

1 Influence of heating conditions and initial thickness on the effectiveness of thin intumescent 2 coatings

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7 Highlights:

- 8 Experimental methodology to gauge the thermo-physical response of intumescent coatings.
- 9 The swelling and the swelled thickness govern the effectiveness of intumescent coatings.
- 10 Heating conditions govern the swelling rate of intumescent coatings.
- 11 Applied initial thickness governs the maximum swelled thickness.
- 12 Empirical correlations for swelling rate and maximum swelled thickness.

13 Abstract:

14 The study presented herein shows an experimental methodology aimed at analysing the
15 effectiveness of intumescent coatings through a detailed characterisation of their thermo-physical
16 response for a range of heating conditions and applied initial dry film thickness (DFT). Steel plates
17 coated with a commercial solvent-based thin intumescent coating were exposed to well-defined
18 and highly-repeatable heating conditions in accordance with the H-TRIS test method. Experimental
19 results emphasise that the swelling process and the resulting swelled thickness govern the thermo-
20 physical response of intumescent coatings, thus their effectiveness. During swelling, the coated
21 steel asymptotically tends to the temperature range 300-350°C, regardless of the heating condition
22 or the initial DFT. Thermo-Gravimetric Analysis (TGA) experiments demonstrate that the coating
23 undergoes the swelling reaction at this temperature range. Once the swelling process is completed,
24 the steel temperature increases above 350°C. The steel temperature acts as an indicator of the
25 swelling process, as the reaction occurs in the proximity to the steel-coating interface. The
26 intumescent coating swells and insulates the steel substrate by displacing the already-swelled
27 coating towards the direction of the source of heat. Aiming at predicting the swelling of
28 intumescent coatings, empirical correlations are derived: the swelling rate is governed by the
29 heating conditions and the maximum swelled thickness is governed by the applied initial DFT.

30 **Keywords:** intumescent coatings; steel structures; swelling; heating conditions; initial thickness;
31 heat transfer; fire testing; H-TRIS; fire safety.

32 1. Introduction and background

33 Steel structures represent a mainstream building structural system in the modern construction
34 industry. As structural systems, the integrity and stability of steel structures may be compromised
35 during and after a fire due to loss of strength and stiffness, as well as thermally induced forces and
36 displacements [1]. The application of thermal barriers characterised by low thermal diffusivity is
37 the traditional solution to reduce the temperature increase of the load-bearing structure during a

38 fire [2]. Conventional solutions, such as gypsum plasterboards or cementitious spray-on systems,
39 are usually deemed to be relatively inexpensive and easy to apply, but aesthetically unpleasant and
40 an undesirable choice in varied applications, such as slender structures with visible steelwork.

41 The unique advantages of intumescent coatings, such as the low impact on the attractive
42 architectural appearance of bare steel structures and flexibility for both on- and off-site
43 applications, have fostered their success and extensive use all over the world [3-5]. Consequently,
44 intumescent coatings currently represent a dominant fire safety solution for protecting load-bearing
45 structural steel systems. Upon sufficient heating, intumescent coatings swell to form a low-density
46 and highly-insulating porous media that prevents the steel elements from reaching high
47 temperatures [6]. The formulation of thin intumescent coatings for the built environment is
48 typically waterborne or solvent-based. They are usually applied to a target Dry Film Thickness
49 (DFT) of a few millimetres and, when exposed to heat, they can swell up to 100 times their initial
50 thickness [5, 7].

51 Within the structural and fire safety engineering practice, the insulating capacity of intumescent
52 coatings is commonly assessed using two simplified engineering design methods based on
53 exposure to the standard temperature-time fire curve in a furnace [8-9]. These methods are
54 developed based on experimentally measured temperatures of coated steel samples tested in a
55 standard fire resistance test. The first method consists of creating *tabulated fire ratings*, where
56 manufacturers offer design tables that list the minimum DFTs required to ensure a certain level of
57 fire protection (i.e. the steel temperature remains below a certain predefined critical value in the
58 standard fire resistance furnace test). Alternatively, the European *effective thermal conductivity*
59 *method* can be used to simulate the heat transfer from the fire into the steel using a lumped
60 capacitance approximation of the transient heat conduction problem [9]. This method assumes that
61 the intumescent coating does not expand, but it experiences a transient change of its thermal
62 conductivity. The resulting temperature-dependent effective thermal conductivity of the
63 intumescent coating estimates an equivalent thermal barrier to the protected structure and this
64 method implicitly assumes that the thermo-physical properties of the intumescent coating only
65 depend on the temperature [10]. However, intumescent coatings are chemically reactive materials
66 and numerous researchers have emphasised the influence of the heating conditions on the
67 intumescent process and the overall insulating effectiveness [6, 11-16]. In particular, slow-growing
68 fires or low heating regimes may have a negative impact on the insulating performance of
69 intumescent coatings by causing incomplete swelling or even melting and delamination [6, 14, 15].

70 As a consequence, the current procedures do not represent a comprehensive design practice to
71 ensure the fire safety of steel structures. They do not fully assess the effectiveness of intumescent
72 coatings through a detailed characterisation of the heat transfer within the swelling coating. Most
73 importantly, these simplified engineering methods simulate the temperature evolution of coated
74 steel samples in furnaces exposed to a single heating scenario, not addressing the whole range of
75 potential heating regimes occurring in a fire. In a world moving towards performance-based
76 engineering solutions, there is a need for explicitly understanding how different factors may
77 influence the effectiveness of intumescent coatings, e.g. heating conditions and applied initial
78 thickness. By obtaining this scientific and practical knowledge, it will be possible to formulate and
79 validate models able to produce realistic and reliable predictions for the fire-safe design of steel
80 structures [10].

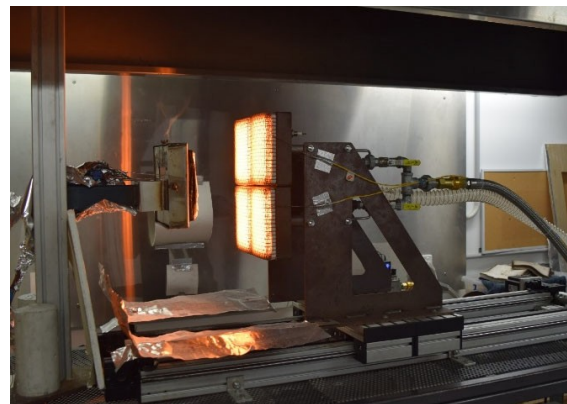
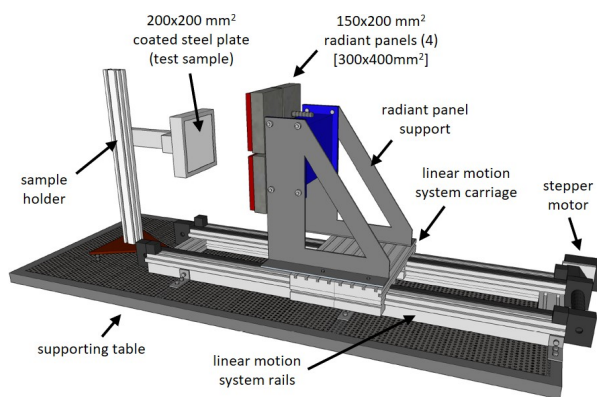
81 The available literature presents limited research studies that have looked at assessing the
82 effectiveness of intumescent coatings through their thermo-physical response [10]. This progress
83 is commonly inhibited by inadequate testing methodologies and experimental setups. In particular,
84 standard fire resistance tests in furnaces have been questioned due to the poor repeatability and the
85 uncertain thermal boundary conditions imposed on test samples [17-18]. In addition, the closed
86 environment of standard furnaces does not allow for accurate visual inspection of test samples
87 during the heating exposure, a key aspect to comprehend the thermo-physical response of
88 intumescent coatings [19]. A few researchers have proposed various approaches and
89 methodologies to analyse the heat transfer within intumescent coatings by placing in-depth
90 thermocouples within intumescent coatings [20-22]. However, this methodology has been adopted
91 in only a few cases because of the experimental difficulties related to gauging accurate
92 measurements of the in-depth temperature distributions without disturbing the swelling process.

93 The study presented herein shows an experimental methodology aimed at analysing the
94 effectiveness of intumescent coatings through a detailed characterisation of their thermo-physical
95 response. In particular, the influences of different heating conditions and the applied initial
96 thickness were investigated. Steel plates coated with a commercial solvent-based thin intumescent
97 coating were exposed to well-defined and highly-repeatable heating conditions using the Heat-
98 Transfer Rate Inducing System (H-TRIS) test method. Test samples were thoroughly instrumented
99 in order to measure the real-time swelled coating thickness, the exposed surface temperature, the
100 steel temperature and the in-depth transient temperature profile within the intumescent coating.

101 2. Material and methods

102 2.1 Experimental methodology

103 The experimental methodology was chosen in order to have direct control and quantification of the
104 thermal boundary conditions imposed on the test samples, ensuring high repeatability between
105 experiments at low economic and temporal costs. The Heat-Transfer Rate Inducing System (H-
106 TRIS) offers these advantages over conventional testing, therefore it was selected as the appropriate
107 experimental methodology [18]. H-TRIS accurately controls the relative position between the
108 target exposed surface of the test sample and the surface of an array of radiant panels, moving on
109 a computer-controlled linear motion system (Fig. 1). In this way, H-TRIS is able to impose a well-



110 Fig. 1. Illustration of the experimental setup based on the H-TRIS test method.

111 defined time-history of incident radiant heat flux on the exposed surface of the test sample. In
112 addition, thanks to its open environment, H-TRIS allows for the visual inspection of the test
113 samples during the heating exposure (e.g. measuring the swelled coating thickness). The H-TRIS
114 assembled for this specific research study was composed of four high-performance natural-gas-
115 fired radiant panels mounted on a supporting frame and creating a 300 x 400 mm² radiant source
116 of heat (Fig. 1). In this configuration, the apparatus can impose a wide range of incident radiant
117 heat fluxes included between 5 and 100 kW/m² [19].

118 2.2 Test samples and description of the experiments

119 The samples used in this experimental study are 200 x 200 mm², 10 mm thick mild carbon steel
120 plates, resulting in a section factor A_p/V (i.e. ratio between exposed surface and volume of steel)
121 equal to 100 m⁻¹ (Fig. 1). Based on the assembled H-TRIS, the sample dimensions were chosen in
122 order to achieve a surface distribution of incident radiant heat flux on the sample surface with a
123 deviation lower than 10%. The steel plates were professionally coated with a solvent-based thin
124 intumescent coating. The product is commercialised worldwide for providing up to 120 minutes
125 fire resistance to universal steel sections and cellular beams. It is commonly used in the built
126 environment for internal, semi-exposed or external use and it is suitable for off-site and on-site
127 application. The coating is a fast-track and self-priming coating, therefore it was applied in one
128 hand using airless spray equipment, without the use of any primer or topcoat. After one month of
129 curing, the applied DFT was measured using a non-destructive film thickness gauge at five
130 different locations (at each corner and the centre of each coated plate). Based on the mean DFT
131 measured over the steel plate surface, the test samples were selected to be categorised into three
132 groups:

- 133 □ “Low DFT” – 1.00 mm (± 0.20 mm)
- 134 □ “Medium DFT” – 1.80 mm (± 0.20 mm)
- 135 □ “High DFT” – 2.90 mm (± 0.20 mm)

136 Using the H-TRIS test method, coated samples were individually tested for 60 minutes under
137 different levels of constant incident radiant heat flux: 10, 25, 40, 50, 70 and 90 kW/m² (Table 1).
138 The heating conditions were explicitly chosen in order to subject the intumescent coating to various
139 ranges of temperatures and heating rates, triggering the swelling reaction in different ways.
140 Particularly, based on a previous research study, a constant incident radiant heat flux of 10 kW/m²
141 was expected not to initiate the swelling process of the intumescent coating [15]. During the heating
142 exposure, a custom-built steel frame was used in order to hold the test sample aligned with the
143 inirepeatable thermal boundary conditions, heat losses at the back of the test sample were
144 minimised by insulating the unexposed surface of test samples using a layer of 20 mm thick ceramic
145 wool (ISOLITE ISOWOOL blanket) and 13 mm thick plasterboard (Knauf FireShield).

146 2.3 Instrumentation

147 The experimental setup was instrumented in order to systematically gauge all the possible
148 information necessary to describe the thermo-physical response of the intumescent coating during
149 the heating exposure.

- 150 1) The *thickness of the swelled intumescent coating* was measured by image processing of video
151 footages taken using a high-resolution camera placed at the side of the test sample, aligned with

152 the surface of the test sample (Fig. 2). The swelled coating thickness was estimated in
 153 correspondence of the central area of test samples, therefore disregarding edge effects at the
 154 sample boundaries. The real-time measurement of the coating thickness was also used for
 155 continuously adjusting the relative distance between the intumescent coating surface and the
 156 array of radiant panels. In this way, the incident radiant heat flux at the exposed surface of the
 157 test sample was maintained to the specified value during the full duration of experiments.

158 2) Up to seven K-type thermocouples (1.5 mm diameter) were installed in the test sample in order
 159 to measure the *transient temperature profile within the intumescent coating*. Prior to testing, 1.8
 160 mm holes were drilled through the steel plate in order to allow the insertion of the in-depth
 161 thermocouples from the rear of the test sample (Fig. 2). Preliminary tests evidenced that, if the
 162 thermocouples were placed at the beginning of the heating exposure, they would have perturbed
 163 the swelling process and the development of the intumescent char. Therefore, the thermocouples
 164 were inserted at specific locations within the swelling coating during the heating exposure. The
 165 real-time measurement of the swelled coating thickness was used to understand when a
 166 thermocouple could be inserted at a certain depth. The thermocouples were positioned at depths
 167 multiple of 5 mm from the interface between the coating and the steel plate: 5, 10, 15, 20, 25,
 168 30, 35 mm. Particular care was taken in order not to damage the surface crust developed by the
 169 intumescent coating, which represents a key feature for the development of an effective thermal
 170 barrier [14].

171 3) The *temperature of the steel plate* was measured using up to three K-type thermocouples
 172 attached to the unexposed surface of the test samples (Fig. 2).

173 4) The *exposed surface temperature of the intumescent coating* was measured using an Infra-Red
 174 camera (model FLIR SC655: 16-bit 640 x 480 pixel resolution at 50 Hz, spectral range 7.5 - 14
 175 μm , temperature range up to 2000 °C) (Fig. 2).

Table 1. Test matrix.

| Sample group | Heating conditions | Number of repetitions | DFT _{mean} [mm] |
|---------------------|----------------------|-----------------------|--------------------------|
| “Low DFT” | 10 kW/m ² | 1 | 0.887 |
| | 25 kW/m ² | 2 | 1.062, 1.204 |
| | 30 kW/m ² | 2 | 0.996, 1.069 |
| | 50 kW/m ² | 2 | 1.194, 1.196 |
| | 70 kW/m ² | 2 | 1.162, 1.198 |
| | 90 kW/m ² | 3 | 1.134, 1.146, 1.146 |
| “Medium DFT” | 10 kW/m ² | 2 | 1.620, 1.712 |
| | 25 kW/m ² | 2 | 1.638, 1.786 |
| | 30 kW/m ² | 2 | 1.680, 1.816 |
| | 50 kW/m ² | 3 | 1.794, 1.920, 2.014 |
| | 70 kW/m ² | 2 | 1.712, 1.898 |
| | 90 kW/m ² | 3 | 1.630, 1.770, 1.870 |
| “High DFT” | 10 kW/m ² | 1 | 2.716 |
| | 25 kW/m ² | 2 | 2.714, 2.902 |
| | 30 kW/m ² | 2 | 2.750, 2.822 |
| | 50 kW/m ² | 2 | 2.854, 2.866 |
| | 70 kW/m ² | 2 | 2.878, 2.954 |
| | 90 kW/m ² | 3 | 2.992, 3.038, 3.086 |



177
178
179

Fig. 2. Different aspects of the experimental setup designed to gauge the thermo-physical response of intumescent coatings during heating exposure.

180 2.4 Thermo-Gravimetric Analysis (TGA)

181 Aside from the experiments using H-TRIS, Thermo-Gravimetric Analysis (TGA) was performed
182 on small powder samples of dry intumescent coating (8-10 mg) in order to study the thermal
183 decomposition of the intumescent coating and understand at which temperature ranges the different
184 reactions occur, particularly the intumescent swelling reaction. The TGA experiments were carried
185 out using a PerkinElmer STA 6000. The intumescent coating was tested under different heating
186 rates (5, 10, 20 and 30 °C/min) under N₂ or air in the temperature range 30-900 °C.

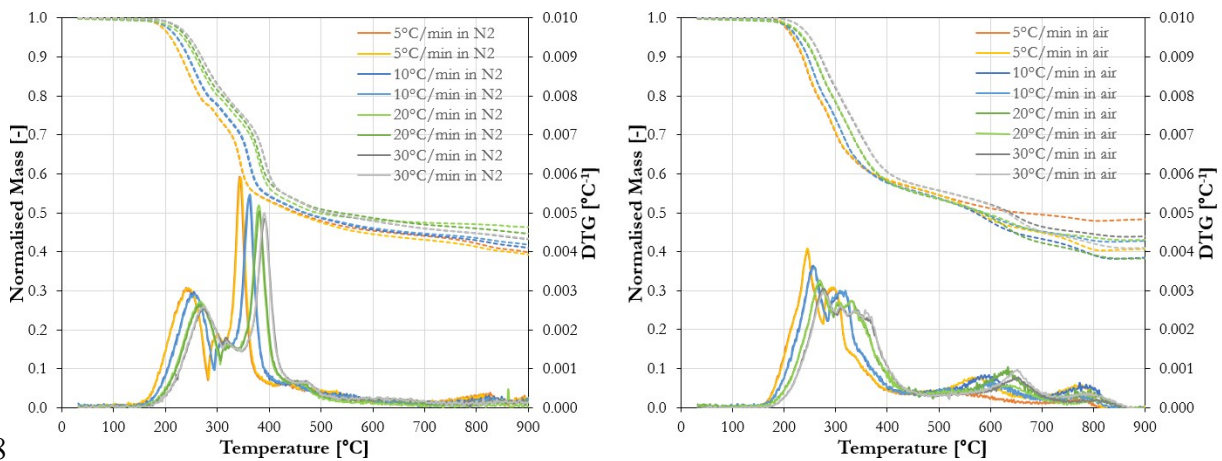
187 3 Experimental results

188 3.1 TGA results

189 Fig. 3 presents the results obtained from the TGA experiments in terms of normalised mass and its
190 derivative (DTG curve). According to the available literature, the TGA results highlights that the
191 product tested in this experimental study has similar characteristics to typical intumescent
192 formulations. For instance, the common intumescent formulations are typically composed of a
193 combination of ammonium polyphosphate (APP) as carbonisation catalyst, pentaerythritol (PER)
194 as carbonisation agent, melamine (MEL) as blowing agent and acrylic resin as carbonic agent and
195 binder. In these typical formulations, the carbonisation catalyst and agent transform their crystalline
196 structure and melt at temperatures between 200 and 300°C, increasing the coating viscosity and
197 releasing volatiles. The first peak in the DTG curves denotes this process, usually specified as
198 “*Thermal Decomposition Zone*” or “*Melting Zone*”. The further decomposition and interaction of
199 the different chemical compounds lead to the formation of the porous char structure by
200 esterification: the blowing agent is activated and it releases large quantities of gases, which are
201 trapped within the molten coating. The second peak in the DTG curves denotes this process, usually
202 specified as “*Reaction Zone*” or “*Swelling Zone*” at temperatures between 300 and 400°C. The
203 single reactions of the different compounds are often difficult to outline because of the synergic
204 effect of blowing agent, carbonization catalyst and agent due to their similar decomposition and

205 reaction temperatures. In the two different atmospheres and under different heating rates, the main
 206 reactions occur at similar temperature ranges (200-400°C). These reactions are typically
 207 endothermic. Additionally, an oxidising atmosphere results in reactions shifting towards lower
 208 temperatures with a lower reaction rate compared to a reducing atmosphere. Another difference
 209 arises when the char gradually oxidises at temperatures higher than 600°C: the porous char structure
 210 degrades and CO₂ is released. This aspect is emphasised in the TGA results in air atmosphere: a
 211 first reaction was detected at about 650°C and a second reaction at about 800°C. The oxidation
 212 reactions are exothermic and they produce minor mass loss (lower than 5% each) [10, 23, 24].

213 In general, it is important to underline that the intumescent swelling reaction (second DTG peak)
 214 typically occurs at temperatures between 350 and 400°C and the main reactions of the intumescent
 215 coating can be considered to be completed at about 400 °C. At that temperature the main
 216 decomposing and swelling reactions are completed: the majority of the mass has been lost (about
 217 40%), seeing the significant amount of inorganic compounds (about 40-45%).



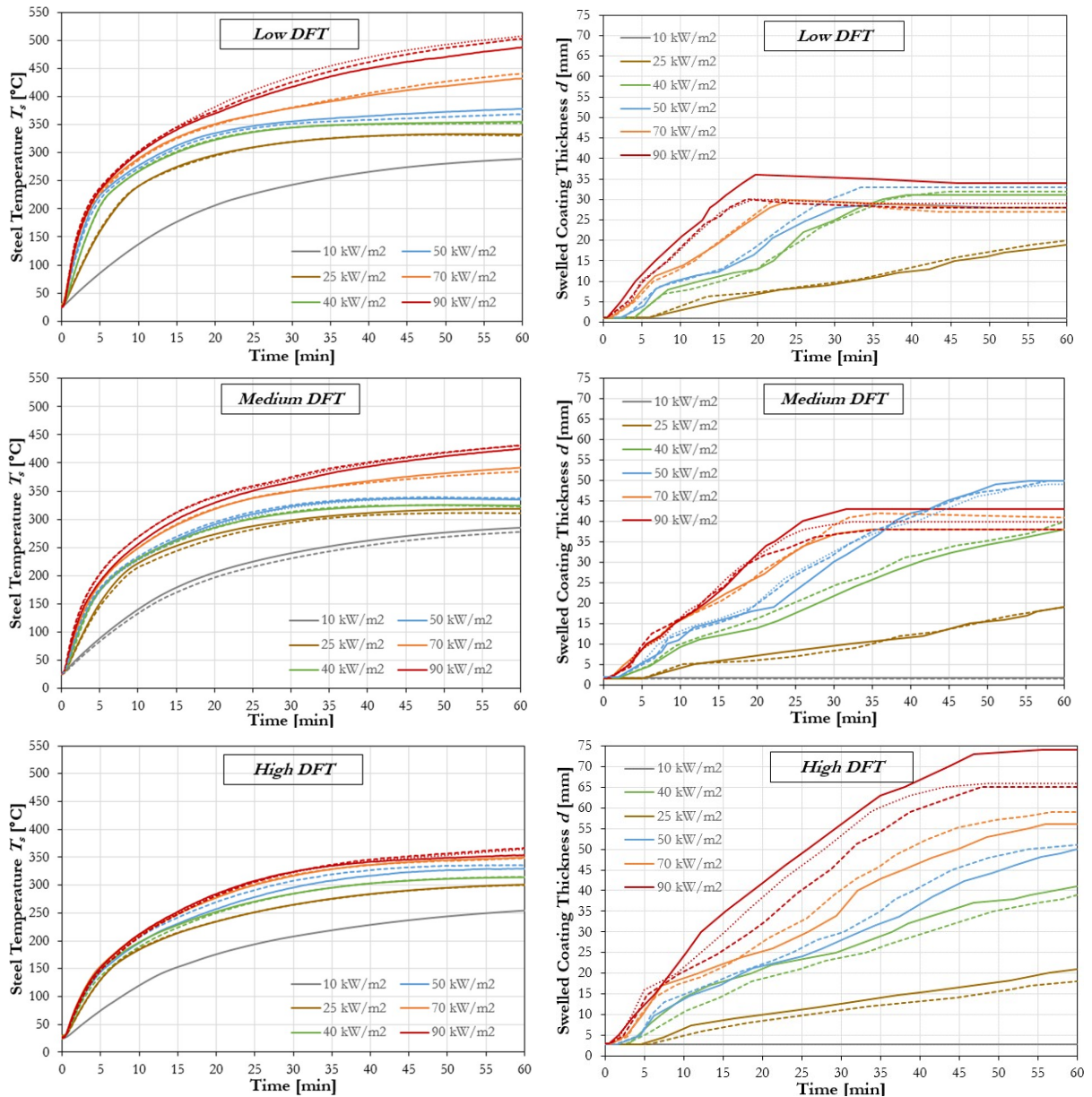
218
 219 Fig. 3. TGA results in nitrogen (left) and air (right) atmospheres.

220 3.2 Steel temperatures and swelled coating thicknesses

221 Regarding the results obtained from the H-TRIS experiments, the performance of intumescent
 222 coatings was firstly characterised according to the evolution of the steel temperatures and the
 223 swelled coating thicknesses during the thermal exposure. Fig. 4 shows the evolution of the steel
 224 temperatures and the swelled coating thicknesses for all the different experiments carried out on
 225 coated samples. The good repeatability between experiments was confirmed by the agreement of
 226 the temperature readings and the estimations of the swelled coating thickness. Throughout all the
 227 experiments, the steel temperatures measured using thermocouples had deviations lower than 10%,
 228 the central area of the test samples swelled rather homogeneously and the swelled coating
 229 thicknesses were measured with an accuracy of ± 2 mm. For simplicity and neatness of graphical
 230 visualisation, only the average values are displayed in this manuscript. In the graphs, the same
 231 colour collects all the experiments with the same heating conditions, while continuous, dashed and
 232 dotted lines reports single experimental repetitions.

233 As regards the steel temperatures, most of the coated steel plates reached a steady-state temperature
 234 by the end of the heating exposure. However, in a few cases, the steel never reached a quasi-steady
 235 state temperature and the temperature kept increasing during the heating exposure, such as 50, 70

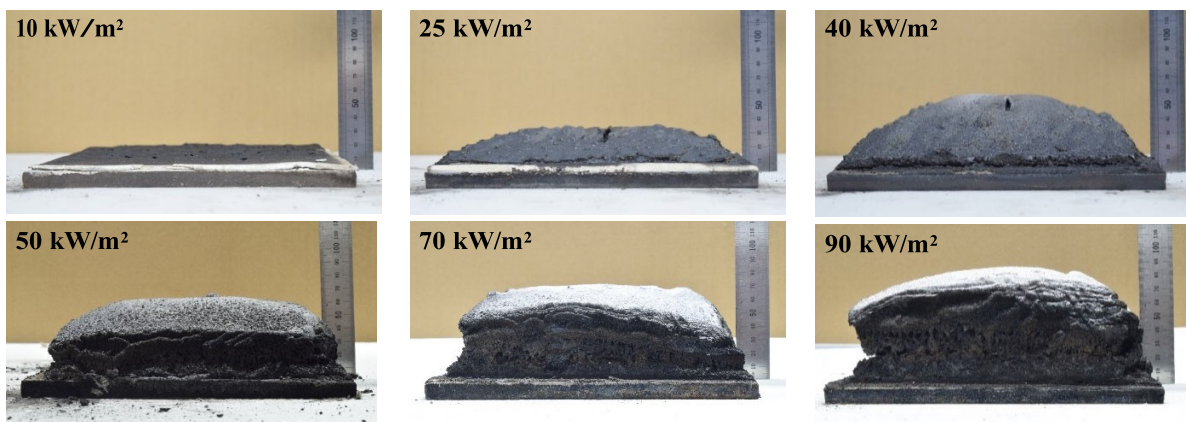
236 and 90 kW/m² for “*Low DFT*” and 70 and 90 kW/m² for “*Medium DFT*”. This aspect can be
 237 directly associated with the completion of the swelling process of the intumescent coating: in these
 238 cases, the coating completed the swelling process before the end of the experiment. In other cases,
 239 where the coating continuously swelled during the experiments, the steel plates tended to a similar
 240 range of steady-state temperatures, included between 300 and 350°C. The external incident heat
 241 flux had a minor influence. On the other hand, a higher applied initial DFT foreseeably produced
 242 a lower steady-state steel temperature due to the thicker porous char.



243 Fig. 4. Comparison of the evolution of the coated steel temperatures and the swelled coating
 244 thicknesses for the different applied initial DFTs and different constant incident heat fluxes.

245 With regards to the swelled coating thicknesses, right after the application of the incident heat flux,
 246 the intumescent coating quickly started swelling with different rates depending on the heating

247 conditions, i.e. the slope/derivative of the thickness-time curve (Fig. 4). As expected, the samples
 248 exposed to 10 kW/m^2 did not practically swell, regardless of the applied initial DFT. For the higher
 249 heat fluxes, the swelling rate of the intumescent coating appeared to be directly influenced by the
 250 external incident heat flux, while independent on the applied initial DFT. On the contrary, the
 251 applied initial DFT governed the maximum thickness that the coating could have reached during
 252 the thermal exposure. In particular, test samples coated with “*Low DFT*”, “*Medium DFT*” and
 253 “*High DFT*” swelled up to about 30 mm, 40 mm and 65 mm, respectively. Fig. 5 shows the typical
 254 porous chars developed by the intumescent coating at the end of the thermal exposure: as shown
 255 in Fig. 4, a thicker intumescent porous char was produced for a higher constant incident heat flux.
 256 In order to emphasise the difference between different heating conditions, Fig. 5 reports the test
 257 samples coated with “*High DFT*”: in this case, the intumescent coating was able to swell
 258 throughout the whole duration of the heating exposure and develop the thickest porous chars
 259 (within the limits of this experimental study). For high heat fluxes, Fig. 5 also highlights the
 260 oxidation reactions occurring at the surface of the intumescent coating: the char turned into ash at
 261 the coating surface crust, characterised by a white/grey colour. This phenomenon can be clearly
 262 observed for constant incident heat fluxes of 70 and 90 kW/m^2 , partially for 50 kW/m^2 . Fig. 5 also
 263 shows that typical porous chars formed into a dome-like shape, in some cases (40 kW/m^2) more
 264 than others. However, the char shape had a minor influence on the experimental outcomes of this
 265 research study because all the temperature and swelling measurements were concentrated in the
 266 central area of the test sample, where even temperature and homogenous swelling were observed.
 267 In addition, the one-dimensional heat transfer was ensured due to the small view factor of the
 268 sample edges compared to the exposed surface of the intumescent coating.



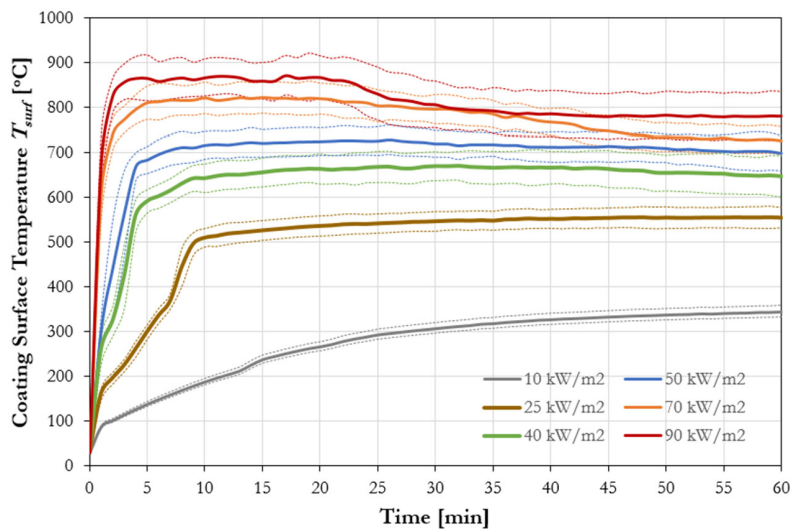
269 Fig. 5. Typical porous chars developed by the intumescent coating at the end of the thermal
 270 exposure for different constant incident heat flux (“*High DFT*”).

271 3.3 Surface coating temperature

272 In a post-test analysis, the temperature evolution at the exposed surface of the intumescent coating
 273 was evaluated by processing the data obtained by the Infra-Red camera. The coating emissivity
 274 value was set equal to 0.90 and the coating temperature was averaged over a $50 \times 50 \text{ mm}^2$ area,
 275 placed at the centre of the test sample. The emissivity value has a key role in this process and it can
 276 significantly influence the results. Consequently, a sensitivity analysis of the surface emissivity
 277 value of the intumescent coating was performed: the same procedure was repeated for varying
 278 coating emissivity 0.90 ± 0.05 , accordingly to the average values found in a previous research study

279 (spectral range 2 - 20 μm) [15]. Fig. 6 shows the envelopes of the measured temperatures at the
280 coating surface in all the experiments carried out under different heating conditions and applied
281 initial DFTs. The continuous lines report the average temperatures calculated with an emissivity
282 equal to 0.90, while the dotted lines define the envelopes obtained from the sensitivity analysis
283 (maximum values: $\varepsilon = 0.85$; minimum values: $\varepsilon = 0.95$).

284 During the different experiments, the coating behaved like a low thermal inertia material by quickly
285 reaching a specific surface temperature depending on the external heat flux and keeping a quasi-
286 constant temperature during the rest of the heating exposure (thermally thick material characterised
287 by a high Biot number). As expected, higher coating surface temperatures were measured for higher
288 external constant incident heat fluxes. The applied initial DFT did not significantly influence the
289 evolution of the coating surface temperature. In the second part of the heating exposure, the measured
290 temperature gradually decreased, particularly for higher heat fluxes. This aspect could be related to
291 the reduction in the emissivity due to the oxidation of the coating surface, which can be visually
292 assessed through the colour change (white/grey). Another reason could be related to the migration
293 of the oxidation front within the intumescent porous char: once the oxidation reaction (exothermic)
294 is completed, the surface temperature decreases. Without any doubt, the lower surface temperatures
295 measured in the cases of 70 kW/m^2 and 90 kW/m^2 can be directly associated with oxidation processes
296 taking place at the coating surface. For heat fluxes higher than 50 kW/m^2 , the measured surface
297 temperatures were above 700°C: at this temperature range, oxidation is expected. This aspect is
298 confirmed by the TGA results in oxidising atmosphere and photographs of the intumescent porous
299 chars (Fig. 5), but it certainly needs further investigation to clarify the effects of the surface oxidation
300 on the emissivity of swelling intumescent coatings.



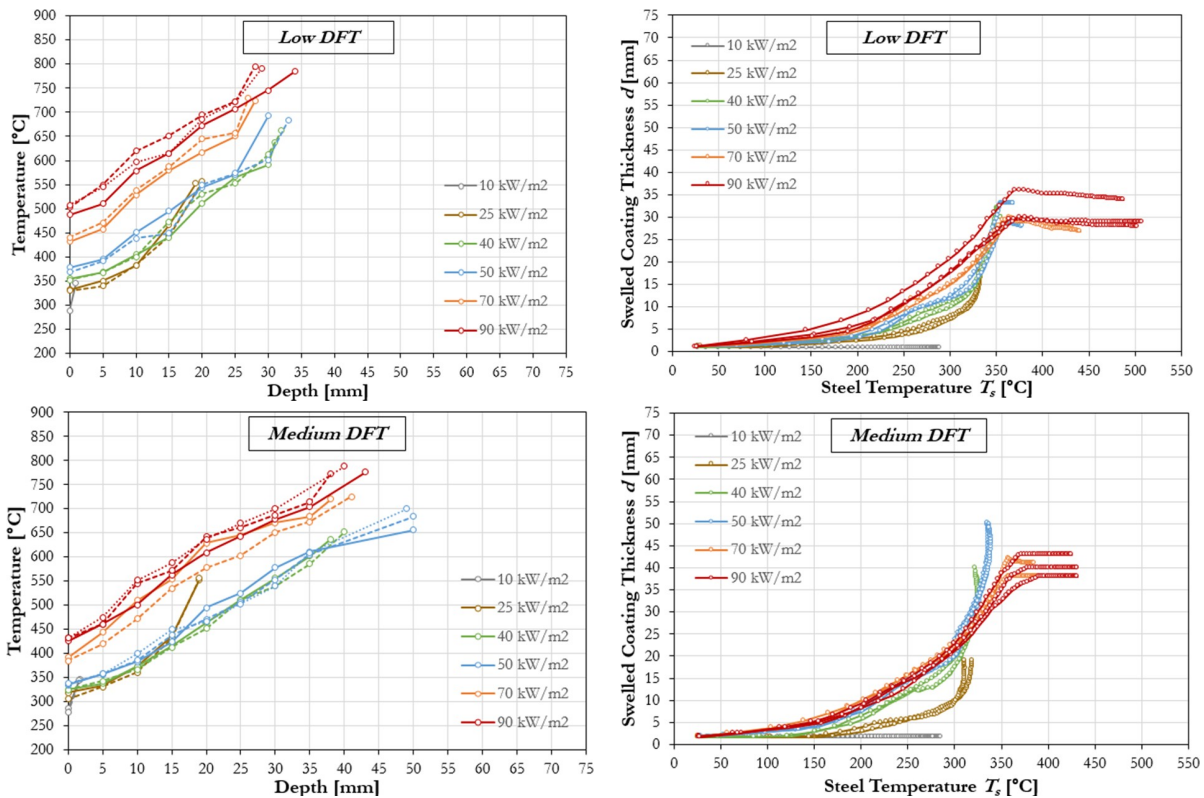
301 Fig. 6. Envelopes of the temperature evolution at the coating surface for the different external
302 constant incident heat fluxes (all experiments with different applied initial DFTs are included).
303

304 3.4 Temperature profiles within the swelling coating

305 The heat transfer within swelling intumescent coatings was then investigated analysing the
306 evolution of the in-depth temperature profiles. First, the agreement of the temperature readings
307 between different experimental repetitions confirmed the good repeatability. In addition, the results

308 highlighted the success of the designed experimental methodology able to accurately gauge the

309 thermo-physical response of intumescent coatings. Comparisons between experiments with and
 310 without in-depth thermocouples also confirmed the minor interference of the installed
 311 instrumentation. Fig. 7 shows the temperature profiles measured at the end of the heating exposure
 312 for all the different experiments on coated samples. The temperature profiles can be assumed as
 313 steady-state if the swelling process of the intumescent coating was completed. The in-depth
 314 temperatures at different depths within the intumescent coating are reported with the average
 315 surface temperatures ($\epsilon = 0.90$). For visualisation purposes, the error bars were omitted from the
 316 graphs. However, the in-depth thermocouples were placed within the intumescent coating with an
 317 accuracy ± 2 mm and the measured in-depth temperatures had a deviation lower than 10%. The
 318 steady-state temperature profiles shown in Fig. 7 had similar thermal gradients (slope of the in-
 319 depth temperature profile) within the intumescent coating. This aspect suggested that the
 320 intumescent porous char had similar thermal and physical properties, regardless of the imposed
 321 heating conditions. As already explained in the previous section, after the first transient period, the
 322 coating surface temperature can be considered as constant and it can be directly related to the
 323 external constant incident heat flux. Regarding the steel substrate, if the coating underwent
 324 continuous swelling, the steel temperature remained within a similar range ($300\text{-}350^\circ\text{C}$).
 325 Consequently, the thermal gradient with the intumescent coating was governed by the swelled
 326 coating thickness. Since the extremes of the intumescent coating can be considered to have a quasi-
 327 constant temperature, further swelling resulted in stretching the thermal gradient between the steel
 328 substrate and the coating surface. This aspect is highlighted in Fig. 9: at 50 kW/m^2 , a steel plate
 329 coated with “*High DFT*” continuously swelled during the heating exposure and the steel
 330 temperature did not overcome 350°C . On the other hand, at 50 kW/m^2 , a steel plate coated with
 331 “*Low DFT*” completed the swelling reaction after about 30-35 minutes of heating exposure and,
 332 beginning from that moment, the steel temperature started increasing above 350°C .



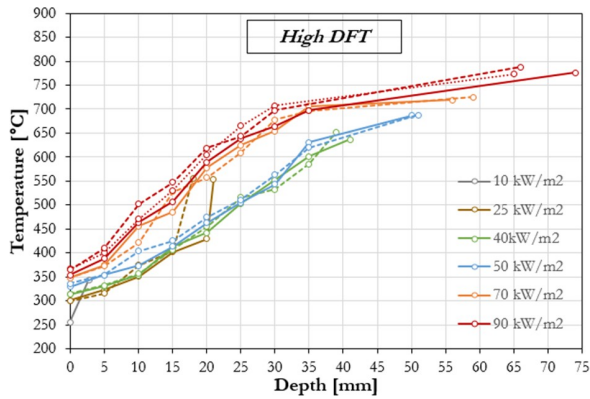


Fig. 7. Comparison of the measured temperature profiles at the end of the heating exposure for different applied initial DFTs and different constant incident heat fluxes.

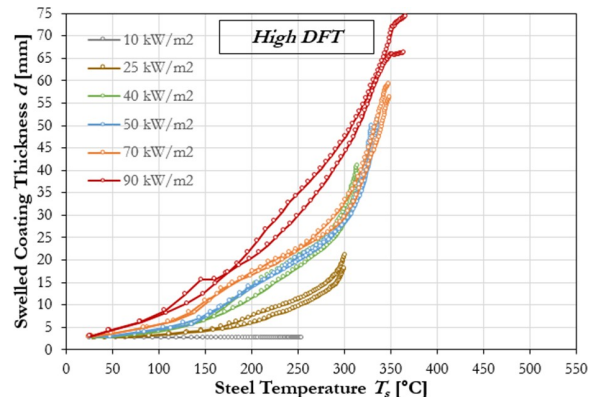
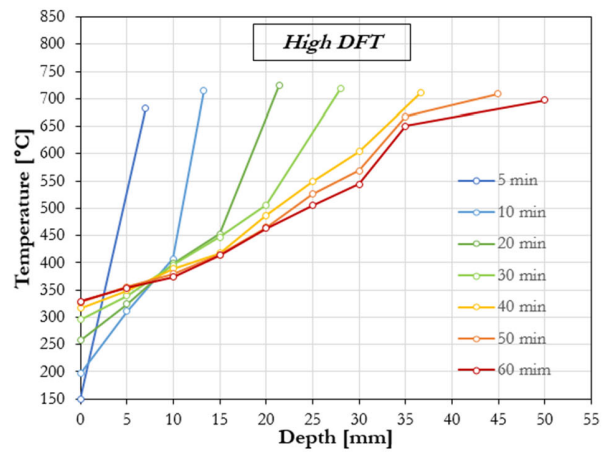
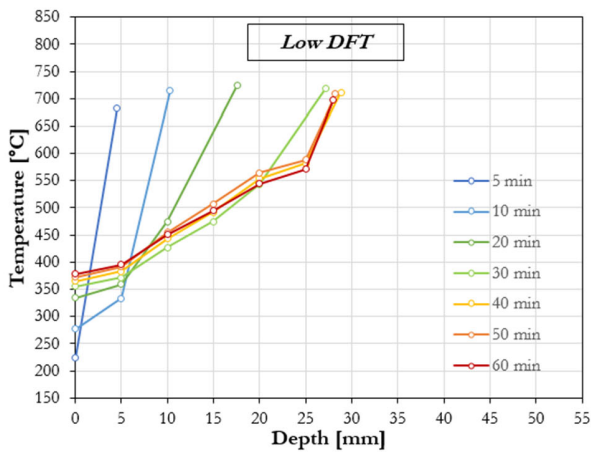


Fig. 8. Swelled coating thicknesses as a function of the coated steel temperature for different applied initial DFTs and different constant incident heat fluxes.

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Fig. 9. Comparison of the evolution of the temperature profiles (in-depth and surface) at different instants during the heating exposure with different applied initial DFTs exposed to 50 kW/m^2 .

337 4 Analysis and discussion

338 So far, the experimental investigation has underlined how the evolutions of the steel temperature
 339 and the swelled coating thickness are closely related and they have key roles in the understanding
 340 and the assessment of the effectiveness of intumescent coatings. Fig. 8 reports the evolution of the
 341 swelled coating thicknesses as a function of the coated steel temperature for different applied initial
 342 DFTs and heating conditions. The experimental results confirmed how, in case of continuous
 343 swelling, the coated steel plates asymptotically tended to a similar temperature range included
 344 between 300 and 350°C , regardless of the heating condition or the applied initial DFT. Contrarily,
 345 when the coating completed the swelling process, the steel temperatures increased above this
 346 threshold. This aspect is supported by the results obtained by TGA: the intumescent swelling
 347 reaction occurs at temperatures between 350 and 400°C and it can be considered to be completed
 348 at about 400°C .

349 The evolution of coated steel temperatures provides a first assessment of the coating effectiveness:
350 i.e. the colder the steel, the better thermal insulation. In turn, as shown in Fig. 8, the coated steel
351 temperatures can be directly linked to the coating swelling process. Therefore, it can be concluded
352 that the swelling process and the resulting swelled thickness govern the thermo-physical response
353 of intumescent coatings, thus their effectiveness. In particular, the coated steel temperature acts as
354 an indicator of the swelling process of intumescent coatings: if the steel temperature overcomes
355 350°C, the swelling reaction is completed. This aspect has been verified also by a close
356 investigation of the recorded video footage. This experimental outcome suggests that the swelling
357 reaction takes place close to the steel substrate: particularly, about the interface between the steel
358 and the applied intumescent coating. The intumescent coating swells and insulates the steel
359 substrate by displacing the already-swelled coating towards the direction of the source of heat. The
360 swelling reaction continues at the virgin coating located behind the swelled porous char and in the
361 proximity to the steel substrate. This process lasts until the intumescent coating is fully consumed,
362 which can be directly related to the applied initial DFT. As a conclusion, the steel temperature can
363 be directly associated with the swelling process because it defines the temperature experienced by
364 the virgin coating, which is located behind the swelled porous char and sustains the swelling
365 reaction [25].

366 The non-unique relationship between the steel temperature and the swelled coating thickness
367 shown in Fig. 8 may be explained by the direct influence of the heating conditions. In particular,
368 experimental results highlighted that higher external incident heat fluxes produced higher coating
369 thicknesses while the steel remains at the same temperature. Assuming similar thermal and physical
370 properties of the intumescent porous char (as discussed in section 3.4), a higher net heat flux to the
371 virgin coating, which sustains the swelling reaction, is expected. Consequently, a higher incident
372 heat flux at the coating surface provides higher net heat flux to the swelling reaction, thus it governs
373 the swelling rate. For instance, an incident heat flux of 10 kW/m² did not trigger the swelling
374 reaction due to the low steel temperatures (below 300°C) and the low net heat flux received by the
375 virgin coating.

376 Nevertheless, the experimental study presented herein emphasised how the swelling process and
377 the resulting swelled thickness govern the thermo-physical response of intumescent coatings, thus
378 their effectiveness. In particular, the influence of heating conditions and the applied initial DFT
379 can be clearly outlined and empirical correlations can be derived. First, the applied initial DFT
380 governs the maximum swelled thickness that the intumescent coating could have reached during
381 the thermal exposure. The applied initial DFT provides a quantification of the intumescent material
382 that can potentially swell and hence produces porous char. Fig. 10 defines a possible linear
383 correlation between the applied initial DFT and the maximum swelled thickness of the intumescent
384 coating after the completion of the swelling process. Regarding the heating conditions, the external
385 incident heat flux at the coating surface governs the swelling rate of intumescent coatings. Fig. 11
386 defines a possible linear correlation between the constant incident heat flux and the swelling rate
387 of the intumescent coating. In this calculation, the swelling rate of the intumescent coating was
388 linearised from the onset of swelling until the instant when the maximum swelled thickness was
389 reached. Theoretically, it should be possible to correlate the swelling rate to more fundamental
390 parameters, such as the net flux through the swelled porous char and received by the virgin coating
391 that sustains the swelling reaction. The process would be possible only by formulating a heat
392 transfer model. However, the thermal and physical properties of intumescent porous chars should
393 be defined in order to estimate such parameters. This aspect is outside the scope of the current

394 manuscript, but future studies will focus on that. As a conclusion, this experimental investigation
 395 presented how the swelling of intumescent coatings, which is the main factor that governs their
 396 thermo-physical response and their effectiveness, can be predicted starting from well-defined
 397 thermal boundary conditions at the coating surface and applied initial DFT.

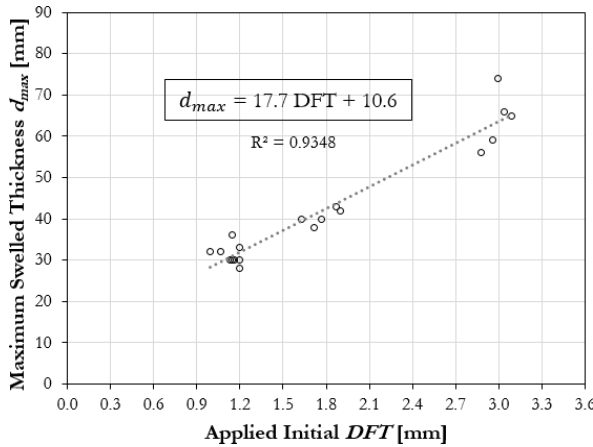


Fig. 10. Relationship between the applied initial DFT and the maximum swelled thickness of the intumescent coating.

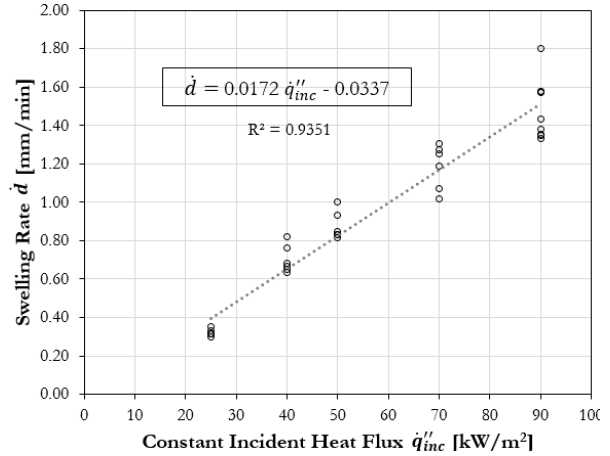


Fig. 11. Relationship between the external constant incident heat flux and the swelling rate of the intumescent coating.

398 5 Conclusions

399 The current practice of designing steel structures protected with intumescent coatings offers
 400 simplified engineering methods able to simulate the temperature evolution of coated steel samples
 401 tested in furnaces and exposed a single heating scenario. However, in a world moving towards
 402 performance-based solutions, there is a need for explicitly understanding how different factors may
 403 influence the effectiveness of intumescent coatings. The study presented herein shows an
 404 experimental methodology aimed at analysing the effectiveness of intumescent coatings through a
 405 detailed characterisation of their thermo-physical response for a range of heating conditions and
 406 applied initial dry film thickness (DFT). Steel plates coated with a commercial solvent-based thin
 407 intumescent coating were exposed to well-defined and highly-repeatable heating conditions using
 408 radiant panels and in accordance with the Heat-Transfer Rate Inducing System (H-TRIS) test
 409 method. Experimental results demonstrate high repeatability between experiments and the ability
 410 to measure real-time swelled coating thickness, the exposed surface temperature, the steel
 411 temperature and the in-depth transient temperature profile within the intumescent coating. From
 412 the experimental results, the following concluding remarks may be drawn:

- 413 □ The swelling process and the resulting swelled thickness govern the thermo-physical response
 414 of intumescent coatings, thus their effectiveness. During swelling, the temperature of coated
 415 steel plates asymptotically tends to a temperature range between 300 and 350°C, regardless of
 416 the heating condition or the applied initial DFT. When the coating completes its swelling
 417 process, the steel temperature increases above 350°C. This aspect is supported by the material
 418 characterisation obtained by TGA experiments: the swelling reaction occurs at temperatures
 419 between 350 and 400°C and it can be considered to be completed at about 400 °C.

- 420 □ The swelling reaction occurs in the proximity to the steel-coating interface. The intumescent
421 coating swells and insulates the steel substrate by displacing the already-swelled coating
422 towards the direction of the source of heat. This explains why coated steel temperature acts as
423 an indicator of the swelling process of intumescent coatings.
- 424 □ The measured in-depth temperature profiles within the swelling coating suggest that the
425 intumescent porous char has similar thermal and physical properties, regardless of the heating
426 conditions or the applied initial DFT. The thermal gradient within the intumescent coating is
427 governed by the swelled coating thickness.
- 428 □ The heating conditions and the initial thickness differently influence the swelling process of
429 intumescent coatings: the applied initial DFT governs the maximum swelled thickness, while
430 the external incident heat flux at the coating surface governs the swelling rate. Using the
431 empirical correlations derived based on the experimental results, the swelling of the tested
432 intumescent coating can be predicted.

433 Future studies should focus on quantifying the thermal and physical properties of the intumescent
434 porous char and implementing heat transfer models able to simulate the response of intumescent
435 coatings. In particular, it would be interesting to understand if the net heat flux to the virgin coating,
436 which is located behind the swelled porous char and sustains the swelling reaction, may be
437 correlated to the swelling rate. Finally, the authors believe that the product tested in this
438 experimental study represents a common behaviour of typical thin intumescent coatings
439 commercially available in the market. However, other products with different formulations should
440 be investigated before generalising research outcomes.

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512 Figure captions

513 Fig. 1. Illustration of the experimental setup based on the H-TRIS test method.

514 Fig. 2. Different aspects of the experimental setup designed to gauge the thermo-physical response
515 of intumescent coatings during heating exposure.

516 Fig. 3. TGA results in nitrogen (left) and air (right) atmospheres.

517 Fig. 4. Comparison of the evolution of the coated steel temperatures and the swelled coating
518 thicknesses for the different applied initial DFTs and different constant incident heat fluxes.

519 Fig. 5. Typical porous chars developed by the intumescent coating at the end of the thermal
520 exposure for different constant incident heat flux (*“High DFT”*).

521 Fig. 6. Envelopes of the temperature evolution at the coating surface for the different external
522 constant incident heat fluxes (all experiments with different applied initial DFTs are included).

523 Fig. 7. Comparison of the measured temperature profiles at the end of the heating exposure for
524 different applied initial DFTs and different constant incident heat fluxes.

525 Fig. 8. Swelled coating thicknesses as a function of the coated steel temperature for different
526 applied initial DFTs and different constant incident heat fluxes.

527 Fig. 9. Comparison of the evolution of the temperature profiles (in-depth and surface) at different
528 instants during the heating exposure with different applied initial DFTs exposed to 50 kW/m².

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530 intumescent coating.

531 Fig. 11. Relationship between the external constant incident heat flux and the swelling rate of the
532 intumescent coating.

533 Table captions

534 Table 1. Test matrix.