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Chemical Vapor Deposition of Hollow Graphitic Spheres for Improved Electrochemical Durability

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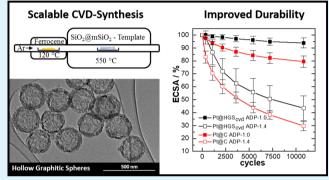
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ABSTRACT: The wet-chemical synthesis of hollow graphitic spheres, a highly defined model catalyst support for electrocatalytic processes, is laborious and not scalable, which hampers potential applications. Here, we present insights into the chemical vapor deposition (CVD) of ferrocene as a simple, scalable method to synthesize hollow graphitic spheres (HGS $_{\rm cvd}$). During the CVD process, iron and carbon are embedded in the pores of a mesoporous silica template. In a subsequent annealing step, iron facilitates the synthesis of highly ordered graphite structures. We found that the applied temperature treatment allows for controlling of the degree of graphitization and the textural properties of HGS $_{\rm cvd}$. Further, we demonstrate that platinum loaded on HGS $_{\rm cvd}$ is significantly more stable during electrochemical degradation



protocols than catalysts based on commercial high surface area carbons. The established CVD process allows the scalable synthesis of highly defined HGS and therefore removes one obstacle for a broader application.

KEYWORDS: mesoporous carbon, liquid-free synthesis, chemical vapor deposition, stability enhancement, PEMFC

■ INTRODUCTION

Increasing energy demand and depletion of fossil resources lead to an intensified search for alternative and sustainable energy systems. One promising technology for mobile applications is the polymer electrolyte membrane fuel cell.^{1,2} The electrical energy is generated from the electrochemical reaction between hydrogen and oxygen, with water as the only byproduct. Typical state-of-the-art catalysts for the oxygen reduction reaction (ORR) on the cathode side of the fuel cell consist of homogeneously dispersed platinum and platinumalloy nanoparticles supported on high surface area carbon materials.³ A major restriction in successful commercialization and implementation of the technology is the availability of platinum and its high overpotential as well as the lack of longterm stability.⁴⁻⁶ The underlying degradation mechanisms were identified by means of identical location transmission electron microscopy (TEM).^{7,8} In general, the degradation can be divided into five mechanisms, including Pt dissolution, Ostwald ripening, carbon corrosion, particle detachment, and agglomeration. 9-11 Hollow graphitic spheres (HGS) were reported to significantly suppress degradation mechanisms such as particle detachment and agglomeration, thanks to a confinement of the nanoparticles in the mesopores of the HGS. 10-12 Templating methods are typically utilized for the synthesis of mesoporous materials with tailored textural properties, subdivided into hard and soft templating methods. ^{13,14} The wet-chemical synthesis of HGS requires a multi-step hard templating process: initially, core—shell mesoporous silica spheres (SiO₂@mSiO₂) are synthesized, as reported by Büchel et al. ¹⁵ These hard templates are employed to scaffold the textural properties (i.e., shell thickness, pore size, and void diameter) of the resulting HGS replica. For this, divinylbenzene, as the carbon source, and iron, as the graphitization catalyst, are infiltrated in three subsequent impregnation steps. ^{10,12} Overall, this complex multistep procedure, partly at high dilution, makes scale-up of the synthesis process very difficult, thus hampering the technical use of fuel cell catalysts based on this process. ^{16–19}

Alternatively, replication of nanostructured templates could be achieved via chemical vapor deposition (CVD) processes. Classically, CVD is used for the production of solid thin films on flat substrates, and also mesoporous membranes were employed as templates for the synthesis of carbon nanotubes. Commonly, gaseous hydrocarbons (e.g., ethylene, methane, benzene, and acetylene) are decomposed at the host

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material.^{25–28} The simultaneous deposition of metal particles and carbon was achieved by sublimation and subsequent pyrolysis of ferrocene.²⁹ Recently, Lei et al.³⁰ extended this approach, employing mesoporous ordered silica (SBA-15) powder as the template. The strong interaction of the pyrolytic carbon clusters with the pore walls of the SBA-15 led to the formation of ordered mesoporous carbon (CMK-5) replicas. In contrast to the wet-chemical impregnation process, the incorporation of iron and carbon was obtained within a single step. The embedded iron can be utilized to catalyze the graphitization of the decomposed carbon, ^{31,32} significantly altering the textural properties of the obtained carbon replica.³⁰ Additionally, the CVD of ferrocene employing SiO₂@mSiO₂ templates was reported for the synthesis of hollow graphitic carbon spheres.^{33–36}

In the following, the influence of temperature on the graphitization degree and the consequential textural changes of the resulting hollow graphitic spheres (HGS $_{\rm cvd}$) are reported in detail. Additionally, the HGS $_{\rm cvd}$ supports were decorated with Pt nanoparticles and employed for the ORR demonstrating improved catalytic durability compared to Pt nanoparticles loaded on commercial high surface area carbon (Pt@C).

■ EXPERIMENTAL SECTION

HGS_{cvd} Synthesis. The synthesis of the hard template was reported by Büchel et al. ¹⁵ A detailed report on the wet-chemical synthesis of HGS, including the hard template, was compiled by our group. ¹⁶ Briefly, 350 mL of ethanol, 65 mL of water, and 7.6 mL of ammonium hydroxide solution (25 wt % in water) were mixed for 5 min. Then, 13.9 mL of TEOS was added under rapid stirring. After 2 h, a mixture of 9.9 mL of TEOS and 3.9 mL of OTMS was added to the white suspension. The mixture was stirred overnight. Then, the suspension was centrifuged and the solid was dried at 75 °C overnight. The dried material was calcined in air with a heating rate of 1 K/min to a final temperature of 550 °C. The dwelling time was 3 h. The obtained solid was ground using a mortar and pestle.

For the CVD of ferrocene, the procedure described by Lei et al. was adapted.³⁴ Typically, a quartz crucible containing 2 g of SiO₂@mSiO₂ template and a crucible containing 10 g of ferrocene were placed in a quartz tube. The quartz tube was transferred into a tubular furnace that was heated to $550~^{\circ}\text{C}$ for 1.5 h (5 K/min) in an argon flow of 100 mL/min, with the crucible containing the template centered in the heating zone. The quartz tube inlet was enveloped with a heating jacket that was rapidly heated to 120 °C (standard tube, NS29) or 140 °C (large setup, NS45) once the tubular furnace reaches 500 °C. The crucible containing ferrocene was centered to the heating zone of the heating jacket. After a dwelling time of 1.5 h, both heating devices were switched off and cooled to ambient temperature naturally while maintaining the Ar flow. The resulting composite material spontaneously ignites in the presence of air, presumably caused by the finely dispersed iron nanoparticles in the material. Therefore, the sample was passivated by the aid of an O2/N2 (1:99 vol %) flowing gas mixture of 100 mL/min for >1.5 h before it can be safely stored without further precautionary measure. Following the passivation, the sample was heated in 90 min to the respective annealing temperature of 1000 °C, 900 °C, 800 °C, or 700 °C for 4 h in an argon flow of 100 mL/min. The silica residues were leached by HF: 1 g of composite was submerged in 7 mL of HF (40%) for 24 h and washed with water multiple times. Following the silica leaching, leaching of iron was performed by the addition of an excess of 7 mL/ $g_{composite}$ HCl (30%) overnight. Finally, the samples were washed with water and dried at

Pt@HGS $_{cvd}$ Synthesis. The synthesis of Pt@HGS can be subdivided into three individual steps. Initially, the metal precursors are impregnated via incipient wetness impregnation. For a typical synthesis of 100 mg Pt@HGS $_{cvd}$, 80 mg of the HGS $_{cvd}$ support was impregnated with H $_2$ PtCl $_6 \times x$ H $_2$ O $_{aq}$. H $_2$ PtCl $_6 \times x$ H $_2$ O $_{aq}$ (38.8 μ L,

2.64 mol/L; ≥99.9%; Sigma-Aldrich) was dissolved in 10.9 μ L of Millipore water (18.2 MΩ cm at 25 °C). The resulting solution is equal to the total pore volume of the employed support. In order to ensure complete pore filling, the powder was sonicated for 30 min. For the second step, the powder was dried and subsequently reduced. Therefore, the sample was dried for 60 min at 120 °C (3 K/min) under an Ar flow (300 mL/min) and subsequently heated to 220 °C (3 K/min) under a H₂/Ar gas stream (60/240 mL/min) with a holding time of 90 min. The sample was cooled naturally to ambient temperature under an Ar flow (300 mL/min). Finally, the sample was annealed at 850 °C for 2.5 h (5 K/min) under an Ar atmosphere (200 mL/min).

X-ray Diffraction Analysis. A Bragg Brentano diffractometer (Θ/Θ) from STOE (Cu K α 1,2 X-ray source), equipped with a secondary graphite monochromator and a proportional gas detector, was employed for the collection of the X-ray diffraction (XRD) pattern. The opening of the divergence slit was set to 0.8° and the receiving slit was set to 0.6 mm. The width of the horizontal mask was chosen to be 8 mm. A background-free single-crystal quartz sample holder was employed for the measurements.

 N_2 **Physisorption.** The measurements were carried out with a Micromeritics 3 Flex instrument. The samples were activated under vacuum for at least 8 h at 250 °C. The measurements were performed at 77.4 K using a static volumetric method with a relative pressure tolerance of 5%. For relative pressures below $0.1p/p^0$, an incremental dose mode (15 cm³/g STP, equilibration intervals 10 s) was employed.

Transmission Electron Microscopy. The TEM micrographs were obtained using a Hitachi H-7100 microscope (100 kV, Wcathode) and a Hitachi HF-2000 microscope (200 kV) equipped with a cold field emission gun. All samples were placed on a Lacey carbon film supported by a copper grid without further treatment.

Thermogravimetric Analysis. Thermogravimetric analysis (TGA) and differential scanning calorimetry (DSC) were performed on a Netzsch STA 449F3 thermal analyzer. The measurements were performed in the temperature range of 45–1000 °C conducted with a heating rate of 20 K/min. The gas composition was set to 60/40 mL/min (air/Ar), where argon is employed as a protective purge.

Half-Cell Electrochemical Measurements. The specific activity (SA), mass activity (MA), and electrochemical surface area (ECSA) were measured via a thin-film rotating disk electrode (RDE) method. The electrochemical measurements were performed in a threeelectrode compartment Teflon cell at room temperature. The catalyst ink consisted of a catalyst powder dispersed in 5 mL of ultrapure water with an ultrasound bath; a 20 μ L droplet of the suspension was then deposited onto a carbon disk of 0.196 cm² geometric surface area, embedded in a Teflon tip. A catalyst loading of $10 \,\mu g_{Pt}/cm^2$ was employed for stability and activity investigations. For the degradation tests, a droplet of Nafion (7 µL of a 5 wt % Nafion/isopropanol solution 1/50) was deposited onto the dry catalyst film. The Teflon tip was then connected to a RDE (Radiometer Analytical, France), which served as the working electrode. Both the counter electrode, a graphite rod, and the reference electrode, a saturated Ag/AgCl electrode (Metrohm), were housed in separate compartments. In order to avoid chloride contamination, the reference electrode compartment was further separated from the main compartment by a Nafion membrane (Tschurl modification). A Gamry reference 600 potentiostat was employed and controlled in combination with the rotator and the gas system with an in-house-developed LabVIEW software. The electrolyte consisted of 0.1 M HClO₄ which was prepared with ultrapure water (18 $M\Omega$ cm, Millipore) and concentrated HClO₄ (Merck, Suprapur). The Ohmic drop was compensated by positive feedback. All potentials are given with respect to the reversible hydrogen electrode (RHE) potential, which was determined for each experiment individually. Activities were extracted from cyclic voltammograms (CVs) recorded in an O2saturated electrolyte at 1600 rpm and at 0.9 V_{RHE} with a 50 mV/s scan rate. In order to isolate the contribution related to oxygen reduction, the RDE polarization curves were corrected for capacitive processes (CV in an Ar-saturated electrolyte).

The accelerated degradation tests include two specific protocols, namely, ADP-1.0 and ADP-1.4, which consisted of 10,800 degradation cycles at 1 V/s between 0.4 and 1.0 and 0.4 and 1.4 $V_{\rm RHE}$, respectively. The degradation tests were performed without rotation and in an Ar-saturated electrolyte. In order to monitor the ECSA evolution during degradation, CO-stripping was employed to measure the ECSA after 0, 360, 1080, 2160, 3600, 5400, 7200, and 10,800 potential cycles.

The CO-stripping curves were integrated subtracting the nonfaradic contribution (CV in Ar-saturated electrolyte) and assuming a Pt surface charge density of $380~\mu\text{C/cm}^2$. The relative ECSA values were calculated by normalizing the measured ECSA with respect to the ECSA determined after 200 activation cycles. More details about this method can be found in ref 11. The electrochemical activation procedure applied consisted of 200 cleaning cycles (0.05–1.4 V_{RHE}) 0.2 V/s). In this phase, the surface carbon impurities are removed. This protocol was applied prior to the determination of SA and ECSA, as well as in the first 200 cycles of the ADP protocol. The commercial catalyst Pt@C used for comparison was purchased from Tanaka and had a platinum loading of 46 wt % and a mean platinum particle size of 3 nm. 11

RESULTS AND DISCUSSION

The employed setup for the HGS_{cvd} synthesis is depicted in Figure 1. Both ferrocene and the silica template, placed inside



Figure 1. Scheme of the setup for the CVD process.

individual quartz crucibles, are arranged in consecutive heating zones. Ferrocene is heated to 120 $^{\circ}$ C and transported by a constant Ar flow over the SiO₂@mSiO₂ silica template, located in the center of a tube furnace heated to 550 $^{\circ}$ C. Ferrocene decomposes exclusively inside the mesoporous network of the template (Figures S1 and S2) due to the high affinity of ferrocene to the silica template surface.³⁷

The composite was annealed at 700, 800, 900, and 1000 $^{\circ}$ C under an Ar atmosphere. Following the annealing step, the silica template and iron particles were removed in two distinct acid leaching steps. The final samples were referred to as HGS_{cvd}-700, -800, -900, and -1000 to indicate their annealing temperature. For all the heat-treated samples, a significant increase in thermal stability was observed compared to the leached composite material (Figure S3).

The graphitization degree after the different annealing steps was analyzed by XRD measurements (Figure 2).

The absence of reflections for the HGS $_{\rm cvd}$ -800 sample indicates the presence of disordered carbon structures. For HGS $_{\rm cvd}$ -900 and -1000, the reflections visible at 26° (002) and 42° (100) reveal the presence of additional highly ordered graphite structures. The graphitization of carbon is catalyzed by embedded iron nanoparticles from the CVD process. Without iron, temperatures well above 2000 K would be required to obtain highly ordered graphite structures. The difference in relative intensity, comparing HGS $_{\rm cvd}$ -900 and -1000, corresponds to a difference in the degree of graphitization. Further insights are obtained by TGA and DSC (Figure 3).

The TGA curves show an onset of thermal decomposition at \sim 500 °C, whereas for HGS $_{\rm cvd}$ -900 and -1000, an additional shoulder at around 700 °C is present. This is in agreement

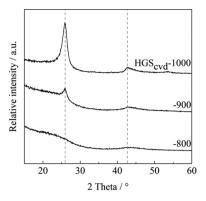


Figure 2. X-ray diffractogram for HGS_{cvd} -1000, -900, and -800. Dashed lines were added as a guideline for the eye, highlighting the reflections attributed to graphite.

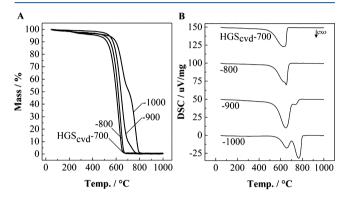


Figure 3. TGA (A) and DSC (B) of HGS_{cvd} annealed at different temperatures. The DSC data is plotted with a respective *y*-axis offset of 50 μ V/mg between traces for clarity.

with the corresponding DSC signals, in which a second peak evolved between 700 and 800 °C for the HGS_{cvd} -900 and -1000 samples. These results indicate the presence of two distinct carbon structures, with highly graphitic carbon having higher thermal stability. This again supports the finding that the higher annealing temperatures lead to the formation of highly ordered carbon structures. Based on the TGA curves, quantification of the distinct carbon structures is possible. HGS_{cvd} -900 and -1000 contain ~8 and ~48 wt % of the highly ordered graphite structure, respectively. Images of the different HGS_{cvd} samples obtained by TEM are presented in Figure 4 and in the Supporting Information (Figures S4 and S5). A comparison of the materials by Raman spectroscopy is provided in Figure S6.

The micrographs show successful replication of the $SiO_2@mSiO_2$ templates, presenting a mesoporous shell with a hollow interior. For the HGS-900 and -1000 samples, carbon tube-like structures are present, randomly oriented and enveloping the mesoporous shell. These structures show a high degree of crystallinity, with an interlayer distance of 0.33 nm determined by TEM. The quantitative difference is in agreement with previous measurements, as their fraction significantly increases with higher annealing temperature. In order to gain further understanding of the formation of the highly ordered graphite structures, the pre-leached composites (HGS $_{composite}$) are inspected (Figure 5).

The HGS_{composite}-700, -800, and -900 samples show a homogeneous distribution of iron particles (Figures 5 and S7), with average particle sizes of 10.4 ± 1.9 , 11.8 ± 1.8 , and 15.6 ± 1.8

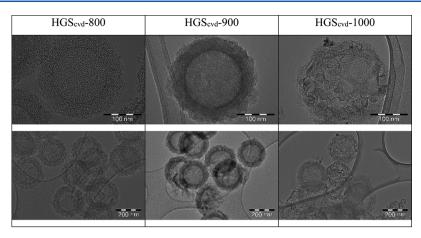


Figure 4. TEM micrographs of the HGS_{cvd}-800, -900, and -1000 samples.

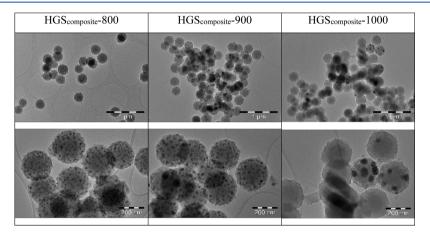


Figure 5. TEM micrographs of the pre-leached composite materials of the HGS_{ccomposite}-800, -900, and -1000 samples.

4.5 nm, respectively. The corresponding increase in particle size can be attributed to the increase in temperature, accelerating particle growth. For HGS_{composite}-1000, the iron particle size distribution is highly inhomogeneous, with particle diameters exceeding >50 nm, which are also infrequently found for the HGS_{composite}-900 sample. Additionally, the iron particles formed during annealing are unevenly distributed, and in the majority of composite structures, no iron particles can be found. These results suggest that the carbon tube-like growth process presumably causes the formation of highly ordered graphite structures, similar to the nanotube growth observed via in situ TEM studies, 38,40 ultimately leading to the formation of large iron particle agglomerates.

The influence of the formation of highly ordered graphite on mesoporosity is analyzed by N_2 physisorption measurements (Figure 6).

The different HGS_{cvd} samples and the silica template show type IV(a) isotherms, indicating that the templating process is generally successful. For the carbon replicas, a significant increase in surface area and pore volume is obtained due to the lower density of carbon and the absence of a dense core. The HGS_{cvd}-1000 sample shows a significant decrease in adsorbed quantity compared to HGS_{cvd}-900 and -800. This decrease can be attributed to the increased fraction of highly ordered graphite and the partial collapse of the templated mesoporous network. The iron-catalyzed growth is achieved if the concentration of carbon exceeds its solubility limit in the iron particles. Thus, the disordered carbon dissolves in the

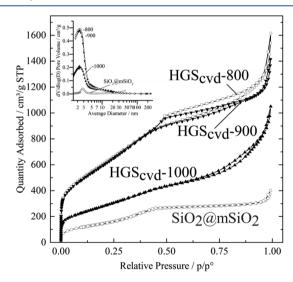


Figure 6. N_2 physisorption isotherm of the template material (SiO₂@ mSiO₂) and HGS_{cvd}-1000, -900, and -800. The inset shows the pore size distributions determined by the BJH method from the adsorption branch.

iron particles and precipitates in the form of highly ordered graphite, growing as a tube-like structure through the mesoporous replica. Consequently, a decrease in pore volume and surface area with increasing quantity of ordered graphite is observed (Table 1 and Figure 6). Nevertheless, the pore

Table 1. Summary of the N₂ Physisorption Measurements

samples	$S_{\rm BET}^{}$, m ² /g	$TPV^{a,c}$, cm^3/g	d_{pore}^{a} , nm
SiO2@mSiO2	560	0.3	2.8
HGScvd-800	2260	1.8	2.6
HGScvd-900	2285	1.9	2.5
HGScvd-1000	1060	1.3	2.6

"Determined via the BJH method from the adsorption branch (the desorption branch, which is normally recommended, might be influenced by capillary criticality). ^bSurface area determined via the BET method between relative pressures of $p/p^0 = 0.05-0.3$. For relative pressures at $0.95p/p^0$ following the Gurvich rule.

diameter remains independent of the annealing temperature/graphitization degree as illustrated by the pore size distribution. Figure 6 reveals that the heat treatment does not influence the templating process but the growth and/or final fraction of ordered carbon structures, as can be seen from the unaltered pore diameter, which is in agreement with the silica template.

To judge the reproducibility and scalability of the CVD process, a similar setup was built using a larger quartz tube (diameter NS45). To still allow sublimation of ferrocene into the furnace chamber, the temperature of the heating jacket was increased from 120 to 140 °C. Under otherwise identical reaction conditions and furnace temperatures of 1000 °C, more than 1.2 g of HGS was produced in one batch (HGS $_{\rm cvd}$ -1000-NS45). A comparison of XRD, TGA, and DSC results is provided in Figure 7. A characterization by Raman spectroscopy and an overview of TEM micrographs are given in the Supporting Information (Figures S6 and S8).

The larger relative intensity of the reflexes at 26° (002), 42° (100), and 54° (004) in the XRD pattern of HGS_{cvd} -1000-NS45 implies a higher degree of graphitization. The same can be inferred from TGA and DSC. While the sample synthesized using the smaller setup shows a distinct shoulder in the TGA curve, the same feature is not easily determined for HGS_{cvd} -1000-NS45, the weight loss curve is shifted to a slightly higher temperature as a whole. A rough estimation of the share of graphitic carbon by TGA is >50 wt %. DSC shows a similar trend, suggesting that HGS_{cvd} -1000-NS45 contains a higher share of highly graphitic carbon.

Overall, the implementation of CVD synthesis in a different, larger setup proves the reproducibility and scalability of the process. The higher graphitization of the product in the larger setup, potentially caused by a different heating profile or a higher degree of pore filling of the template, is beneficial for

the application in electrocatalysis and underlines the potential of this process for further improvement.

In order to investigate the potential benefit of the synthesized HGS $_{\rm cvd}$, it was employed as a catalyst support for the ORR. Therefore, the HGS $_{\rm cvd}$ -1000 sample was loaded with 20 wt % of Pt nanoparticles by an incipient wetness impregnation method (Figure 8). HGS $_{\rm cvd}$ -1000 was selected

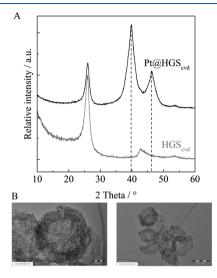


Figure 8. $HGS_{CVD}1000$ loaded with Pt nanoparticles analyzed by XRD (A) and TEM (B).

for the electrochemical tests, as it was expected to offer higher conductivity and improved corrosion stability, thanks to the presence of the highly ordered graphite structures. The Pt average particle size of 3.1 \pm 0.5 nm determined by TEM (Figure S9) is similar to the size of the mesopores in HGS_{cvd}, measured via N₂ physisorption, although pores below 10 nm are typically underestimated by 20–30% by the BJH method. The X-ray reflections at 39.67° (111) and 45.96° (200) can be clearly attributed to the impregnated Pt particles that are evenly distributed inside the mesopores of the support materials (Figure 8). The pronounced reflex broadening indicates the presence of small nanoparticles and the absence of large particles.

The electrochemical properties of $Pt@HGS_{cvd}$ -1000 were evaluated via half-cell measurements, following two distinct accelerated degradation protocols (ADPs). For the first ADP, potentials present during typical load cycles were applied, in which the samples were exposed to potentials between 0.4 and

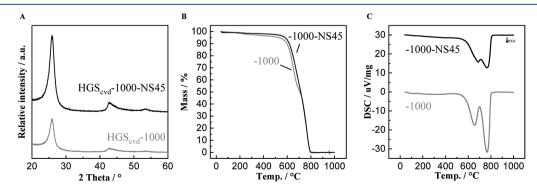


Figure 7. X-ray diffractogram (A), TGA (B), and DSC (C) of the HGS_{cvd} synthesized in two different setups. The DSC data is plotted with a respective y-axis offset of 30 μ V/mg.

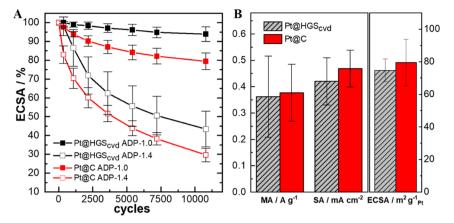


Figure 9. Comparison of the stability (A) and activity (B) of $Pt@HGS_{cvd}$ -1000 and Pt@C. The stability comparison was conducted following the ADP with an upper potential limit of 1.0 or 1.4 V_{RHE} . In (B), the MA, SA, and ECSA in the fresh state are shown.

 $1.0~V_{RHE}$ with a scan rate of 50 mV/s for 10,800 cycles (ADP-1.0). Higher potentials conceivably occurring during start-stop conditions were employed during the second accelerated degradation protocol (ADP-1.4), cycling between 0.4 and 1.4 V_{RHE} (scan rate: 50 mV/s; 10,800 cycles). The respective degradation results, SA, and MA of the catalysts are summarized in Figure 9.

In terms of activity, both Pt@HGS_{cvd}-1000 and Pt supported on commercial high surface area carbons (Pt@C) show similar results, as expected, since both catalyst systems have similar particle sizes. In terms of stability, Pt@HGS_{cvd}-1000 offer superior performance in direct comparison to Pt@C, following the employed degradation protocols. For both ADP-1.0 and ADP-1.4, the loss in ECSA is significantly more pronounced for Pt@C compared to Pt@HGS_{cvd}-1000. The increased stability of Pt@HGS is consistent with previous reports by our group and was directly attributed to the confinement of the platinum nanoparticles in the pores of the HGS. This confinement suppresses the degradation of the nanoparticles by agglomeration and/or coalescence. 10,11,17,18 The electrochemical analysis in the current work (Figure 9) verifies this improved electrochemical stability for Pt@HGS_{cvd}-1000. The particular suitability of HGS as a support material for fuel cell catalysts therefore also applies to the material produced by CVD.

CONCLUSIONS

In summary, the successful synthesis of mesoporous hollow graphitic spheres (HGS $_{\rm cvd}$) via CVD has been demonstrated. The fraction of highly ordered graphite could be adjusted by variation of the annealing temperature. Shares of graphitic carbon of >50 wt % were obtained, employing ferrocene for the CVD and subsequent annealing at 1000 °C. Thanks to the organometallic precursor, both the selective deposition of carbon and iron is achieved, where iron acts as a graphitization catalyst during the subsequent annealing step. The growth of the highly ordered graphite structures causes partial restructuring of the templated porous carbon network, reducing the surface area and the total pore volume as a result of graphitization.

The benefits of the porous network were revealed by the enhanced stability against electrochemical degradation in direct comparison to commercial catalysts, in which Pt is deposited on high surface area carbon materials.

Thanks to the CVD of ferrocene, the synthesis of HGS is possible without the need of a multi-step nanocasting process, reducing synthesis complexity and offering synthesis scalability as shown using the larger setup that yielded HGS with an even higher degree of graphitization.

ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/acsaem.1c00643.

TEM micrographs of the composite after CVD; N_2 physisorption data of the template before and after CVD; TGA of the composite before and after annealing at 800 °C for 4 h; TEM micrographs of HGS_{cvd}-700 before and after the leaching procedure; Raman spectroscopy data; TEM micrographs of HGS_{cvd}-NS45; Platinum particle size distribution of the Pt@HGScvd-1000 sample (PDF)

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Notes

The authors declare no competing financial interest.

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