

Synergy of Ag and AgBr in a Pressurized Flow Reactor for Selective Photocatalytic Oxidative Coupling of Methane

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ABSTRACT: Oxidation of methane into valuable chemicals, such as C_{2+} molecules, has been long sought after but the dilemma between high yield and high selectivity of desired products remains. Herein, methane is upgraded through the photocatalytic oxidative coupling of methane (OCM) over a ternary Ag-AgBr/TiO₂ catalyst in a pressurized flow reactor. The ethane yield of 35.4 μ mol/h with a high C_{2+} selectivity of 79% has been obtained under 6 bar pressure. These are much better than most of the previous benchmark performance in photocatalytic OCM processes. These results are attributed to the synergy between Ag and AgBr, where Ag serves as an electron acceptor and promotes the charge transfer



and AgBr forms a heterostructure with TiO_2 not only to facilitate charge separation but also to avoid the overoxidation process. This work thus demonstrates an efficient strategy for photocatalytic methane conversion by both the rational design of the catalyst for the high selectivity and reactor engineering for the high conversion.

KEYWORDS: oxidative coupling of methane, pressurized flow reactor, synergy of Ag and AgBr, ethane, photocatalysis

INTRODUCTION

Large reserves of natural gas and shale gas, especially those in remote areas, have raised incentives for the on-site and large-scale conversion of methane (CH₄) to high-value chemicals, which also avoids adverse environmental impact due to the nearly 30-time more potent greenhouse gas effect of methane than CO₂.^{1,2} However, the low polarisability and high C–H bond energy (439 kJ/mol) of CH₄ make its economic conversion extremely challenging.³ Methane conversion, including the nonoxidative coupling of methane, oxidative coupling of methane (OCM), and partial oxidation of methane, has been developed in thermocatalysis for the production of value-added products, such as C₂₊ hydrocarbons and alcohols.^{4–6} However, most of the processes require strong oxidants (H₂O₂ or H₂SO₄) and/or harsh reaction conditions (e.g., high temperature and pressure).^{4,7,8}

Photocatalysis uses the energy of photons instead of heat to drive thermodynamically nonspontaneous reactions, such as water splitting, carbon dioxide reduction, etc. Since photons are the main energy source, photocatalytic reactions can be conducted under very mild conditions. Methane oxidation by oxygen gas to C₁ oxygenates (e.g., CH₃OH, CH₃OOH, and HCHO) in the presence of water has been well-studied using oxide-based photocatalysts. The selectivity of products can be manipulated via the modification of different co-catalysts.⁹ For instance, a high primary products (CH₃OOH and CH₃OH) yield of 25.4 μ mol/h and a selectivity of 95% were achieved over TiO₂ modified by Au-CoO_x dual co-catalyst.¹⁰ Up to now, photocatalytic methane conversion has already been achieved over TiO₂, ZnO, WO₃, etc.^{11–17} However the upgrade of methane into C₂ products is still one of the most challenging pathways as it is difficult to minimize overoxidation while maintaining a high conversion rate.^{18–21} Recently, CH₄ was successfully converted into C_2H_6 at a selectivity of 90% in a photochemical looping process by an Ag-HPW/TiO₂ photocatalyst.²² However, the ethane yield (2.3 μ mol/h) was very moderate, and a subsequent catalyst recovery process was required to regenerate the active silver species on TiO₂. More importantly, when O₂ was introduced into the reaction atmosphere, only overoxidation products (CO_x) were obtained.²³

Apart from the selection of photocatalysts, the reaction system is equally important for an efficient photochemical process. Most of the reported reactors used in photocatalytic methane conversion were batch reactors.²⁴ However, the products in a batch reactor easily undergo overoxidation in the presence of oxidants because all products from methane conversion are more reactive than methane itself. Thus, the use of flow reactors in photocatalytic methane conversion is crucial to manipulate the mass transfer, thus minimizing the drawback of batch reactors and improving the selectivity of the less stable valuable chemicals. Our group reported the first photocatalytic OCM in a flow reaction system, an improved ethane (C_2H_6) yield of 6.8 μ mol/h was achieved, but it was still quite moderate.¹⁹ Very recently, Au-ZnO/TiO₂ was also reported for photocatalytic OCM in a flow reactor under atmospheric pressure.²⁵ A high C_2H_6 yield of 100 μ mol/h was obtained

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Figure 1. Photocatalytic oxidative coupling of methane: (a) products yield and C_2H_6 selectivity over TiO₂, Ag/TiO₂, and Ag–AgBr/TiO₂; (b) products yield over TiO₂ modified by different amounts of AgBr (based on wt % of metallic Ag); (c) products yield and C_2H_6 selectivity over Ag–AgBr/TiO₂ under different pressures; (d) influence of CH₄ to air ratios on the yield under 6 bar over Ag–AgBr/TiO₂; and (e) long-term C_2H_6 production rate and selectivity under 6 bar pressure over Ag–AgBr/TiO₂. Reaction conditions: flow rates of CH₄, Air, and Ar are 40, 1, and 360 mL/min, respectively, 6 bar (except c), 40 °C, 365 nm LED, and 100 mg photocatalysts. The error bar was obtained by carrying out three tests under identical reaction conditions.

without external heating, although the temperature of the catalyst reached 413 K due to Xe lamp irradiation. These results indicate it is still challenging to achieve a high yield of C_2 products at low temperatures. Moreover, the reaction pressure, as a crucial factor in gas phase reactions, has not been investigated in flow systems for photocatalytic methane conversion. Considering the high pressure of natural gas in both production sites and transportation pipelines, it is economical to convert methane in pressurized reactors.

Herein, we report the selective photocatalytic OCM in a pressurized flow reactor over an Ag–AgBr/TiO₂ catalyst. The ethane production rate of 35.4 μ mol/h was achieved, together with an excellent C₂₊ selectivity of 79% operated at a low temperature of 40 °C. The utilization of a pressurized flow reactor likely enhanced the mass transfer of both reactants and products. Ag serves as an electron sink, while AgBr forms a heterostructure with TiO₂, which improves charge separation and migration, and more importantly avoids overoxidation. Overall, the results suggest that both the photocatalyst and the reaction system play important roles in photocatalytic methane conversion.

RESULTS AND DISCUSSION

Ag and AgBr were loaded on anatase TiO_2 by a two-step precipitation-photodeposition method as detailed in the Materials Synthesis (Supporting Information) and denoted Ag-AgBr/TiO₂. The same amount of Ag was also loaded on

 TiO_2 by photodeposition as a reference and denoted Ag/TiO₂. The photocatalysts were tested in a pressurized flow reaction system (Scheme S1). The control experiment shows that the photocatalyst, CH₄, and light irradiation are all indispensable to converting methane at low temperatures (Figure S1). Then, CH₄ conversion was evaluated on TiO₂. Bare TiO₂ produces CO_2 with a selectivity of 91% at a rate of 45.1 μ mol/h (Figures 1a and S2). With 2 wt % Ag deposited on TiO_{2} , the C_2H_6 production rate increases from 2.1 μ mol/h to 36.7 μ mol/h. Additionally, C_3H_8 is also produced at a rate of 1.9 μ mol/h. Ag loading can facilitate the formation of C₂₊ products. However, severe overoxidation is also observed as the CO₂ production rate surges to 99.5 μ mol/h, corresponding to a selectivity of 52%. When Ag and AgBr were co-loaded on TiO_{2} , the C_2H_6 and C₃H₈ production rates slightly reduce to 35.4 and 1.1 μ mol/h, respectively, while CO₂ production is substantially suppressed. A high C₂₊ selectivity of 79% has been achieved over Ag-AgBr/TiO₂ in contrast to 8% over TiO₂ and 44% over Ag/TiO₂.

Following this, a series of Ag–AgBr/TiO₂ photocatalysts with various Ag loading amounts were synthesized to optimize the photocatalytic performance under the reaction pressure of 6 bar (Figures 1b and S2). The selectivity shifts toward C_2H_6 (70%) even with a small AgBr amount of 0.5 wt %. Increasing the amount of AgBr to 2 wt % has little effect on the yield of C_2H_6 but effectively decreases the production of CO₂. Although further increasing the AgBr amount can improve C_{2+} selectivity to as high as 90%, a decrease in the yield of all products is observed. The results indicate that AgBr plays an important role in controlling overoxidation during methane conversion. TiO₂ decorated with 2 wt % AgBr was then chosen for further study to improve both the yield and selectivity of C_2H_6 . The effect of reaction pressure on the photocatalytic OCM performance was investigated (Figures 1c and S3). The yield of C_2H_6 increases from 18.2 to 35.4 μ mol/h as the reaction pressure elevates from 1 to 6 bar. An apparent quantum efficiency under 6 bar based on methane conversion was calculated to be 3% at 365 nm. The photocatalytic performance at 7 bar stops increasing, which is possibly caused by the limited photo-induced carriers generated by the photocatalyst. The enhanced performance under elevated pressures is mainly due to the enhanced mass transfer, which increases the adsorption of CH4 on the surface of photocatalysts. On the other hand, the selectivity of CO2 gradually increases from 9 to 16% as pressure increases. The partial pressures of both CH₄ and O₂ in the reaction atmosphere increase as the total pressure increases. Considering the activation of O_2 is much easier than that of CH_{4} ,²⁰ O_2 reduction is improved more significantly than CH4 under higher pressures, resulting in the formation of excessive O₂⁻ radicals, which contributes to overoxidation. Thus, the selectivity toward C₂₊ products decreases under higher pressures. The effect of CH₄ to air ratio on the photocatalytic performance was next investigated at a total flow rate of 400 mL/min (Figures 1d and S4). When changing the ratio of CH_4 /air ratio from 40:1 to 1:1, the C_2H_6 production rate first increases from 35.4 to 58.1 μ mol/h at the CH₄/air of 2:1, and finally drops to 52.1 μ mol/h when the CH₄/O₂ ratio reaches 1:1. The yield of CO_2 is greatly accelerated with the increase of O₂ proportion.

The optimized Ag-AgBr/TiO₂ photocatalyst was further tested under 6 bar pressure to examine its long-term durability (Figures 1e and S5). The yield of all products increases in the first 3 h and becomes stable afterward. It suggests that there is an in situ activation process. It is well known that AgBr is lightsensitive and can decompose into Ag and Br₂ upon exposure to irradiation.²⁷ The enhancement of plasmonic Ag signal in the UV-vis diffuse reflectance spectrum (DRS) of Ag-AgBr/TiO₂ after reaction for 3 h suggests that the amount of Ag in the photocatalyst increases, indicating AgBr underwent partial decomposition at this stage (Figure S6). The reduced Br 3d Xray photoelectron spectroscopy (XPS) signal after the photocatalytic OCM reaction for 3 h and the similar intensity of the XPS peaks after running for 3 and 12 h suggest that AgBr is not fully decomposed even after the long-term irradiation (Figure S7). The main Ag species in AgBr/TiO₂ before the photocatalytic reaction are positively charged silver (Figure S8i, e.g., AgBr), with only a small amount of metallic Ag. After the reaction for 3 h, the portion of metallic Ag increases while Ag⁺ decreases. This results from the fact that AgBr is partially decomposed into metallic Ag at the first 3 h of irradiation. The ratio of Ag to AgBr is calculated to be 1.34:1 based on the integrated area of the corresponding band after the catalyst is run for 3 h. Further prolonging the reaction time to 12 h results in a slight increase of Ag with an Ag to AgBr ratio of 1.57:1. The XPS results further confirm that AgBr almost remains and the chemical state of Ag in Ag-AgBr/TiO₂ is hardly changed during the photocatalytic OCM reaction from 3 to 12 h. X-ray diffraction (XRD) also confirms the partial decomposition of AgBr after 3 h and the amount of AgBr is relatively stable in the subsequent 9 h (Figure S9), consistent with the reported.²⁸ Photoluminescence (PL) spectra display improved separation of charge carriers in Ag–AgBr/TiO₂ after 3 h of reaction (Figure S10). A similar luminescent property was observed in the photocatalyst after 3 and 12 h of methane conversion. Combined with the long-term photocatalytic performance, the above results reveal that AgBr is rather stable after the initial in situ activation process. Table S1 shows the performance of different reported photocatalysts for photocatalytic C₂H₆ production from methane, and it is clear that Ag–AgBr/TiO₂ shows a high C₂H₆ production rates of 34.5 μ mol/h in photocatalytic methane oxidation by air with a C₂₊ selectivity of 79% in a low reaction temperature of 40 °C.

XRD patterns of the photocatalysts display the main component of anatase (Figure 2a). Ag was not detected in



Figure 2. (a) XRD spectra of TiO₂, Ag-TiO₂, and Ag-AgBr/TiO₂; (b) Ag 3d high-resolution XPS spectra of Ag/TiO₂ and Ag-AgBr/TiO₂; (c) UV-vis DRS spectra; (d) PL spectra of TiO₂, Ag-TiO₂, and Ag-AgBr/TiO₂; and (e, f) TEM images of Ag-AgBr/TiO₂.

either Ag/TiO₂ or Ag–AgBr/TiO₂, possibly due to its small particle size and/or high dispersity.^{29,30} Peaks at 14.1 and 20.0 degrees are assigned to (200) and (220) crystal planes of AgBr (PDF#06-0438), confirming the existence of AgBr on Ag–AgBr/TiO₂. Ag 3d high-resolution XPS spectra of Ag–AgBr/TiO₂ prove the presence of both metallic and positively charged Ag (Figure 2b). The peaks at 363.9 and 370.3 eV are attributed to the Ag 3d_{5/2} and Ag 3d_{3/2} of positively charged Ag ions, while those at 363.3 and 369.3 eV are ascribed to the Ag 3d_{5/2} of metallic Ag.^{31,32} The molar ratio of Ag/AgBr on the surface of TiO₂ was calculated to be 1.57:1 based on the integrated area of the related Ag 3d_{3/2} peak (or only 1.2 wt % of metallic Ag on the photocatalyst). Combined

with the Br 3d spectrum (Figure S7), XPS analysis reveals the co-existence of Ag and AgBr on Ag-AgBr/TiO₂. The band at 460 nm of UV-vis DRS spectra of Ag/TiO₂ and Ag-AgBr/ TiO₂ is attributed to the plasmonic effect of metallic Ag (Figure 2c).³³ Absorption of AgBr is not observed in the DRS spectrum of Ag-AgBr/TiO2, possibly due to the low loading amount. Then, the absorption spectrum of pure AgBr was measured (Figure S11), representing a visible absorption when the amount of AgBr is large enough. PL spectroscopy was used to investigate the charge separation and recombination process of the photocatalysts. TiO₂ shows the highest PL emission, implying an intense recombination process. Ag loading causes a reduction in the PL intensity, and co-modification of TiO_2 with Ag and AgBr results in the lowest PL signals. Considering the similar absorption of three catalysts in the UV region, the most efficient charge separation is achieved over Ag-AgBr/ TiO₂. To further study the effect of AgBr on charge separation and migration, the open circuit photovoltage decay spectra of three catalysts were measured (Figure S12a-c). The average lifetimes of the charges in TiO₂, Ag/TiO₂, and Ag-AgBr/TiO₂ are determined to be 6.4, 12.1, and 52.9 s, respectively (Figure S12d). The eightfold increased lifetime indicates that the formation of a heterojunction between TiO₂ and AgBr significantly prolongs the charge lifetime. The longest lifetime of charge carriers is resulted from the efficient separation of electrons and holes and could improve photon efficiency in photocatalysis.

Transmission electron microscopy (TEM) images show that TiO_2 consists of nanoparticles of 20–30 nm (Figure S13a). High-resolution TEM (HRTEM) displays the (101) plane of anatase TiO_2 with an interplanar spacing of 0.346 nm (Figure S13b). Metallic Ag nanoparticles can be confirmed by the line scan of Ag/TiO₂ (Figure S14). Nanoparticles of AgBr with diameters of 100-200 nm were observed in Ag-AgBr/TiO₂ (Figure 2e). Small Ag nanoparticles of 5 nm are also found to co-exist with AgBr on TiO_2 in Ag-AgBr/TiO₂ (Figure 2f). The HRTEM (Figure S15) further verifies the existence of AgBr in Ag–AgBr/TiO₂, the interplanar distances of 0.206 and 0.290 nm are ascribed to the (220) and (200) crystal facets of AgBr, which is in accordance with the XRD analysis. In the scanning transmission electron microscopy energy-dispersive spectrometry (EDS) mapping images (Figure S16), the Ti element from TiO₂ is detected in the selected area. Ag and Br elements are consistent with large particles of AgBr. The quality of Br mapping is slightly lower than Ag. This is mainly because that AgBr is partially decomposed under the long-term irradiation of the electron beam. Overall, Ti, O, Ag, and Br are detected in Ag-AgBr/TiO₂ as observed from the EDS sum spectrum (Figure S16e).

The reduction of oxygen gas by electrons and oxidation of methane by holes are two crucial steps during photocatalytic OCM. The oxygen reduction capability of the three photocatalysts was tested via linear sweep voltammetry (LSV) in a three-electrode cell at a potential ranging from 0.4 to -1.2 V vs Ag/AgCl (Figure S17). In the absence of air, little current is generated until the applied voltage reaches -1.0 V due to hydrogen evolution. On the contrary, a negative current is generated at the onset potential of -0.4 V in the presence of air, which is attributed to the oxygen reduction reaction. Therefore, the signal obtained in the presence of air is contributed by both oxygen reduction and hydrogen evolution. To reflect the actual oxygen reduction ability of the catalysts, the difference between the LSV spectra obtained with and

without air is replotted (Figure 3a). The results show that Ag nanoparticles play a major role in oxygen reduction, as both



Figure 3. (a) Oxygen reduction LSV spectra of TiO_2 , Ag $-TiO_2$, and Ag $-AgBr/TiO_2$ (solid line) and LSV spectrum of Ag $-AgBr/TiO_2$ tested in the absence of air (dotted line), (b) EPR O_2^- spectra of TiO_2 , Ag $-TiO_2$, and Ag $-AgBr/TiO_2$; (c) XPS valance band spectra of TiO_2 and AgBr; and (d) transient photocurrent plots of TiO_2 , Ag $-TiO_2$, and Ag $-AgBr/TiO_2$ with a bias potential of 0.25 V vs Ag/AgCl.

Ag/TiO₂ and Ag-AgBr/TiO₂ show improved current density compared with TiO_2 when the bias is more negative than -0.6V. Ag/TiO₂ exhibits the highest current density due to the highest metallic Ag amount of 2 wt %. This is consistent with the previous report that metallic Ag could promote oxygen adsorption on TiO2.34 Ag acts as an electron sink and can promote charge separation by accepting electrons from the conduction band (CB) of TiO2. Therefore, more photogenerated holes in the Ag-containing photocatalysts are available to activate methane molecules. As a result, the improved conversion rate of CH₄ is achieved after the loading of Ag. O₂ can then be reduced by electrons on the surface of Ag to produce superoxide radicals (O_2^{-}) . To confirm this, the formation of O₂⁻ radicals was monitored by electron paramagnetic resonance (EPR) using 5,5-dimethyl-1-pyrroline N-oxide as the spin-trapping reagent (Figure 3b). No EPR signal is generated in dark conditions (Figure S18), suggesting that the formation of O_2^- resulted from the combination of O_2 and photoinduced electrons. Ag/TiO₂ and Ag-AgBr/TiO₂ generate a higher level of O_2^- radicals than TiO₂, which remains in the same order as the LSV oxygen reduction results when the bias is more negative than -0.6 V. The highest amount of O₂⁻ radicals are generated over Ag/TiO₂. O₂⁻ radicals clean the surface of the photocatalyst by combining with H^+ to produce H_2O . Ag serves as an electron acceptor and catalyzes O₂ reduction, which contributes to charge separation and photon efficiency, thus resulting in improved methane conversion. However, a high level of O_2^{-} radicals also encourage the complete mineralization of organic compounds or overoxidation to produce CO2.35 Thus, a large amount of CO_2 (99.5 μ mol/h) was detected in the photocatalytic OCM over Ag/TiO2. Ag-AgBr/TiO2 shows intermediate oxygen reduction properties among three photocatalysts, which is beneficial for reducing the selectivity of CO₂ while maintaining a relatively high CH₄ conversion.

XPS valence band (VB) spectra were measured, which shows that the relative VB potentials of AgBr and TiO₂ are 1.9 and 3 eV, respectively (Figure 3c). Taking into account of the reported VB potential of anatase TiO₂ is 2.9 V vs NHE,³⁶ the VB potential of AgBr should be 1.8 V vs NHE. Thus, photoholes can potentially transfer from the VB of TiO₂ to AgBr in Ag–AgBr/TiO₂ upon light irradiation, resulting in a reduced oxidation potential. Thus, the overoxidation is suppressed and a high selectivity toward C₂H₆ is reasonable after the introduction of AgBr. To further evaluate the oxidation capability of the photocatalysts, the transient photocurrents of TiO₂, Ag/TiO₂, and Ag-AgBr/TiO₂ were measured in a 0.5 M NaSO₄ aqueous solution containing 10 vol % methanol. A bias potential of 0.25 V was applied in the test (Figures S19 and 3d). TiO₂ shows a high photocurrent density of 40 μ A/cm², suggesting a fast electron transfer from the working electrode to the counter electrode and intensive methanol oxidation. When adding Ag to TiO₂, the photocurrent is slightly reduced somehow. It is probably because the electrons are trapped by metallic Ag, which then reduces some intermediates from methanol oxidation. When methanol is removed from the electrolyte, Ag/TiO₂ displays the highest photocurrent for water oxidation among the three catalysts (Figure S20). The lowest photocurrent is generated by Ag-AgBr/TiO₂. After photogenerated holes transfer from the VB of TiO₂ to AgBr, the oxidation potential is reduced, leading to a slow methanol oxidation process. This also mitigates the overoxidation of the produced C₂₊ to CO₂. A much higher selectivity toward C₂₊ products has thus been achieved over $Ag-AgBr/TiO_2$ compared with TiO₂ and Ag/TiO₂.

To provide insights into the reaction mechanism and reaction pathway, in situ diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) was performed on Ag/TiO₂ and Ag–AgBr/TiO₂ (Figure 4). The infrared (IR) signal at



Figure 4. In situ DRIFTS spectra of Ag/TiO_2 and $Ag-AgBr/TiO_2$ in dark and under light irradiation in reaction atmosphere ($CH_4/air = 40:1$).

2875/2880 cm⁻¹ under light irradiation is ascribed to the stretching vibration of C–H in CH₃· radicals adsorbed on the oxide surface. This band is stronger in the spectrum of Ag/TiO₂ than Ag–AgBr/TiO₂, which shows the same trend as the methane conversion performance over the two photocatalysts. The peaks at 2358 and 2331/2326 cm⁻¹ are typical signals originating from CO₂ generated due to overoxidation in the photocatalytic OCM process. The CO₂ peaks over Ag/TiO₂ are much stronger than Ag–AgBr/TiO₂ and the intensity keeps increasing with prolonged irradiation time. In contrast, Ag–AgBr/TiO₂ generates a moderate amount of CO₂ under identical reaction conditions. This result is in accordance with the product selectivity of Ag/TiO₂ and Ag–AgBr/TiO₂. An additional band at 1552/1558 cm⁻¹ is ascribed to the HCOO·

species, which is an important intermediate and finally results in the formation of CO_2 in the methane oxidation process. The strong band at 1558 cm⁻¹ indicates that the consumption of HCOO- is slower than its formation over Ag-AgBr/TiO₂, suggesting a mild overoxidation process. However, the HCOOspecies on Ag/TiO₂ can be facilely converted to CO_2 , which is deduced from the low IR band intensity of HCOO- species at 1552 cm⁻¹. The IR spectra over the two photocatalysts show different features when the irradiation time reaches 70 to 120 min, as displayed in Figure S21. An increased absorption across the whole spectrum is observed over Ag/TiO2 with the increased irradiation time. Due to the fast oxidation of methane by Ag/TiO_2 , the amount of O_2 gas decreases rapidly in the reaction chamber. Therefore, photogenerated electrons could not be consumed due to the low level of oxygen and electrons start to accumulate on the CB of TiO₂, consistent with the report that the photogenerated electrons display an IR absorption from 4000 to 1500 cm^{-1.37} Nevertheless, this phenomenon is not observed in the IR spectra of Ag-AgBr/ TiO₂. The spectra almost overlap at the irradiation time from 70 to 120 min. This indicates that a slow oxygen consumption process and a mild methane oxidation process are achieved over Ag-AgBr/TiO₂, compared with Ag/TiO₂. This result is in accordance with the LSV oxygen reduction and EPR O₂trapping analysis.

To provide evidence on the universal synergy effect of Ag and AgBr on semiconductors for photocatalytic methane conversion, an Ag-AgBr/ZnO photocatalyst was synthesized by the same method, and its performance is compared with the pristine ZnO. ZnO, with a similar band structure as TiO₂, should display similar behavior as TiO₂ in photocatalytic methane conversion. The results are shown in Figure S22. When pure ZnO is applied as the photocatalyst, CH₃OH and CO_2 are generated at production rates of 6.1 and 7.5 μ mol/h, respectively. It suggests that the methyl radicals formed from the reaction between methane and photoholes are mostly overoxidised into CO2. The production of CH3OH could probably be due to the unique surface features of ZnO, which might facilitate CH₃OH desorption. Overall, coupling of methyl radicals is not encouraged on ZnO surfaces as C₂H₆ is not detected in the products. After modification with Ag-AgBr, C_2H_6 with a high production rate of 22.8 μ mol/h is detected. A trace amount of C_3H_8 (0.4 μ mol/h) is also produced, which is the product of further C₂H₆ activation. CH₃OH is not detectable in the products. Most importantly, the production rate of CO₂ is reduced from 7.5 to 4.2 μ mol/h after the modification of ZnO with AgBr. Combined with the methane oxidation performance of the Ag-AgBr/TiO₂ photocatalyst, direct evidence of the function of AgBr in facilitating C₂H₆ production and reducing overoxidation is obtained.

The band gaps of TiO₂ and AgBr were determined to be 3.2 and 2.5 eV, respectively, from the Kubelka–Munk conversion plots (Figure S23), consistent with the reported.³⁶ Combined with the XPS VB analysis (Figure 3c), the CB potentials of AgBr and TiO₂ are determined to be -0.7 and -0.3 V vs NHE, respectively. In Ag–AgBr/TiO₂, AgBr forms a type II heterojunction with TiO₂ (Scheme 1). Upon light irradiation, photoelectrons tend to transport from the CB of AgBr to TiO₂, and further to Ag, while photoholes transfer from the VB of TiO₂ to AgBr. Considering the potentials required for O₂⁻ formation from O₂ reduction and \cdot CH₃ production from CH₄ oxidation are -0.16 and 1.75 V vs NHE, ^{1,22,38} such a structure Scheme 1. Photocatalytic Reaction Pathway of Ag–AgBr/ $\rm TiO_2$

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is not only beneficial for charge separation but also capable of driving the photocatalytic OCM reaction, therefore resulting in improved photon utilization efficiency and a high methane conversion. Although the enhanced charge separation is also achieved in Ag/TiO_2 , the highly oxidative holes at the VB of TiO_2 and the large number of $\mathrm{O_2}^-$ radicals formed on the metallic Ag cause severe overoxidation and significantly deteriorate the selectivity toward C_{2+} products (Scheme S2) in the Supporting Information). After the introduction of AgBr, photogenerated holes at the VB of TiO₂ transfer to that of AgBr and then oxidize methane into methyl radicals and protons. A mild methane oxidation process is thus achieved by the less oxidative holes at the VB of AgBr. Next, the formed methyl radicals are prone to couple into C₂H₆ and are less likely to undergo overoxidation due to the relatively weak oxidation potential of photoholes in the VB of AgBr. In parallel, O_2^- radicals react with protons to generate water. Some C₂H₆ molecules are activated again by photoholes to form $\cdot C_2H_5$ radicals, which couple with $\cdot CH_3$ radicals and form C_3H_8 .

CONCLUSIONS

In summary, an efficient and selective photocatalytic OCM process has been realized with a ternary Ag-AgBr/TiO₂ photocatalyst in a pressurized flow reactor. The production rate of C_2H_6 achieved is as high as 35.4 μ mol/h, with a C_{2+} selectivity of 74-90% depending on the pressures used, together with an apparent quantum efficiency of 3% at 365 nm. These results suggest that both the reaction system and the photocatalyst play important roles in the performance of photocatalytic methane conversion as detailed by a series of characterizations. The utilization of a pressurized flow reactor enhances the mass transfer of reactants and products, contributing to the high methane conversion and selectivity toward C₂₊ products. A series of electrochemical tests and EPR results proved that Ag nanoparticles serve as an electron acceptor to improve charge separation, while the reactive holes from TiO₂ transfer to AgBr and become less oxidative to avoid overoxidation. Therefore, both the high yield and high selectivity of C2+ products have been obtained. The findings demonstrate a potential to realize the efficient and selective conversion of methane to C_{2+} by the synergy of Ag and AgBr driven by photocatalysis.

ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/acscatal.2c06093.

Experimental procedures and characterization data (PDF)

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Author Contributions

The manuscript was written through the contributions of all authors. All authors have approved the final version of the manuscript.

Notes

The authors declare no competing financial interest.

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REFERENCES

(1) Li, X.; Wang, C.; Tang, J. Methane Transformation by Photocatalysis. *Nat. Rev. Mater.* **2022**, *7*, 617–632.

(2) Lashof, D. A.; Ahuja, D. R. Relative Global Warming Potentials of Greenhouse Gas Emissions. *Nature* **1990**, *344*, 529–531.

(3) Meng, X.; Cui, X.; Rajan, N. P.; Yu, L.; Deng, D.; Bao, X. Direct Methane Conversion under Mild Condition by Thermo-, Electro-, or Photocatalysis. *Chem* **2019**, *5*, 2296–2325.

(4) Guo, X.; Fang, G.; Li, G.; Ma, H.; Fan, H.; Yu, L.; Ma, C.; Wu, X.; Deng, D.; Wei, M.; Tan, D.; Si, R.; Zhang, S.; Li, J.; Sun, L.; Tang, Z.; Pan, X.; Bao, X. Direct, Nonoxidative Conversion of Methane to Ethylene, Aromatics, and Hydrogen. *Science* **2014**, *344*, 616–619.

(5) Hutchings, G. J.; Scurrell, M. S.; Woodhouse, J. R. Oxidative Coupling of Methane Using Oxide Catalysts. *Chem. Soc. Rev.* **1989**, *18*, 251–283.

(6) Woertink, J. S.; Smeets, P. J.; Groothaert, M. H.; Vance, M. A.; Sels, B. F.; Schoonheydt, R. A.; Solomon, E. I. A [Cu2O]2+ Core in Cu-ZSM-5, the Active Site in the Oxidation of Methane to Methanol. *Proc. Natl. Acad. Sci. U. S. A.* **2009**, *106*, 18908–18913. (7) Periana, R. A.; Taube, D. J.; Evitt, E. R.; Löffler, D. G.; Wentrcek, P. R.; Voss, G.; Masuda, T. A Mercury-Catalyzed, High-Yield System for the Oxidation of Methane to Methanol. *Science* **1993**, *259*, 340–343.

(8) Ab Rahim, M. H.; Forde, M. M.; Jenkins, R. L.; Hammond, C.; He, Q.; Dimitratos, N.; Lopez-Sanchez, J. A.; Carley, A. F.; Taylor, S. H.; Willock, D. J.; Murphy, D. M.; Kiely, C. J.; Hutchings, G. J. Oxidation of Methane to Methanol with Hydrogen Peroxide Using Supported Gold-Palladium Alloy Nanoparticles. *Angew. Chem., Int. Ed.* **2013**, *52*, 1280–1284.

(9) Song, H.; Huang, H.; Meng, X.; Wang, Q.; Hu, H.; Wang, S.; Zhang, H.; Jewasuwan, W.; Fukata, N.; Feng, N.; Ye, J. Atomically Dispersed Nickel Anchored on a Nitrogen-Doped Carbon/TiO₂ Composite for Efficient and Selective Photocatalytic CH₄ Oxidation to Oxygenates. *Angew. Chem., Int. Ed.* **2023**, *62*, No. e2022150.

(10) Song, H.; Meng, X.; Wang, S.; Zhou, W.; Song, S.; Kako, T.; Ye, J. Selective Photo-Oxidation of Methane to Methanol with Oxygen over Dual-Cocatalyst-Modified Titanium Dioxide. *ACS Catal.* **2020**, *10*, 14318–14326.

(11) Song, H.; Meng, X.; Wang, Z.; Liu, H.; Ye, J. Solar-Energy-Mediated Methane Conversion. *Joule* **2019**, *3*, 1606–1636.

(12) Hu, D.; Ordomsky, V. V.; Khodakov, A. Y. Major Routes in the Photocatalytic Methane Conversion into Chemicals and Fuels under Mild Conditions. *Appl. Catal.*. B **2021**, 286, No. 119913.

(13) Xie, J.; Jin, R.; Li, A.; Bi, Y.; Ruan, Q.; Deng, Y.; Zhang, Y.; Yao, S.; Sankar, G.; Ma, D.; Tang, J. Highly Selective Oxidation of Methane to Methanol at Ambient Conditions by Titanium Dioxide-Supported Iron Species. *Nat. Catal.* **2018**, *1*, 889–896.

(14) Chen, X.; Li, Y.; Pan, X.; Cortie, D.; Huang, X.; Yi, Z. Photocatalytic Oxidation of Methane over Silver Decorated Zinc Oxide Nanocatalysts. *Nat. Commun.* **2016**, *7*, 12273.

(15) Villa, K.; Murcia-López, S.; Andreu, T.; Morante, J. R. Mesoporous WO3 Photocatalyst for the Partial Oxidation of Methane to Methanol Using Electron Scavengers. *Appl. Catal., B* **2015**, *163*, 150–155.

(16) Lang, J.; Ma, Y.; Wu, X.; Jiang, Y.; Hu, Y. H. Highly Efficient Light-Driven Methane Coupling under Ambient Conditions Based on an Integrated Design of a Photocatalytic System. *Green Chem.* **2020**, 22, 4669–4675.

(17) Jiang, W.; Low, J.; Mao, K.; Duan, D.; Chen, S.; Liu, W.; Pao, C.-W.; Ma, J.; Sang, S.; Shu, C.; Zhan, X.; Qi, Z.; Zhang, H.; Liu, Z.; Wu, X.; Long, R.; Song, L.; Xiong, Y. Pd-Modified ZnO–Au Enabling Alkoxy Intermediates Formation and Dehydrogenation for Photocatalytic Conversion of Methane to Ethylene. *J. Am. Chem. Soc.* **2021**, 143, 269–278.

(18) Zhou, Y.; Zhang, L.; Wang, W. Direct Functionalization of Methane into Ethanol over Copper Modified Polymeric Carbon Nitride via Photocatalysis. *Nat. Commun.* **2019**, *10*, 506.

(19) Li, X.; Xie, J.; Rao, H.; Wang, C.; Tang, J. Platinum- and CuO_x -Decorated TiO₂ Photocatalyst for Oxidative Coupling of Methane to C₂ Hydrocarbons in a Flow Reactor. *Angew. Chem., Int. Ed.* **2020**, *59*, 19702–19707.

(20) Meng, L.; Chen, Z.; Ma, Z.; He, S.; Hou, Y.; Li, H. H.; Yuan, R.; Huang, X. H.; Wang, X.; Wang, X.; Long, J. Gold Plasmon-Induced Photocatalytic Dehydrogenative Coupling of Methane to Ethane on Polar Oxide Surfaces. *Energy Environ. Sci.* **2018**, *11*, 294–298.

(21) Wu, S.; Tan, X.; Lei, J.; Chen, H.; Wang, L.; Zhang, J. Ga-Doped and Pt-Loaded Porous TiO_2 -SiO₂ for Photocatalytic Nonoxidative Coupling of Methane. *J. Am. Chem. Soc.* **2019**, *141*, 6592–6600.

(22) Yu, X.; Zholobenko, V. L.; Moldovan, S.; Hu, D.; Wu, D.; Ordomsky, V. V.; Khodakov, A. Y. Stoichiometric Methane Conversion to Ethane Using Photochemical Looping at Ambient Temperature. *Nat. Energy* **2020**, *5*, 511–519.

(23) Yu, X.; De Waele, V.; Löfberg, A.; Ordomsky, V.; Khodakov, A. Y. Selective Photocatalytic Conversion of Methane into Carbon Monoxide over Zinc-Heteropolyacid-Titania Nanocomposites. *Nat. Commun.* **2019**, *10*, 700. (24) Song, H.; Meng, X.; Wang, S.; Zhou, W.; Wang, X.; Kako, T.; Ye, J. Direct and Selective Photocatalytic Oxidation of CH_4 to Oxygenates with O_2 on Cocatalysts/ZnO at Room Temperature in Water. J. Am. Chem. Soc. **2019**, 141, 20507–20515.

(25) Song, S.; Song, H.; Li, L.; Wang, S.; Chu, W.; Peng, K.; Meng, X.; Wang, Q.; Deng, B.; Liu, Q.; Wang, Z.; Weng, Y.; Hu, H.; Lin, H.; Kako, T.; Ye, J. A selective Au-ZnO/TiO₂ hybrid photocatalyst for oxidative coupling of methane to ethane with dioxygen. *Nat. Catal.* **2021**, *4*, 1032–1042.

(26) Miao, T. J.; Wang, C.; Xiong, L.; Li, X.; Xie, J.; Tang, J. In Situ Investigation of Charge Performance in Anatase TiO₂ Powder for Methane Conversion by Vis-NIR Spectroscopy. *ACS Catal.* **2021**, *11*, 8226–8238.

(27) Yu, H.; Xu, L.; Wang, P.; Wang, X.; Yu, J. Enhanced Photoinduced Stability and Photocatalytic Activity of AgBr Photocatalyst by Surface Modification of Fe(III) Cocatalyst. *Appl. Catal., B* **2014**, *144*, 75–82.

(28) Shiozawa, T.; Kobayashi, T. High Resolution Electron Microscopic Study of Photolytic Silver in Silver Bromide. *Phys. Status Solidi* **1987**, *104*, 649–659.

(29) Zhang, H.; Wang, G.; Chen, D.; Lv, X.; Li, J. Tuning Photoelectrochemical Performances of Ag-TiO₂ Nanocomposites via Reduction/Oxidation of Ag. *Chem. Mater.* **2008**, *20*, 6543–6549.

(30) Zheng, Z.; Huang, B.; Qin, X.; Zhang, X.; Dai, Y.; Whangbo, M. H. Facile in Situ Synthesis of Visible-Light Plasmonic Photocatalysts $M@TiO_2$ (M = Au, Pt, Ag) and Evaluation of Their Photocatalytic Oxidation of Benzene to Phenol. *J. Mater. Chem.* **2011**, *21*, 9079–9087.

(31) Katsumata, H.; Hayashi, T.; Taniguchi, M.; Suzuki, T.; Kaneco, S. Highly Efficient Visible-Light Driven AgBr/Ag₃PO₄ Hybrid Photocatalysts with Enhanced Photocatalytic Activity. *Mater. Sci. Semicond. Process.* **2014**, *25*, 68–75.

(32) Wang, P.; Huang, B.; Qin, X.; Zhang, X.; Dai, Y.; Whangbo, M. H. Ag/AgBr/WO₃-H₂O: Visible-Light Photocatalyst for Bacteria Destruction. *Inorg. Chem.* **2009**, *48*, 10697–10702.

(33) Li, S.; Shen, Y.; Xie, A.; Yu, X.; Qiu, L.; Zhang, L.; Zhang, Q. Green Synthesis of Silver Nanoparticles Using Capsicum Annuum L. *Extract. Green Chem.* **2007**, *9*, 852–885.

(34) Seyedmonir, S. R.; Strohmayer, D. E.; Geoffroy, G. L.; Vannice, M. A.; Young, H. W.; Linowski, J. W. Characterization of Supported Silver Catalysts. I. Adsorption of O_2 , H_2 , N_2O , and the H_2 -Titration of Adsorbed Oxygen on Well-Dispersed Ag on Ti O_2 . J. Catal. **1984**, 87, 424–436.

(35) Wang, Z.; Ma, W.; Chen, C.; Ji, H.; Zhao, J. Probing Paramagnetic Species in Titania-Based Heterogeneous Photocatalysis by Electron Spin Resonance (ESR) Spectroscopy-A Mini Review. *Chem. Eng. J.* **2011**, *170*, 353–362.

(36) Maheu, C.; Cardenas, L.; Puzenat, E.; Afanasiev, P.; Geantet, C. UPS and UV Spectroscopies Combined to Position the Energy Levels of TiO₂ Anatase and Rutile Nanopowders. *Phys. Chem. Chem. Phys.* **2018**, *20*, 25629–25637.

(37) Fu, C.; Li, F.; Yang, J.; Xie, J.; Zhang, Y.; Sun, X.; Zheng, X.; Liu, Y.; Zhu, J.; Tang, J.; Gong, X. Q.; Huang, W. Spontaneous Bulk-Surface Charge Separation of TiO_{2} -{001} Nanocrystals Leads to High Activity in Photocatalytic Methane Combustion. *ACS Catal.* **2022**, *12*, 6457–6463.

(38) Wood, P. M. The Potential Diagram for Oxygen at PH 7. *Biochem. J.* **1988**, 253, 287–289.