differential and algebraic equations (DAEs):

$$\mathbf{f}(\dot{\mathbf{x}}(\tau), \mathbf{x}(\tau), \mathbf{u}(\tau), \boldsymbol{\theta}, \tau) = \mathbf{0} \quad (2.1)$$

$$\hat{\mathbf{y}}(t) = \mathbf{g}(\mathbf{x}(\tau)) \quad (2.2)$$

$$\mathbf{x}(0) = \mathbf{x}_0 \quad (2.3)$$

$$\boldsymbol{\phi} = [\mathbf{u}^T, \tau, \mathbf{x}_0^T]^T \quad (2.4)$$

$$\mathbf{x}(\tau) \in \mathcal{X} \quad (2.5)$$

Eq.(2.1) describes the reactor measured and initialised by Eqs. (2.2) and (2.3) within the design space described by Eqs (2.4) and 2.5) combined.

- Modelling objectives:

- Parameter estimation (Module 3 for maximizing the likelihood function) [2]:

$$\psi_{PE} = \min_{\boldsymbol{\phi} \in \Phi} (\mathbf{y} - \hat{\mathbf{y}})^T \mathbf{V}^{-1} (\mathbf{y} - \hat{\mathbf{y}}) \quad (2.6)$$

- Precision MBDoE (for maximizing a scalar measure of the Fisher information matrix (FIM), in this work the determinant) [3]:

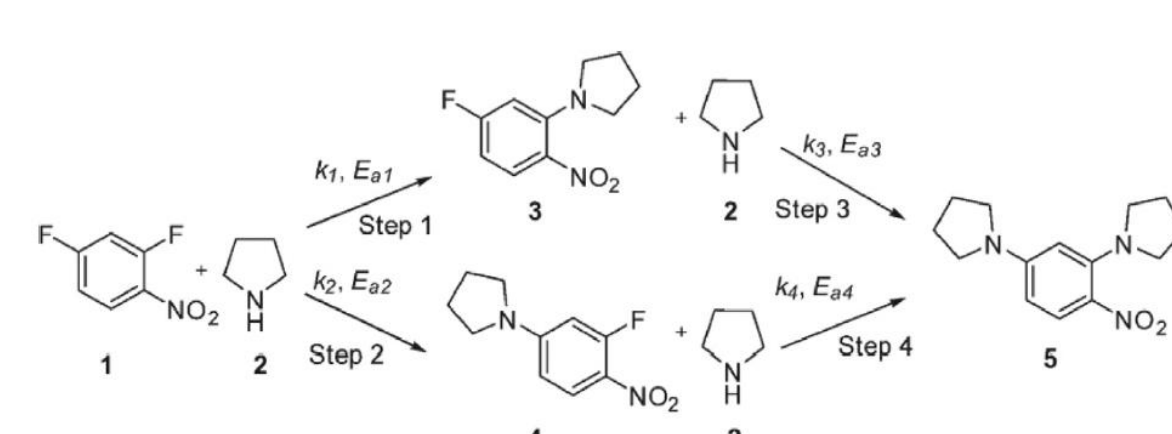
$$\psi_{MBDoE} = \max_{\boldsymbol{\phi} \in \Phi} \sum_{r=1}^r \sum_{s=1}^s \sigma_1^{rs} \mathbf{Q}_r^T \mathbf{Q}_s \quad (2.7)$$

$\mathbf{x}(t)$ : state variable,  $\hat{\mathbf{y}}(t)$ : measurements,  $\mathbf{u}(t)$ : control variables,  $\boldsymbol{\theta}$ : parameters,  $t$ : time;  $\mathbf{y}$ : model expectation,  $\mathbf{V}$ : response covariance matrix with elements  $\sigma_i^{rs}$ ,  $\mathbf{Q}$ : parameter model sensitivities  $\partial \mathbf{f} / \partial \boldsymbol{\theta}$ ,  $\psi$ : objective function

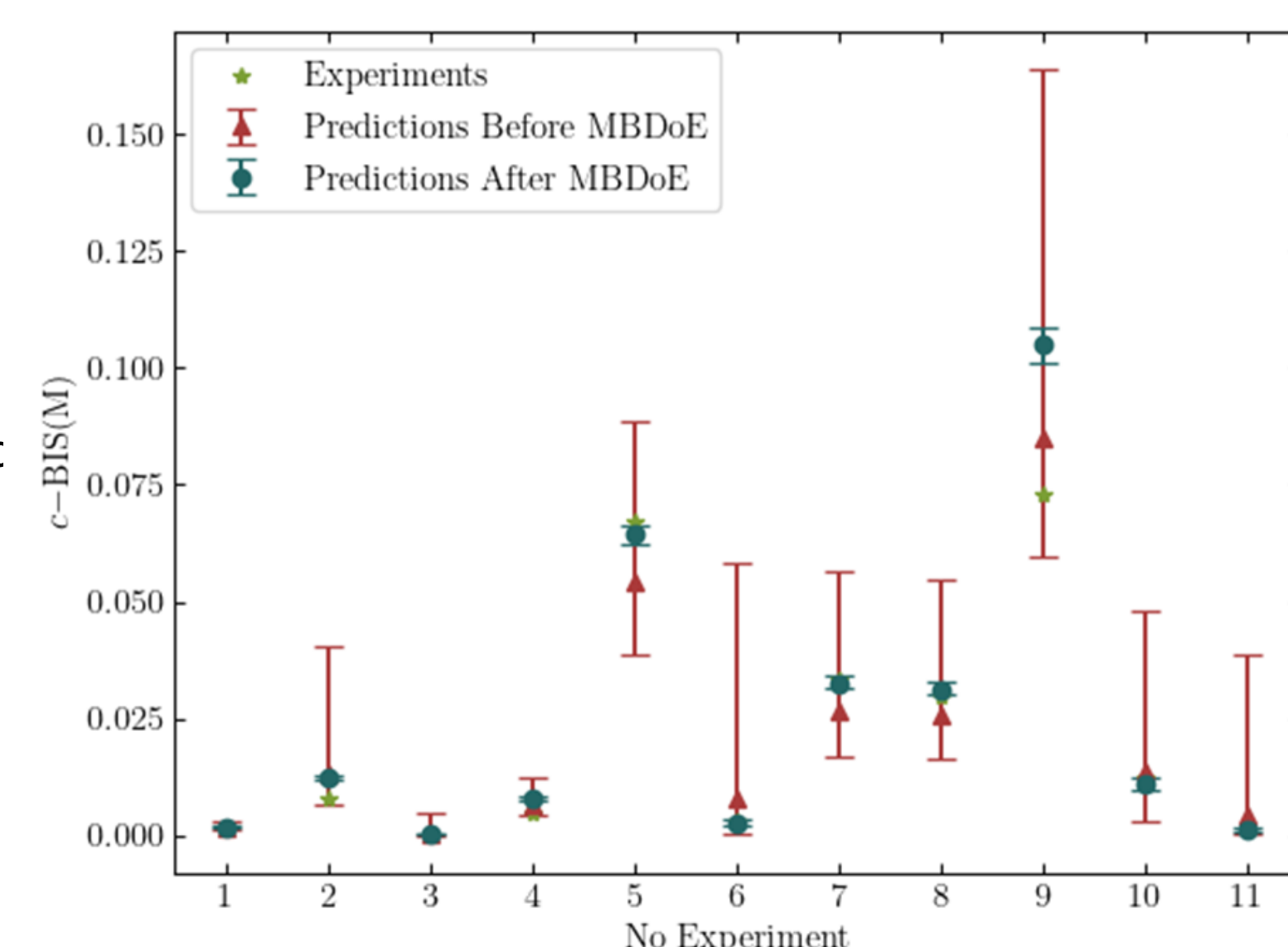
## Results

### Case Study 1: Nucleophilic aromatic substitution

- The reaction mechanism in this case study shown below has been reported [4].
- The resulting kinetic model (Module 1) is reported in Eqs. (3.1) – (3.5).
- On applying MBDoE (Module 4), the parameter statistics and model accuracy improved.



Scheme of reaction steps: nucleophilic aromatic substitution of 2,4-difluoronitrobenzene



### Kinetic modelling

$$\frac{dc_1}{d\tau} = -r_1 + r_2 \quad (3.1)$$

$$\frac{dc_2}{d\tau} = -r_1 - r_2 - r_3 - r_4 \quad (3.2)$$

$$\frac{dc_3}{d\tau} = r_1 - r_3 \quad (3.3)$$

$$\frac{dc_4}{d\tau} = r_2 - r_4 \quad (3.4)$$

$$\frac{dc_5}{d\tau} = r_3 + r_4 \quad (3.5)$$

$c_i$   $i^{th}$  species concentration;  $r_j$  is the reaction rate (mol/s.L) of the  $j^{th}$  reaction

Figure 3.1: Significant reduction in model prediction uncertainty and improved model accuracy impacted by MBDoE

Table 3.1: Parameter values and statistics calculated before and after MBDoE

	$k_1$	$E_{a1}$	$k_2$	$E_{a2}$	$k_4$	$E_{a4}$
Parameter values	1.21	34.53	0.21	27.84	0.057	42.49
$t$ -before ( $t_{rpf}$ (99%) = 2.68)	9.61	39.04	16.91	5.89	0.45	0.23
$t$ -MBDoE ( $t_{rpf}$ (99%) = 2.40)	55.04	260.76	136.65	73.08	27.60	15.60

### Case Study 2: Homogeneous amide formation

- Two mechanisms can be inferred from literature: forward-step and reversible-step.
- $\chi^2$  lack-of-fit test accepted the reversible model (with 4 parameters) as the best model for the amide formation (Module 3).
- The MBDoE module subsequently selected the most Fisher informative experiment that improved the reversible model precision and predictions as shown below by the validation results (Module 5).

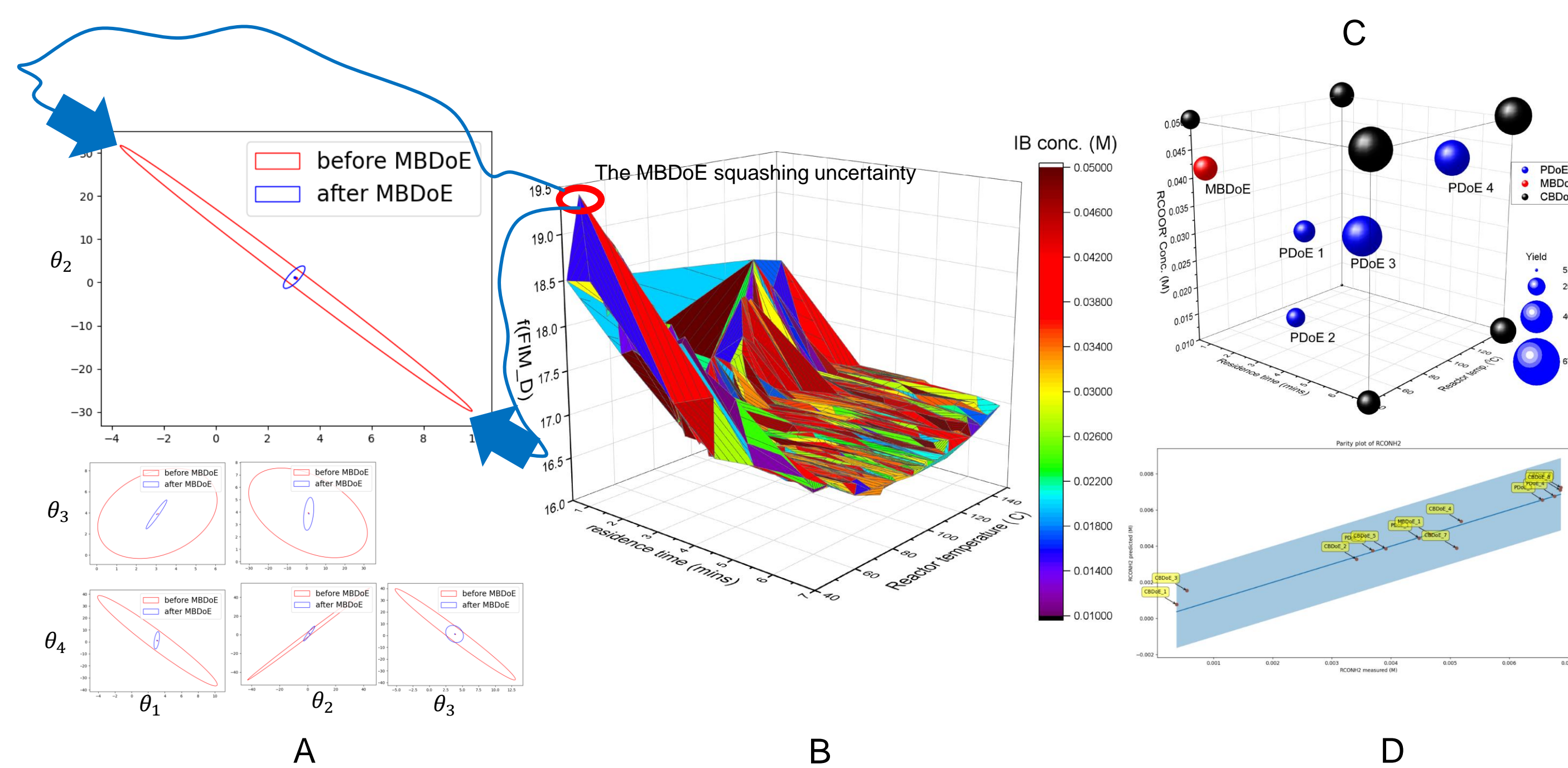


Figure 3.2: A: Parameter precision, B: Fisher information map, C: Design space, and D: Model validation parity plot. PDoe: Preliminary DoE; CBDoe: Control-bound DoE.

## Conclusions

- We have developed a novel cloud-based platform driven by MBDoE to remotely coordinate experimentation in a smart flow reactor.
- The platform in few experiments autonomously identified structure and parameters in kinetic models suitable for pharmaceutical applications.

## Acknowledgement

This project received funding from the EPSRC with the grant name: cognitive chemical manufacturing and reference: EP/R032807/1. The support is gratefully acknowledged.

### References:

- Galvanin, F., Hartman, R. L., Kulkarni, A. A., Nieves-Remacha, M. J., 2022. React. Chem. Eng., 7, 792, DOI: 10.1039/d2re90011d
- Bard, Y. Academic Press 1974.
- Franceschini, G., Macchietto, S., 2008. Chem Eng Sci, 63, 19, doi.org/10.1016/j.ces.2007.11.034
- Hone, C. A., Holmes, N., Akien, G. R., Bourne, R. A. and Muller, F. L., 2017. React. Chem. Eng., 2, 103, DOI: 10.1039/c6re00109b
- Petsagkourakis, P., and Galvanin, F., 2021. Comp. and Chem. Eng., 151 107339, DOI: 10.1016/j.compchemeng.2021.107339

### Personal Information



Emmanuel Agunloye



Panagiotis Petsagkourakis



Federico Galvanin



Sargent Centre  
for Process Systems  
Engineering

